



Evaluating the Air Quality, Climate & Economic Impacts of Biogas Management Technologies

California Bioresources Alliance

11th Annual Symposium

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Today's presentation

- The Opportunity
- The Conundrum
- Our Goals
- Technologies
- Scope and Methods
- Results
 - Efficiency
 - Costs
 - Emissions
 - Technical Conclusions
- Conclusions

The Opportunity

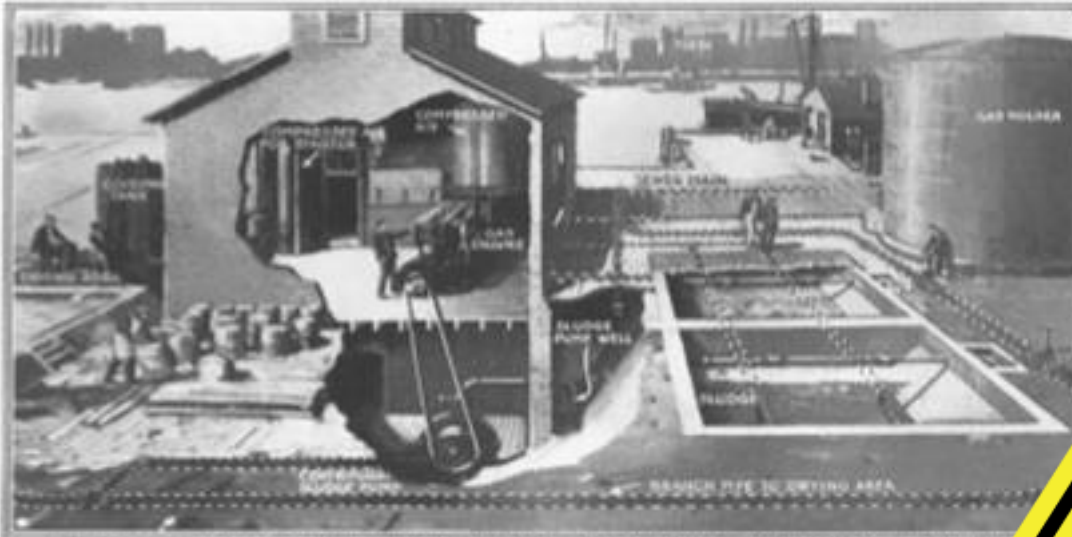
Feedstock	Amount Technically Available	Biomethane Potential (billion cubic feet)	Million gasoline gallon equivalent (GGE)
Animal Manure	3.4 MM BDT	19.7	170
Landfill Gas	106 BCF	53	457
Municipal Solid Waste (food, leaves, grass fraction)	1.2 MM BDT	12.6	109
Water Resource Recovery Facility (WRRF)	11.8 BCF (gas)	7.7	66
Total		93	802

The Opportunity

March, 1922

67

Gas from Sewage Waste Runs City Power Plant



How the sewage disposal plant at Birmingham, England, supplies its own power is described in the illustration. From the sewage drives an engine of 20 brake horsepower, which operates a centrifugal sludge pump.

SEWAGE that costs large cities tremendous sums each year can be turned into a source of power equivalent to thousands of tons of coal! The waste now dumped into rivers or shipped to sea may be used to run factories or to light buildings!

That conversion of sewage into power is possible has been proved conclusively by the city of Birmingham, England. There a suction gas engine of 20 brake horsepower has been successfully driven by the gases given off by sewage sludge.

On the basis of the Birmingham experiments, an American city that must now

pay for the disposal of 400,000 tons of sewage sludge a year might produce 320,000,000 cubic feet of gas suitable for heat and power, or, in terms of energy, 18,000,000 horsepower hours at 20 cubic feet per brake horsepower.

The apparatus for producing gas from sewage consists of two sludge digestion tanks in which the sewage is allowed to ferment. The gases given off are composed of from 25 to 75 per cent of methane, or marsh gas.

A gas engine of the usual type will run on sewage gas without adjustment of the

valves. Sewage gas has a calorific value than some illuminating gas, being about 650 thermal units, as against 500.

The Birmingham engine runs 24 hours a day and is used to operate a centrifugal sludge pump that moves the wet sludge from the gas-generating tank to the drying grounds. In this process a small proportion of the waste material produces enough power to run the pumps of the sewage disposal plant. If all the material were used, there would probably be enough gas available to light the city.

