

GREEN CATALYTIC PROCESSES: SUBSTITUTION OF VOLATILE LIQUID ACIDS WITH SOLID ACIDS

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Pollution Prevention through Nanotechnology Conference

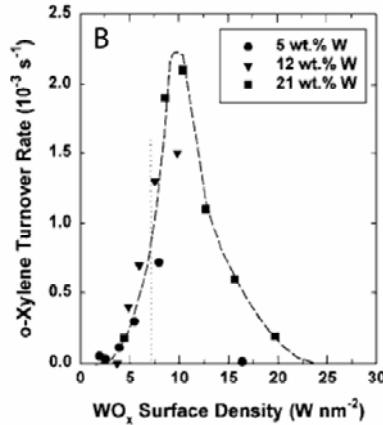
GREEN CATALYTIC PROCESS: SUBSTITUTION OF VOLATILE LIQUID ACIDS WITH SOLID ACIDS

- **Alkylation of n-Alkanes with Liquid Acids (H_2SO_4 , HF, $AlCl_3$, HCl, etc.) is Employed to Synthesize Antiknock Components for Motor Fuel**
- **Strong Acids Required for Alkane Isomerization Step**
 - Isomerization Step: Conversion of n-Alkanes to Branched Alkanes
 - Alkylation Step: Reaction of Branched Alkanes with Olefins
- **Technical Problems Associated with Liquid Phase Alkylation**
 - Corrosion
 - Volatility
 - Spills
- **Strong Solid Acid Can Potentially Replace Liquid Acids**
 - No Corrosion
 - No Volatility
 - No Spills

SOLID WO_3 - ZrO_2 CATALYSTS IDENTIFIED AS STRONG SOLID ACIDS

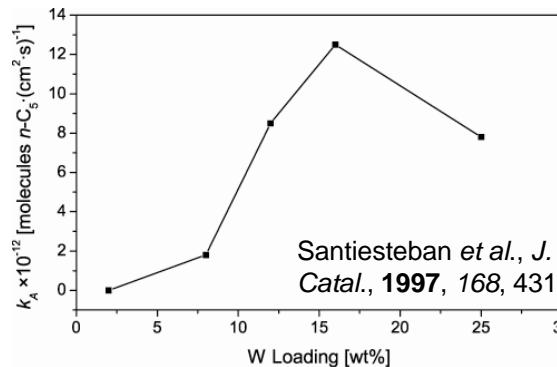
Iglesia & coworkers (UC-Berkeley)

Santiesteban & coworkers (ExxonMobil)

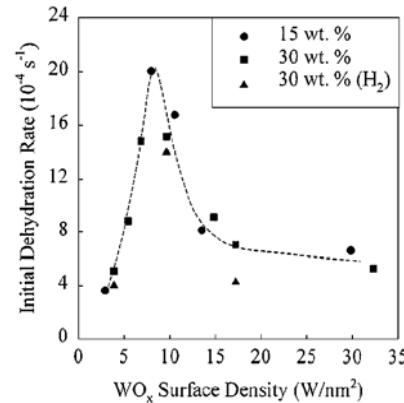


- o-xylene isomerization
- IW impregnation $\text{WO}_3\text{-ZrO}_2$
- 250 °C
- ~1 bar
- Excess H_2 feed

Barton et al., J. Catal., 1999, 181, 57



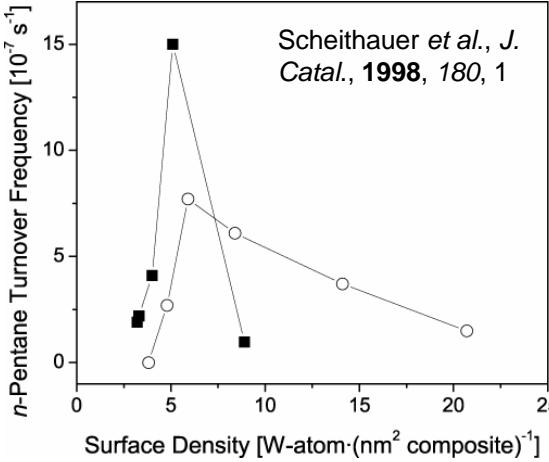
- n -pentane isomerization
- coprecipitated $\text{WO}_3\text{-ZrO}_2$
- 210 °C
- 24 bar
- 2 H_2 :1 $n\text{-C}_5$ molar feed ratio



