

Petroleum Refineries Monitoring Checklist



Final Rule: Mandatory Reporting of Greenhouse Gases

What Must Be Monitored if not Using a CEMS?

For flares, measure these parameters ...

Carbon dioxide emissions

If you monitor carbon content at least weekly:

- | | |
|--|--|
| <input type="checkbox"/> Volume of flare gas combusted during measurement period (daily or weekly) (standard cubic feet (scf)/period) | <input type="checkbox"/> Average carbon content of flare gas combusted during measurement period (daily or weekly) (kg C/kg flare gas) |
| <input type="checkbox"/> Average molecular weight of flare gas combusted during measurement period (daily or weekly) (kilogram (kg)/kilogram-mole) | |

Or:

- | | |
|--|--|
| <input type="checkbox"/> Volume of flare gas combusted during measurement period (daily or weekly) (scf/period) | <input type="checkbox"/> Mole percent concentration of compound "x" in the flare gas stream during the measurement period (mole percent = percent by volume) |
| <input type="checkbox"/> Mole percent CO ₂ concentration in the flare gas stream during the measurement period (mole percent = percent by volume) | |

If you monitor heat content at least weekly:

- | | |
|--|--|
| <input type="checkbox"/> Volume of flare gas combusted during measurement period (daily or weekly) (million (MM) scf/period) | <input type="checkbox"/> Higher heating value (HHV) for flare gas during measurement period (daily or weekly) (British thermal units (Btu/scf = mmBtu/MMscf) |
|--|--|

If you do not measure the higher heating value or carbon content of the flare gas at least weekly:

- | | |
|--|--|
| <input type="checkbox"/> Annual volume of flare gas combusted during normal operations from company records (MMscf/year) | <input type="checkbox"/> Volume of flare gas combusted during indexed start-up, shutdown, or malfunction event (scf/event) |
| <input type="checkbox"/> HHV for fuel gas or flare gas from company records (Btu/scf = mmBtu/MMscf) | <input type="checkbox"/> Average molecular weight of the flare gas during indexed start-up, shutdown, or malfunction event (kg/kg-mole) |
| <input type="checkbox"/> Number of start-up, shutdown, and malfunction events during the year exceeding 500,000 scf/day | <input type="checkbox"/> Average carbon content of flare gas combusted during indexed start-up, shutdown, or malfunction event (kg C/kg flare gas) |

Methane emissions

- Weight fraction of carbon in the flare gas prior to combustion that is contributed by methane from measurement values or engineering calculations (kg C in methane in flare gas/kg C in flare gas) (default is 0.4)

For catalytic cracking units and traditional fluid coking units with rated capacities greater than 10,000 barrels per stream day, measure these parameters...

Carbon dioxide emissions

- | | |
|--|---|
| <input type="checkbox"/> Hourly average percent CO ₂ concentration in the exhaust gas stream from the fluid catalytic cracking unit regenerator or fluid coking unit burner (percent by volume—dry basis) | <input type="checkbox"/> Hourly average percent CO concentration in the exhaust gas stream from the fluid catalytic cracking unit regenerator or fluid coking unit burner (percent by volume—dry basis) |
|--|---|

You must also determine the hourly average exhaust gas flow rate from the fluid catalytic cracking unit regenerator or fluid coking unit burner prior to the combustion of other fossil fuels by monitoring:

- Volumetric flow rate of exhaust gas from the fluid catalytic cracking unit regenerator or fluid coking unit burner prior to the combustion of other fossil fuels (dry scfh)

Or:

- Volumetric flow rate of air to the fluid catalytic cracking unit regenerator or fluid coking unit burner, as determined from control room instrumentation (dscfh)
- Hourly average percent oxygen concentration in exhaust gas stream from the fluid catalytic cracking unit regenerator or fluid coking unit burner (percent by volume—dry basis)
- Volumetric flow rate of oxygen enriched air to the fluid catalytic cracking unit regenerator or fluid coking unit burner, as determined from control room instrumentation (dscfh)
- Hourly average percent CO₂ concentration in the exhaust gas stream from the fluid catalytic cracking unit regenerator or fluid coking unit burner (percent by volume—dry basis)
- Oxygen concentration in oxygen enriched gas stream inlet to the fluid catalytic cracking unit regenerator or fluid coking unit burner based on oxygen purity specifications of the oxygen supply used for enrichment (percent by volume—dry basis)
- Hourly average percent CO concentration in the exhaust gas stream from the fluid catalytic cracking unit regenerator or fluid coking unit burner (percent by volume—dry basis)