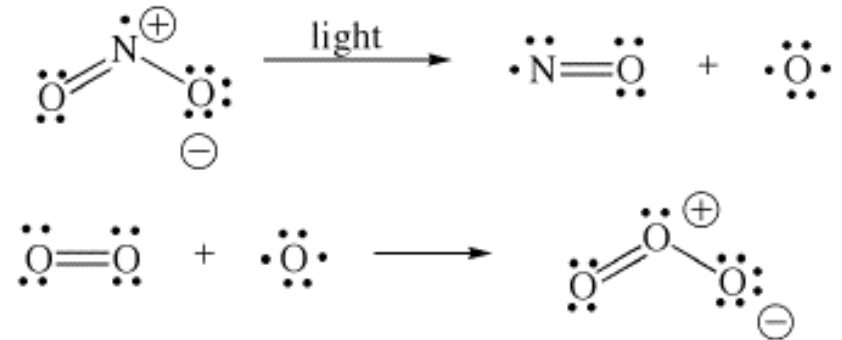


**MICROBES
AT
WORK**

The Conundrum



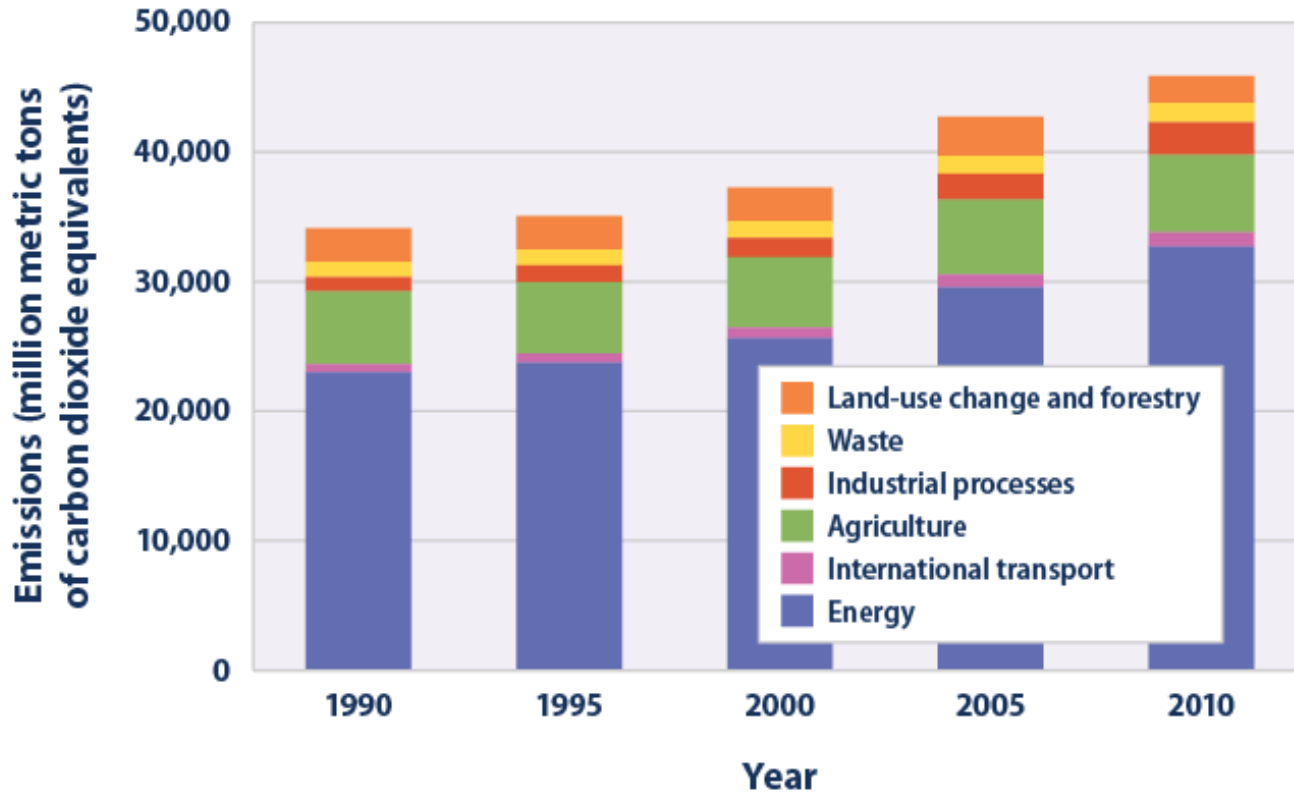
- Sunlight, Oxygen, and $\text{No}_x \rightarrow$ “bad” ozone



- ½ of CA counties — where 80% of Californians live — exceed ozone NAAQS

The Conundrum

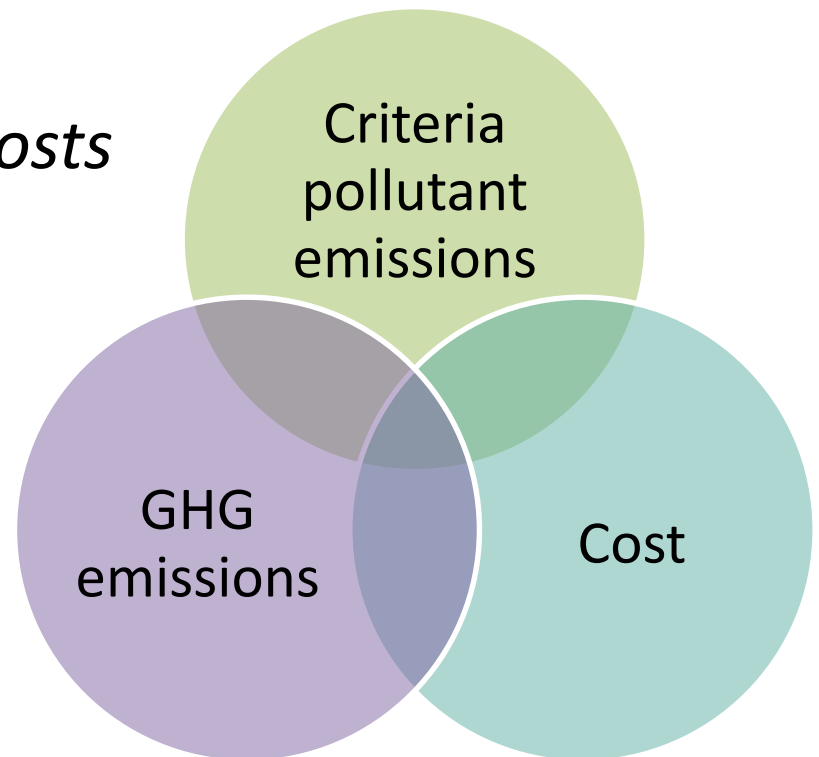
Global Greenhouse Gas Emissions by Sector, 1990–2010