- 2-butanol dehydration
- IW impregnation $\text{WO}_3\text{-ZrO}_2$
- 100 °C
- ~1 bar
- Excess H_2 feed

Baertsch et al., J. Catal., 2002, 205, 44

Knözinger & coworkers (U. of München)

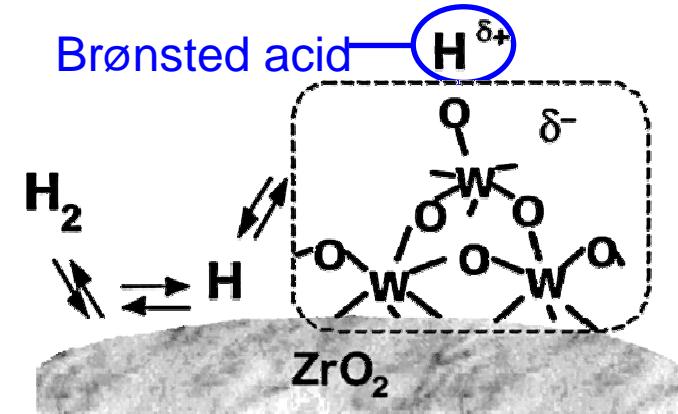


- n -pentane isomerization
- equilibrium adsorption $\text{WO}_3\text{-ZrO}_2$
- 250 °C
- ~1 bar
- Pure $n\text{-C}_5$ feed

- High Surface Acid Activity Occurs at Intermediate WO_x Content

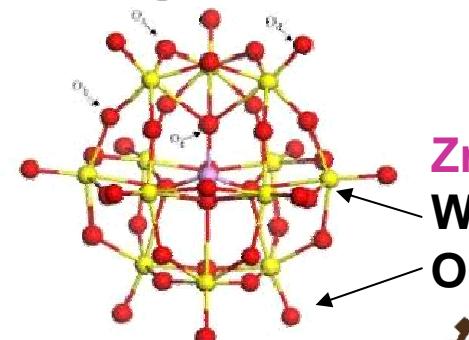
PROPOSED MODELS FOR ENHANCED ACIDITY OF SUPPORTED $\text{WO}_3/\text{ZrO}_x(\text{OH})_{4-2x}$ CATALYTS

- Surface Polytungstate $\text{W}^{+(6-n)}$ Domains (Surface WO_x Monolayer)