Or:

- Volumetric flow rate of air to the fluid catalytic cracking unit regenerator or fluid coking unit burner, as determined from control room instrumentation (dscfh)
- Nitrogen (N₂) concentration in oxygen enriched gas stream inlet to the fluid catalytic cracking unit regenerator or fluid coking unit burner based on measured value or maximum N₂ impurity specifications of the oxygen supply used for enrichment (percent by volume – dry basis)
- Volumetric flow rate of oxygen enriched air to the fluid catalytic cracking unit regenerator or fluid coking unit burner, as determined from control room instrumentation (dscfh)
- Hourly average percent N₂ concentration in the exhaust gas stream from the fluid catalytic cracking unit regenerator or fluid coking unit burner (percent by volume—dry basis)

Methane and nitrous oxide emissions

Calculate emissions using either unit specific measurement data, a unit specific emission factor based on a source test of the unit, or default values provided in the rule.

For catalytic cracking units and traditional fluid coking units with rated capacities of 10,000 barrels per stream day or less (if you do not continuously or no less frequently than daily monitor the O₂, CO₂, and, if necessary, CO concentrations in the exhaust stack), measure these parameters...

Carbon dioxide emissions

- | | |
|--|--|
| <input type="checkbox"/> Annual throughput of unit from company records (barrels/yr) | <input type="checkbox"/> Carbon content of coke based on measurement or engineering estimate (kg C/kg coke) (default = 0.94) |
|--|--|

Methane and nitrous oxide emissions

Calculate emissions using either unit specific measurement data, a unit specific emission factor based on a source test of the unit, or default values provided in the rule.

For fluid coking units that use flexicoking design, measure these parameters...

Use methods described in 40 CFR 98, subpart C (General Stationary Combustion Sources) or monitor same parameters for traditional fluid coking units.

For catalytic reforming units, if you continuously or no less frequently than daily monitor the O₂, CO₂, and (if necessary) CO concentrations in the exhaust stack from the catalytic reforming unit catalyst regenerator prior to the combustion of other fossil fuels, calculate emissions following the requirements of catalytic cracking units with rated capacities greater than 10,000 barrels per stream day; otherwise, measure these parameters...

Carbon dioxide emissions

- | | |
|---|--|
| <input type="checkbox"/> Coke burn-off quantity per regeneration cycle from engineering estimates (kg coke/cycle) | <input type="checkbox"/> Number of regeneration cycles in year |
| <input type="checkbox"/> Carbon content of coke based on measurement or engineering estimate (kg C/kg coke); default = 0.94 | |

Methane and nitrous oxide emissions

Calculate emissions using either unit specific measurement data, a unit specific emission factor based on a source test of the unit, or default values provided in the rule.

For onsite sulfur recovery plants and for sour gas sent off site for sulfur recovery, measure these parameters...

Carbon dioxide emissions

- | | |
|---|--|
| <input type="checkbox"/> Volumetric flow rate of sour gas feed (including sour water stripper gas) to the sulfur recovery plant, from measurement if available, engineering calculations, or company records (scf/year) | <input type="checkbox"/> Mole fraction of carbon in the sour gas to the sulfur recovery plant, from measurement if available or engineering calculations (kg-mole C/kg-mole gas); default = 0.20 |
|---|--|

Non-Claus sulfur recovery units may alternatively elect to monitor:

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|---|--|
| <input type="checkbox"/> Number of venting events per year | <input type="checkbox"/> Venting time for the event (hours) |
| <input type="checkbox"/> Average volumetric flow rate of process gas during the event (scf/hour) [or this may me be determined from process knowledge or engineering estimates] | <input type="checkbox"/> Mole fraction of CO ₂ in process vent during the event (kg-mol GHG/kg-mol vent gas) [or this may me be determined from process knowledge or engineering estimates] |

For coke calcining units, measure these parameters...