- Energy production & use = largest source of GHGs
- Biogas is **biogenic**, w/ a smaller carbon footprint

Our Goals

- EPA Strategic Plan's #1 goal:
 - *Address climate change **and** improve air quality*
- Report's goals:
 - *Compare emissions and costs*
 - *Identify options*
 - *Engage stakeholders*
 - *Move us forward*



Project Goals

- Inform organic waste managers and regulators
- Compare cost and performance of biogas utilization technologies
 - Efficiency
 - Cost of energy
 - Criteria pollutant emissions
 - Greenhouse gas (GHG) emissions

Technologies

- Reciprocating engines
- Gas turbines
- Microturbines
- Fuel cells
- Processing to create Renewable Compressed Natural Gas Vehicle Fuel (RNG / CNG)
- Processing for pipeline injection
- Flaring

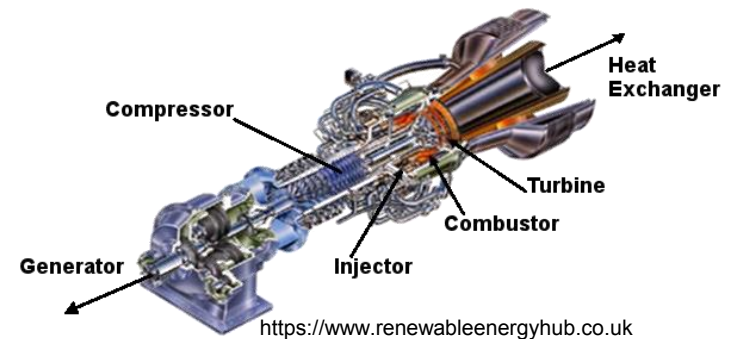
Reciprocating Engines

- Also known as: Reciprocating Internal Combustion Engines (RICE)
- RICE is a piston engine (i.e., reciprocating)
 - Intermittent combustion of fuel-air mixture to
 - create mechanical energy that is
 - converted to electricity by a generator.
- Used extensively throughout the world for stationary power generation
- Size ranges from < 100 kW to several MW.



Gas Turbines (or combustion turbines)

- Similar to jet engines but optimized to produce shaft power (rather than high velocity exhaust gas).
- Fuel is burned continuously with compressed air.
- Hot exhaust gases expand through a turbine to create mechanical energy that is converted to electricity by generator.
- Gas turbine-generator size ranges about 1 to 500 MW.



Mark McDannel, LA County San

Microturbines

- Small gas turbines
- available in capacities ranging from 30 kW to 333 kW
- Combine units to achieve up to several megawatt (MW) facility size.



<http://www.shebovanwto.com/>



<http://www.agenziauniklima.it/>

Fuel Cells

- Use hydrogen and oxygen to produce direct current power through an electrochemical process, rather than combustion-to-mechanical energy process.
- Biogas methane (CH_4) is reformed to make hydrogen available for the fuel cell.
- Systems available from <100 kW to several MW.



Jeff Wall, Moreno Valley Regional WRF



<http://www.fuelcellenergy.com/>

Processing for pipeline injection

- Biogas must be “upgraded” to biomethane, which generally requires:
 - removing trace contaminants and water from biogas and then
 - separating carbon dioxide (CO₂) from methane
- Methane portion is then compressed and injected to the natural gas system
- Finished gas must meet pipeline owner specifications



Könnern, Germany (Harasek, 2011)

Processing to create Renewable Compressed Natural Gas Vehicle Fuel (RNG /CNG)

- Processing system is similar to creating pipeline quality gas:
 - Remove trace contaminants, water and CO₂
- Product must meet vehicle fuel standards (which may or may not be different than pipeline quality standards).
- Biomethane product is compressed and can be used like CNG vehicle fuel.



Flare

- Method for methane (biogas) disposal when other utilization technologies are not practical or economic.
- Methane converted to CO_2 and water vapor by burning in a flare.