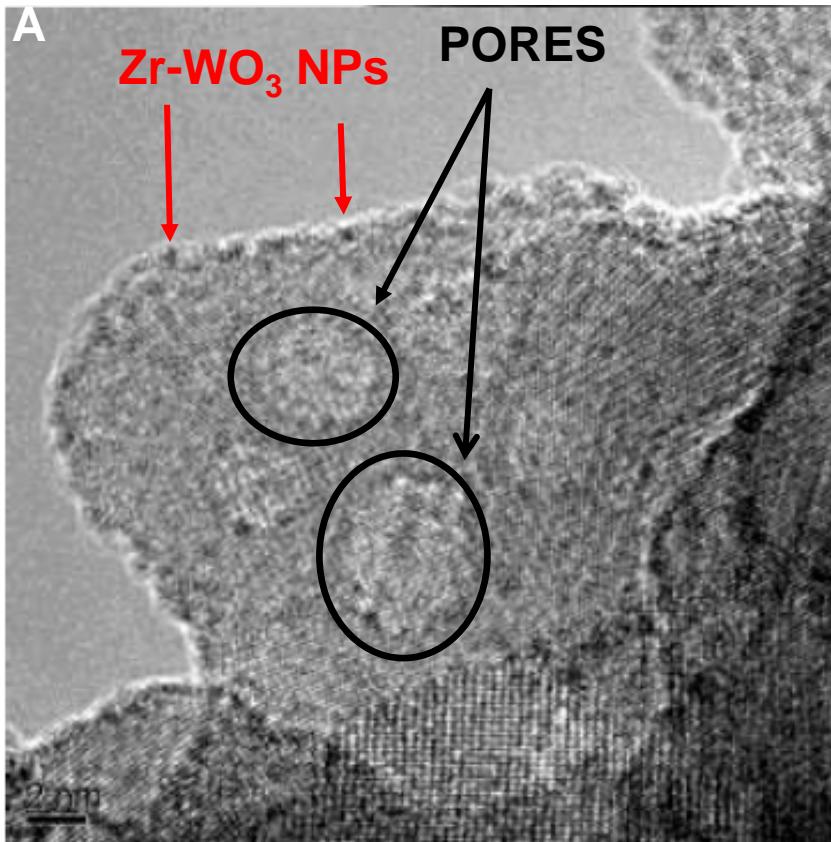


Baertsch *et al.*, *J. Phys. Chem. B*, 2001, 105, 1320

- Polytungstate Domains Containing Zr Cations (Keggin-like structure)

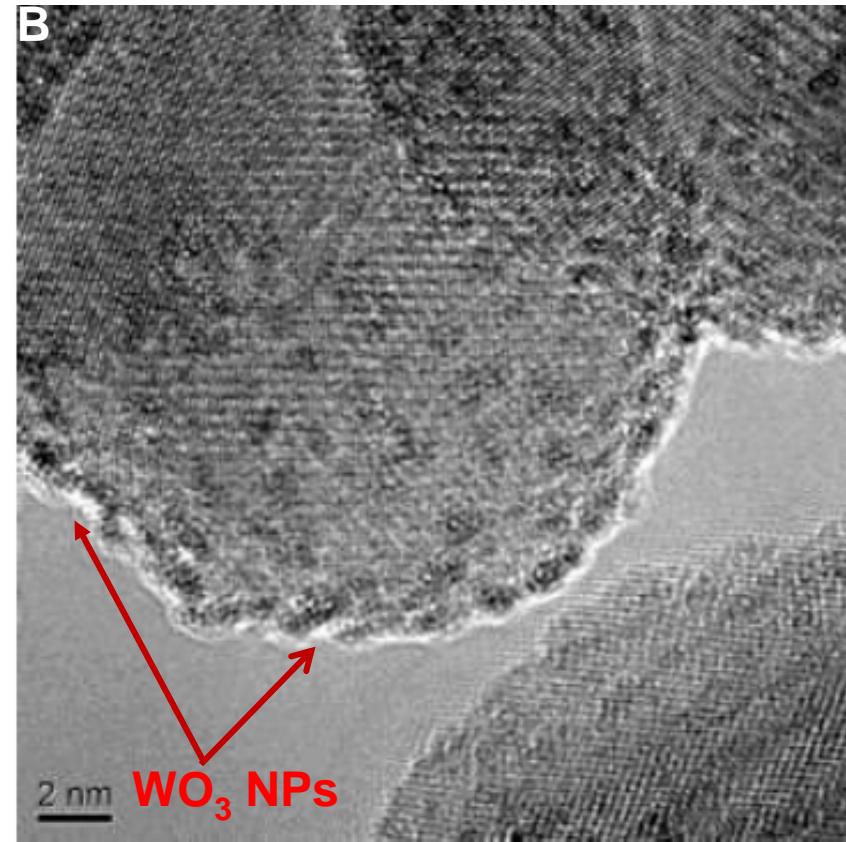


Zr-STABILIZED POORLY ORDERED WO_3 NPs RESPONSIBLE FOR STRONG ACID SITES



[A] 10.1WZrOH-1073(6.2)