Carbon dioxide emissions

- | | |
|---|--|
| <input type="checkbox"/> Annual mass of green coke fed to the coke calcining unit from facility records (metric tons/year) | <input type="checkbox"/> Annual mass of petroleum coke dust collected in the dust collection system of the coke calcining unit from facility records (metric ton petroleum coke dust/year) |
| <input type="checkbox"/> Average mass fraction carbon content of green coke from facility measurement data (metric ton C/metric ton green coke) | <input type="checkbox"/> Average mass fraction carbon content of marketable petroleum coke produced by the coke calcining unit from facility measurement data (metric ton C/metric ton petroleum coke) |
| <input type="checkbox"/> Annual mass of marketable petroleum coke produced by coke calcining unit from facility records (metric tons petroleum coke/year) | |

For uncontrolled asphalt blowing operations or asphalt blowing operations controlled by vapor scrubbing, measure these parameters...

Carbon dioxide emissions

- | | |
|--|--|
| <input type="checkbox"/> Annual quantity of asphalt blown (MMbbl/year) | <input type="checkbox"/> Emission factor for CO ₂ from uncontrolled asphalt blowing from facility-specific test data (metric tons CO ₂ /MMbbl asphalt blown); default = 1,100. |
|--|--|

Methane emissions

- | | |
|--|---|
| <input type="checkbox"/> Annual quantity of asphalt blown (MMbbl/year) | <input type="checkbox"/> Emission factor for CH ₄ from uncontrolled asphalt blowing from facility-specific test data (metric tons CH ₄ /MMbbl asphalt blown); default = 580 |
|--|---|

For controlled asphalt blowing operations, measure these parameters...

Carbon dioxide emissions

- | | |
|---|--|
| <input type="checkbox"/> Annual quantity of asphalt blown (MMbbl/year) | <input type="checkbox"/> Carbon emission factor from asphalt blowing from facility-specific test data (metric tons C/MMbbl asphalt blown); default = 2,750 |
| <input type="checkbox"/> Emission factor for CO ₂ from uncontrolled asphalt blowing from facility-specific test data (metric tons CO ₂ /MMbbl asphalt blown); default = 1,100 | |

Methane emissions

- | | |
|--|---|
| <input type="checkbox"/> Annual quantity of asphalt blown (MMbbl/year) | <input type="checkbox"/> Emission factor for CH ₄ from uncontrolled asphalt blowing from facility-specific test data (metric tons CH ₄ /MMbbl asphalt blown); default = 580 |
|--|---|

For delayed coking units, measure these parameters...

Methane emissions

- | | |
|--|---|
| <input type="checkbox"/> Total number of vessel openings for all delayed coking unit vessels of the same dimensions during the year | <input type="checkbox"/> Volumetric void fraction of coking vessel prior to steaming (cf gas/cf of vessel); default = 0.6 |
| <input type="checkbox"/> Height of coking unit vessel (feet) | <input type="checkbox"/> Diameter of coking unit vessel (feet) |
| <input type="checkbox"/> Gauge pressure of the coking vessel when opened to the atmosphere prior to coke cutting, or the gauge pressure of the coking vessel when depressurization gases are first routed to the atmosphere (psig) | <input type="checkbox"/> Mole fraction of methane in coking vessel gas (kg-mole CH ₄ /kg-mole gas); default = 0.01 |

For other process vents that exceed the volume percent thresholds provided in the rule, measure these parameters...

For each Greenhouse Gas

- | | |
|---|---|
| <input type="checkbox"/> Number of venting events per year | <input type="checkbox"/> Venting time for the event (hours) |
| <input type="checkbox"/> Average volumetric flow rate of process gas during the event (scf/hour) [or this may me be determined from process knowledge or engineering estimates] | <input type="checkbox"/> Mole fraction of each GHG in process vent during the event (kg-mol GHG/kg-mol vent gas) [or this may me be determined from process knowledge or engineering estimates] |

For uncontrolled blowdown systems, measure these parameters...