www.johnzink.com



hulsdairy.com/

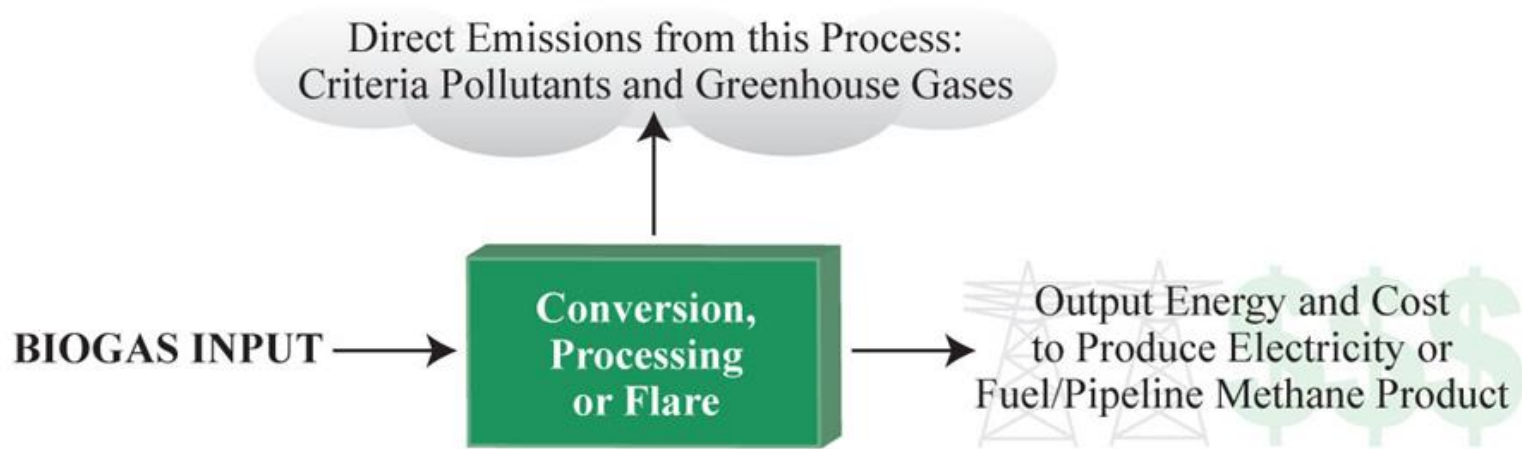
Scope and Methods

- Evaluated on-site use (conversion or upgrading) of already-produced biogas

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- Conversion efficiency:
 - % energy efficiency for electricity production systems, higher heating value basis
 - % yield for renewable CNG and pipeline injection processes
- Costs
 - Levelized Cost of Energy (LCOE) [output basis]
 - Cost to process biogas [input basis]
 - Includes biogas pre-treatment and emissions control costs
- On-site criteria air pollutant and GHG emissions

Scope and Methods



- Limited Scope – starts with existing biogas.
- Does not include the costs and emissions associated with biogas production, & other upstream and downstream processes.
- It is not a full system or life-cycle emissions accounting.

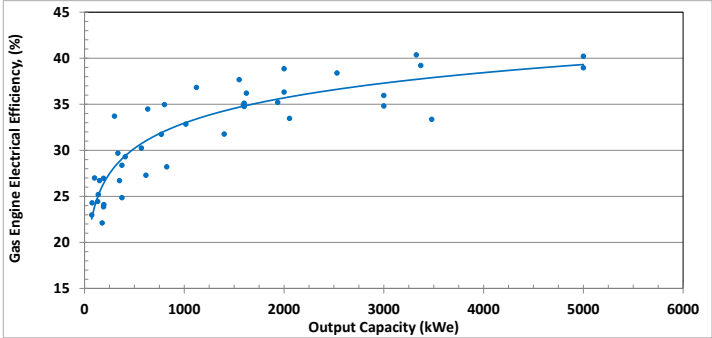
Scope and Methods

Source information included

- peer-reviewed and 'gray' literature,
- operating permits,
- source test reports and
- expert and developer interviews.

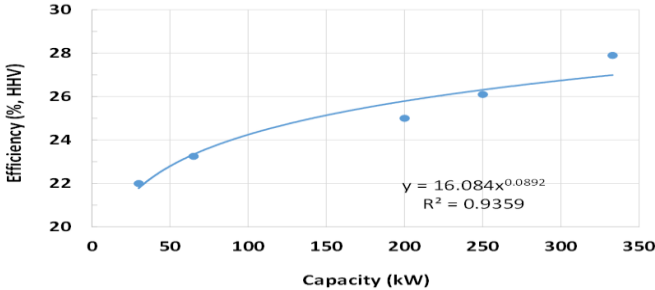
Efficiencies

Reciprocating Engine



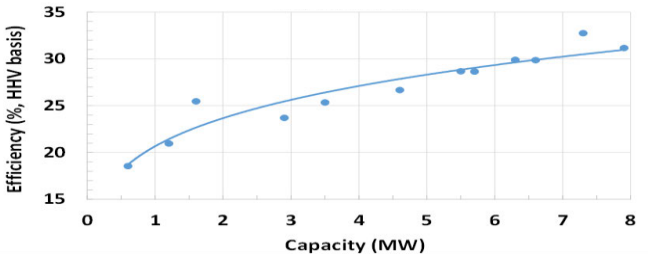
Sources: (ICF 2012, Rutgers 2014, Caterpillar 2015)