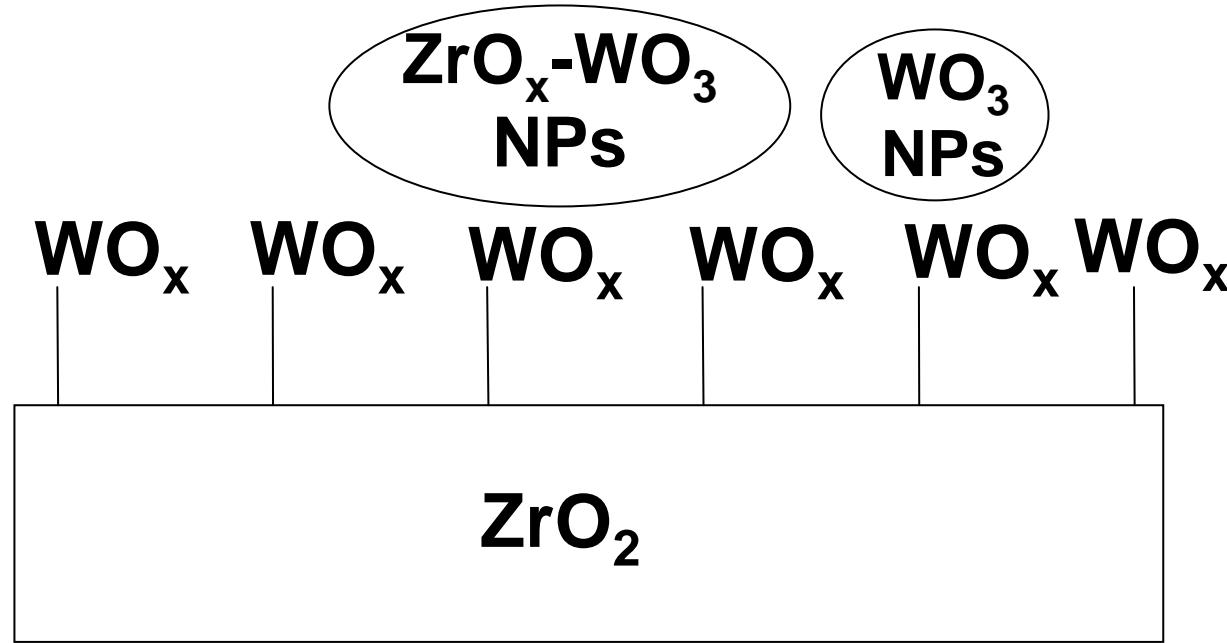
- Surface WO_x Monolayer
- Poorly Ordered Zr-WO₃ NPs (~0.6 nm)
- Strong Acid Sites



[B] 19.5WZrOH-1173(20.2)