The same methods (and thus same parameters measured) to estimate emissions as “Other process vents” can be used. Alternatively the following parameters can be measured to calculate emissions in conjunction with other emission/conversion factors:

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|---|---|
| <input type="checkbox"/> Annual quantity of crude oil plus the quantity of intermediate products received from off site that are processed at the facility (MMbbl/year) | <input type="checkbox"/> Methane emission factor for uncontrolled blown systems (scf CH ₄ /MMbbl); default = 137,000 |
|---|---|

For equipment leaks, measure these parameters...

Process-specific CH₄ composition data (from measurement data or process knowledge) and any of the emission estimation procedures provided in the Protocol for Equipment Leak Emissions Estimates (EPA-453/R-95-017, NTIS PB96-175401), or estimate emissions by measuring the following...

- Number of atmospheric crude oil distillation columns at the facility
- Number of hydrogen plants at the facility
- Cumulative number of catalytic cracking units, coking units (delayed or fluid), hydrocracking, and full-range distillation columns (including depropanizer and debutanizer distillation columns) at the facility
- Number of fuel gas systems at the facility
- Cumulative number of hydrotreating/hydrorefining units, catalytic reforming units, and visbreaking units at the facility

For storage tanks (other than those processing unstabilized crude oil) that have a vapor-phase methane concentration of 0.5 volume percent or more, measure these parameters...

Tank-specific CH₄ composition data (from measurement data or product knowledge) and the AP-42 emission estimation methods provided in Section 7.1 of the AP-42: "Compilation of Air Pollutant Emission Factors, Volume 1: Stationary Point and Areas Sources", including the TANKS Model (Version 4.09D) or similar programs, or estimate emissions by measuring the following in conjunction with emission factor...

- Annual quantity of crude oil plus the quantity of intermediate products received from offsite that are processed at the facility (MMbbl/year)

For storage tanks that process unstabilized crude oil, measure these parameters...

Tank-specific CH₄ composition data (from measurement data or product knowledge) and direct measurement of the gas generation rate, or estimate emissions by measuring the following ...

- Annual quantity of unstabilized crude oil received at the facility (MMbbl/year)
- Mole fraction of CH₄ in vent gas from the unstabilized crude oil storage tank from facility measurements (kg-mole CH₄/kg-mole gas); default = 0.27 if measurement data are not available
- Pressure differential from the previous storage pressure to atmospheric pressure (psi)

For crude oil, intermediate, or product loading operations for which the equilibrium vapor-phase concentration of CH₄ is 0.5 volume percent or more, measure these parameters...

- Product-specific, vapor-phase CH₄ composition data (from measurement data or process knowledge) and the emission estimation procedures provided in Section 5.2 of the AP-42: "Compilation of Air Pollutant Emission Factors, Volume 1: Stationary Point and Area Sources"

What Must Be Monitored if Using a CEMS?

For catalytic cracking units or fluid coking units, in addition to the Tier 4 Calculation Methodology and associated requirements specified in 40 CFR 98, subpart C (General Stationary Fuel Combustion Sources), monitor these parameters if applicable...

- Fuel use in the CO boiler or other post-unit combustion device

For sulfur recovery plants, in addition to the Tier 4 Calculation Methodology and associated requirements specified in 40 CFR 98, subpart C (General Stationary Fuel Combustion Sources), monitor these parameters...

- Fuel use in the Claus burner, tail gas incinerator, or other combustion sources that discharge via the final exhaust stack from the sulfur recovery plant

For coke calcining units, in addition to the Tier 4 Calculation Methodology and associated requirements specified in 40 CFR 98, subpart C (General Stationary Fuel Combustion Sources), monitor these parameters...

- Fuel use in the coke calcining unit that discharges via the final exhaust stack from the coke calcining unit

See also the information sheet for Petroleum Refineries at:
www.epa.gov/climatechange/emissions/downloads/infosheets/petroleumrefineries.pdf.