Microturbine



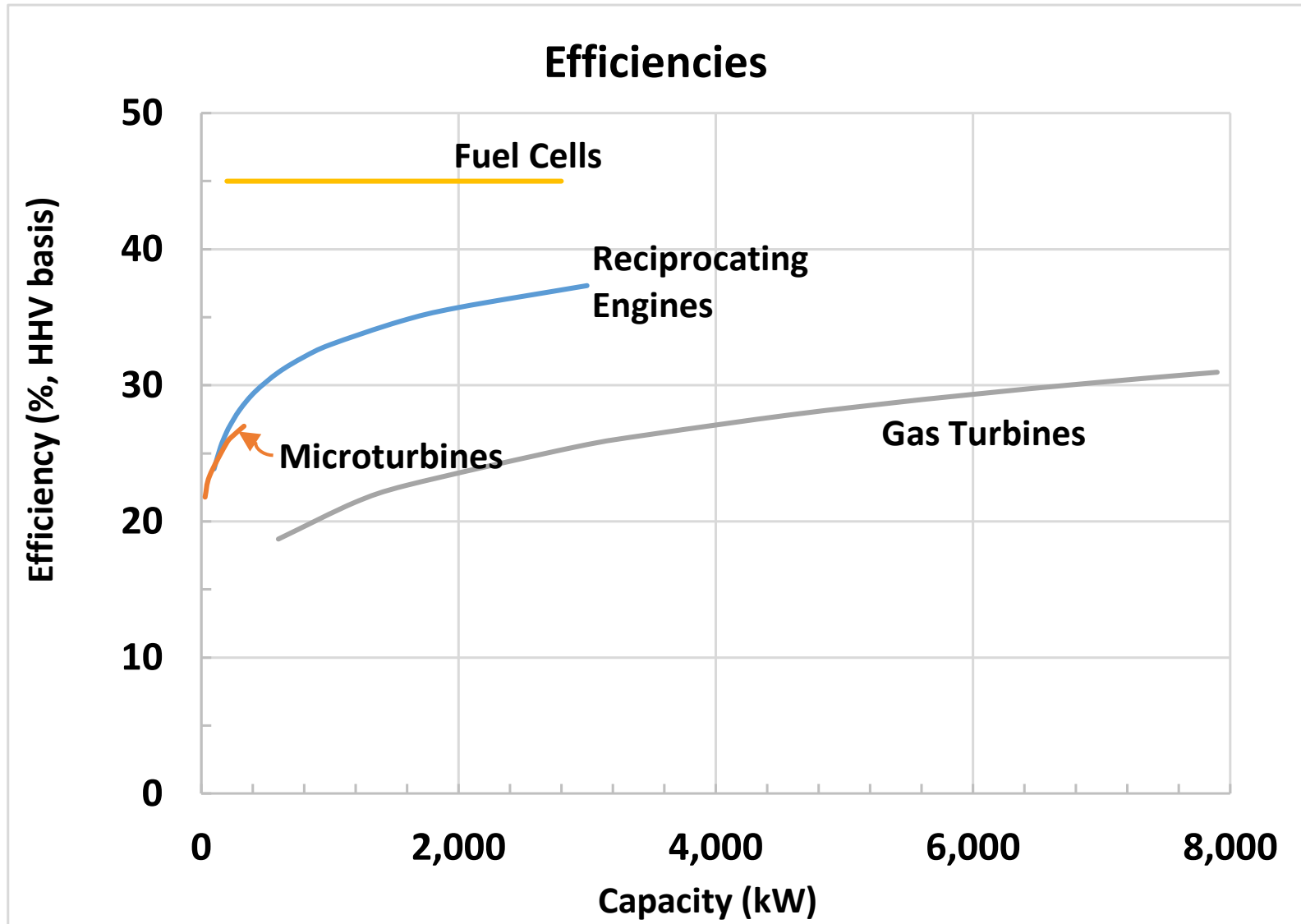
Sources: (Itron 2011, Darrow et al., 2015, FlexEnergy)

Gas Turbine



Sources: (Itron 2011, Solar Turbines 2015, Kawasaki Gas Turbines 2015)

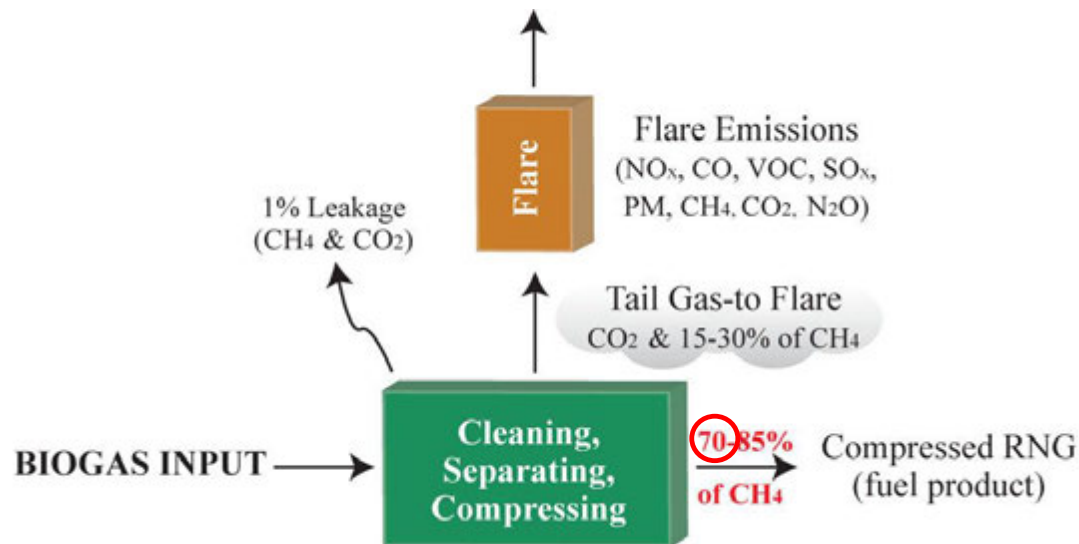
Electricity producing technologies compared