- Surface WO_x Monolayer
- Crystalline WO₃ NPs (~1.2 nm)
- Modest Acid Sites

CATALYTIC ACTIVE SITES PRESENT IN SUPPORTED WO_3/ZrO_2 CATALYSTS



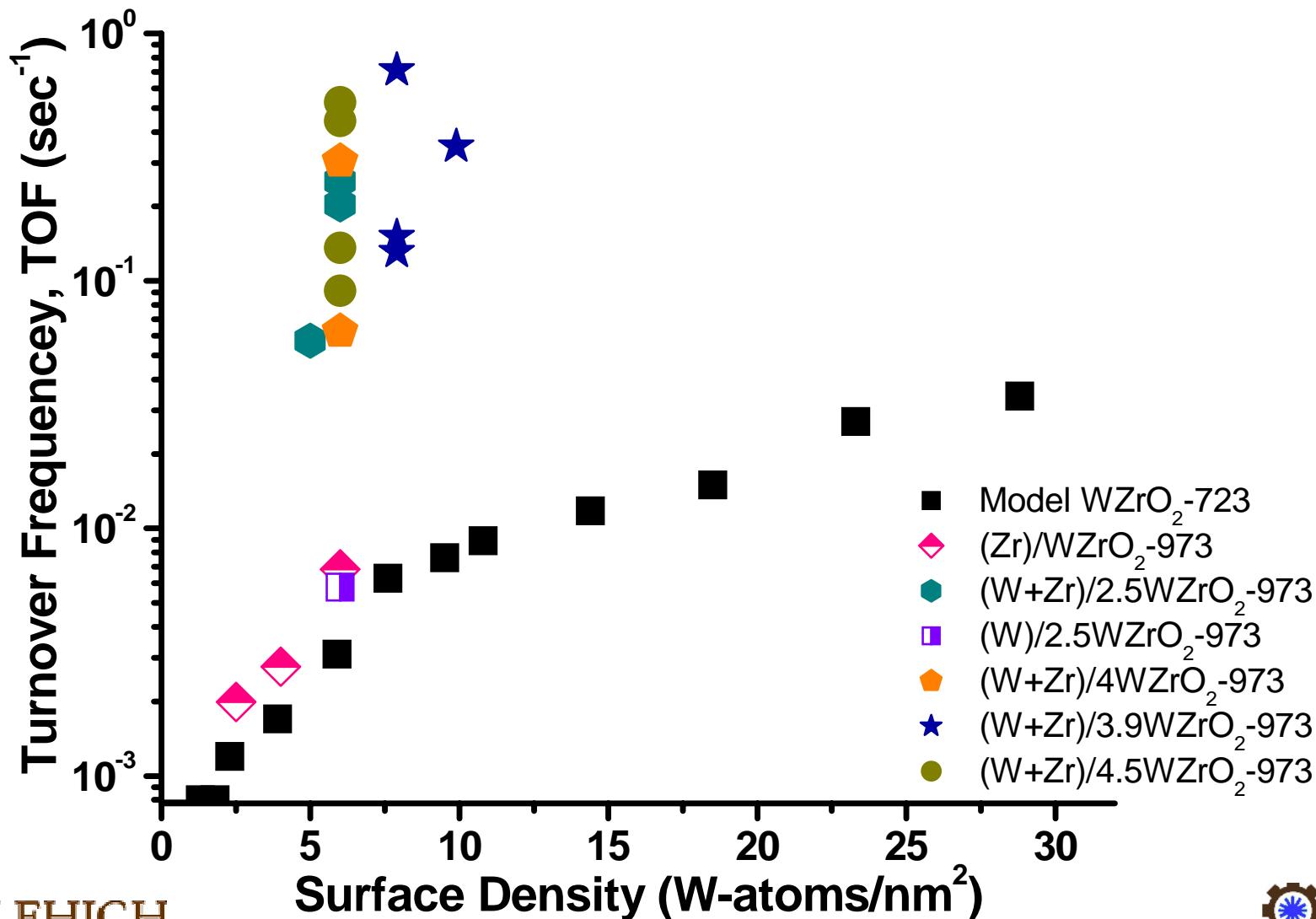
**Surface WO_x Species &
*Zr-Stabilized WO_3 NPs & WO_3 NPs***

CATALYST BY DESIGN:

ENHANCE SOLID ACIDITY WITH MORE Zr-WO₃ NPs

- Catalyst Synthesis
 - Aqueous Solutions of $(\text{NH}_4)_{10}\text{W}_{12}\text{O}_{41} \cdot 5\text{H}_2\text{O}$
 - Toluene Solutions of $\text{Zr}[\text{OC}(\text{CH}_3)_3]_4$
- Support Material: Model WO_3/ZrO_2 Catalysts
- Calcined at 973 K for 4 hr in Air

POORLY ORDERED Zr-STABILIZED WO₃ NPs RESPONSIBLE FOR ENHANCED PERFORMANCE CATALYTIC ACTIVE SITES



CONCLUSIONS

- *Poorly Ordered Zr-Stabilized WO_3 NPs Responsible for Strong Acidic Catalytic Active Sites*

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C.J. Kiely – Lehigh University (HR-TEM)
M. Neurock – University of Virginia (Theory)