RNG/CNG Biomethane “Yield”

Biogas Flow Input (SCFM) *	Methane Recovery or “Yield” (%)	RNG Fuel Product Output (GGE / day) *	Separation Technology	Source Information
50 - 200	70	240 - 965	Single-pass membrane	BioCNG

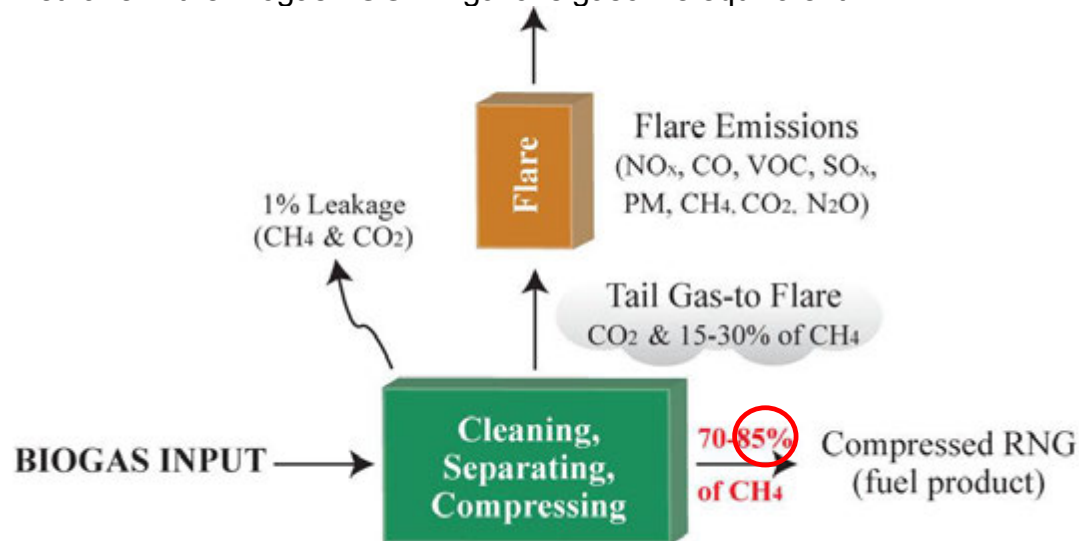
* Assumes 60% methane in the Biogas. GGE = gallons gasoline equivalent



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1600	85	9,360	Pressure Swing Adsorption	Guild, Santos, Grande et al. 2011, Wu, Zhang et al. 2015

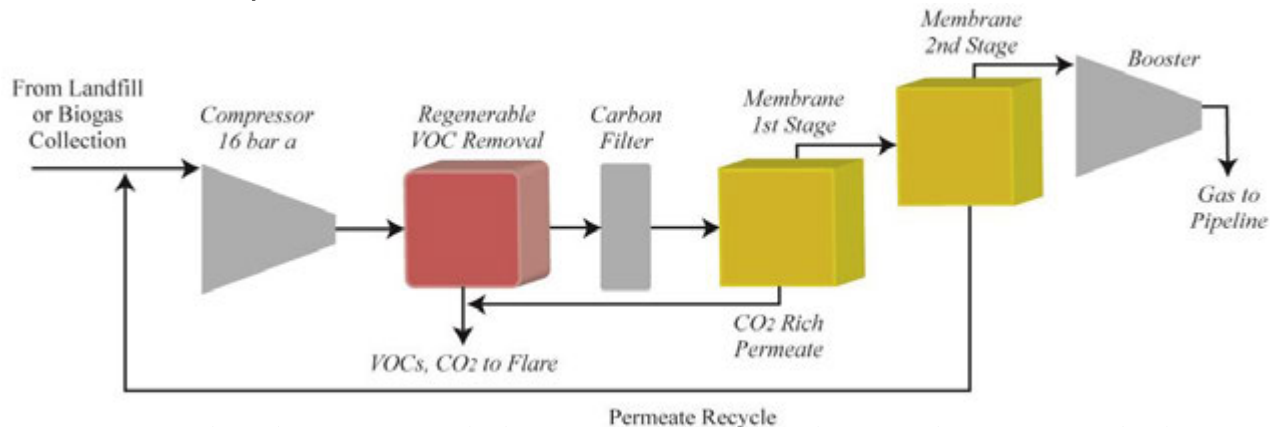
* Assumes 60% methane in the Biogas. GGE = gallons gasoline equivalent



Upgrade & Pipeline Injection

Biomethane “Yield”

- Achievable methane recovery for commercial upgrading technologies is reported to be as high as 96-99%.*
- Facility at Point Loma, California reportedly recovers 85-87% of input methane in the upgrading system (an Air Liquide two-stage permeable membrane system) [Frisbie, 2015]
- Our analysis assumed 90% methane recovery to final product (which needs to have energy content of 990 Btu ft⁻³, or 98% methane concentration)



Adapted from Air Liquide: <http://www.medal.airliquide.com/en/biogaz-systems.html>

* (Petersson and Wellinger 2009, Ryckebosch, Drouillon et al. 2011, Bauer, Hulteberg et al. 2013, IEA 2014)

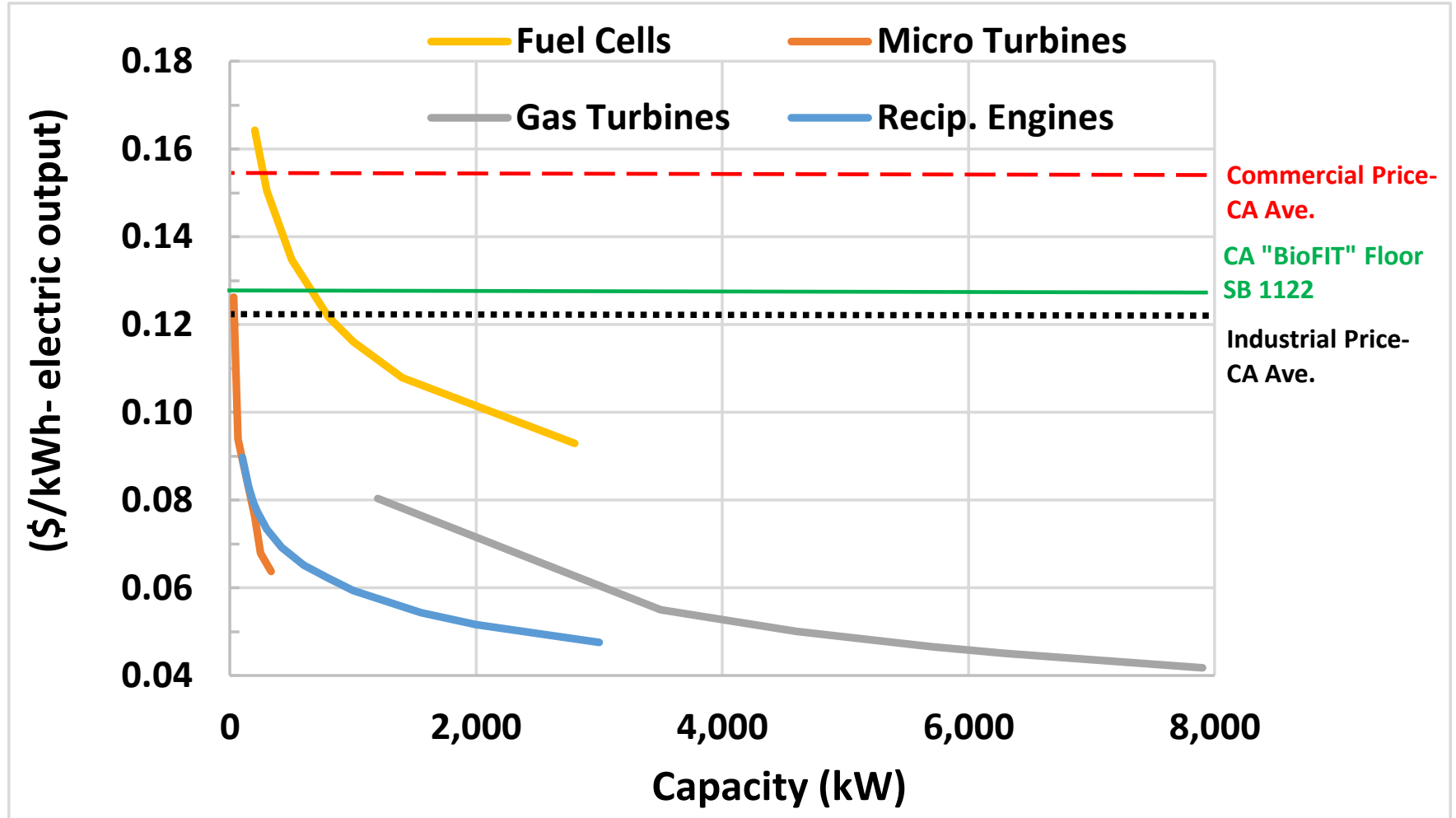
Cost of Energy

- Capital and operating costs taken from literature and discussions with developers;
- Reflects California costs or “cost adders” above U.S. average
- Includes costs for
 - raw biogas cleanup (H_2S and siloxane reduction)
 - air pollution control (APC) equipment for reciprocating engines and gas turbines; APC is presumed **not needed** for microturbines, fuel cells, fuel and pipeline pathways, and flares
- RNG / CNG pathway cost includes on-site fueling equipment
- The upgrade to pipeline injection pathway includes interconnection or injection costs.

Levelized Cost of Energy (LCOE)

- The LCOE represents the required revenue per unit of energy for the project to break even.
- In this analysis, $LCOE = \text{Total Annual Cost} \div \text{Annual Energy Produced}$
 - \$/kWh (electricity systems),
 - \$/gallon-gasoline equivalent (\$/GGE) for RNG/CNG systems,
 - \$/MMBtu for pipeline injection systems & RNG/CNG
- Capital costs were amortized over 20 years at 6% annual interest
- Recall scope starts with existing biogas so biogas has **ZERO** cost in our financial model (the biogas production is already paid for)
- If the biogas did not yet exist, e.g., a digester needed to be built, then the LCOE would be higher

LCOE Comparison –Electricity Systems



RNG/CNG Fuel Cost Estimate

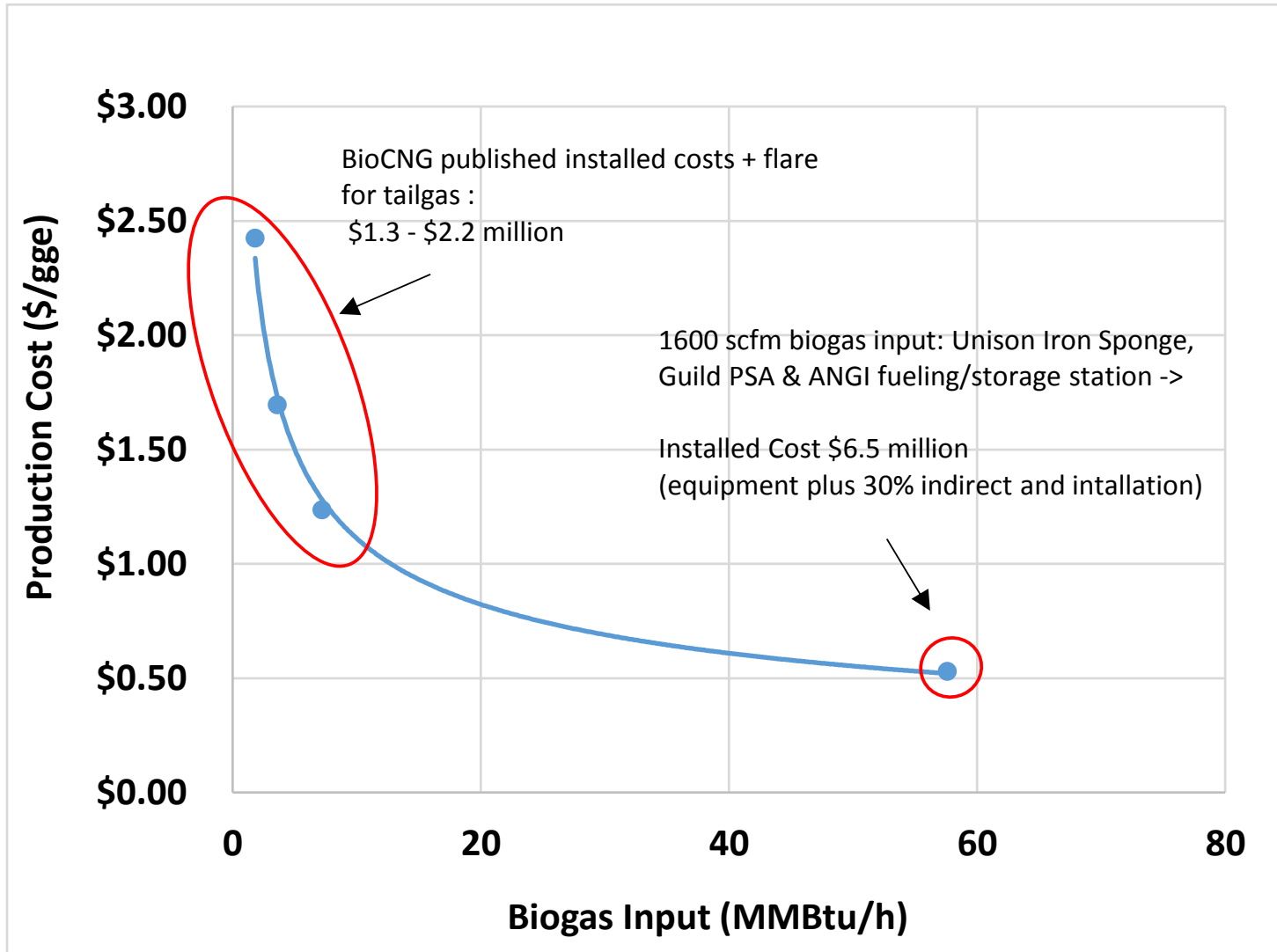
Input- (scfm biogas) ²	Fuel Output (GGE/day)	RNG Equipment Cost (MM \$) ¹	Flare Cost (\$) ³	Total Capital (\$)	Annualized Capital (\$/y) ⁴	O&M CNG (\$/GGE) ¹	CNG O&M (\$/y)	O&M (CNG + Flare) (\$/y)	\$/GGE	\$/MMBtu (output)
50	240	1.2	69,800	1,270,000	111,000	1.06	88,000	91,000	\$2.42	\$18.30
100	480	1.5	116,000	1,620,000	141,000	0.82	137,000	142,000	\$1.69	\$12.79
200	960	2.0	192,000	2,190,000	191,000	0.64	214,000	221,000	\$1.23	\$9.34
1600	9400	6.54	511,000	7,050,000	615,000	0.34	1,090,000	1,110,000	\$0.53	\$4.02

Sources and Notes:

1. Based on BioCNG project sheets, conference presentations, Geosyntec report to Flagstaff Landfill and personal communication, Jay Kemp and Christine Polo, Black and Veatch. 70% methane recovery for single-pass membrane system (BioCNG 50-200 scfm input) and 85% methane recovery for PSA system (1600 scfm input).
2. 60% methane in biogas.
3. Tailgas (methane slip) is flared in this scenario. Added flare capital and operating costs using data from flare scenario.
4. 6% APR, 20-year financing of capital - \$0.12/kWh electricity cost.

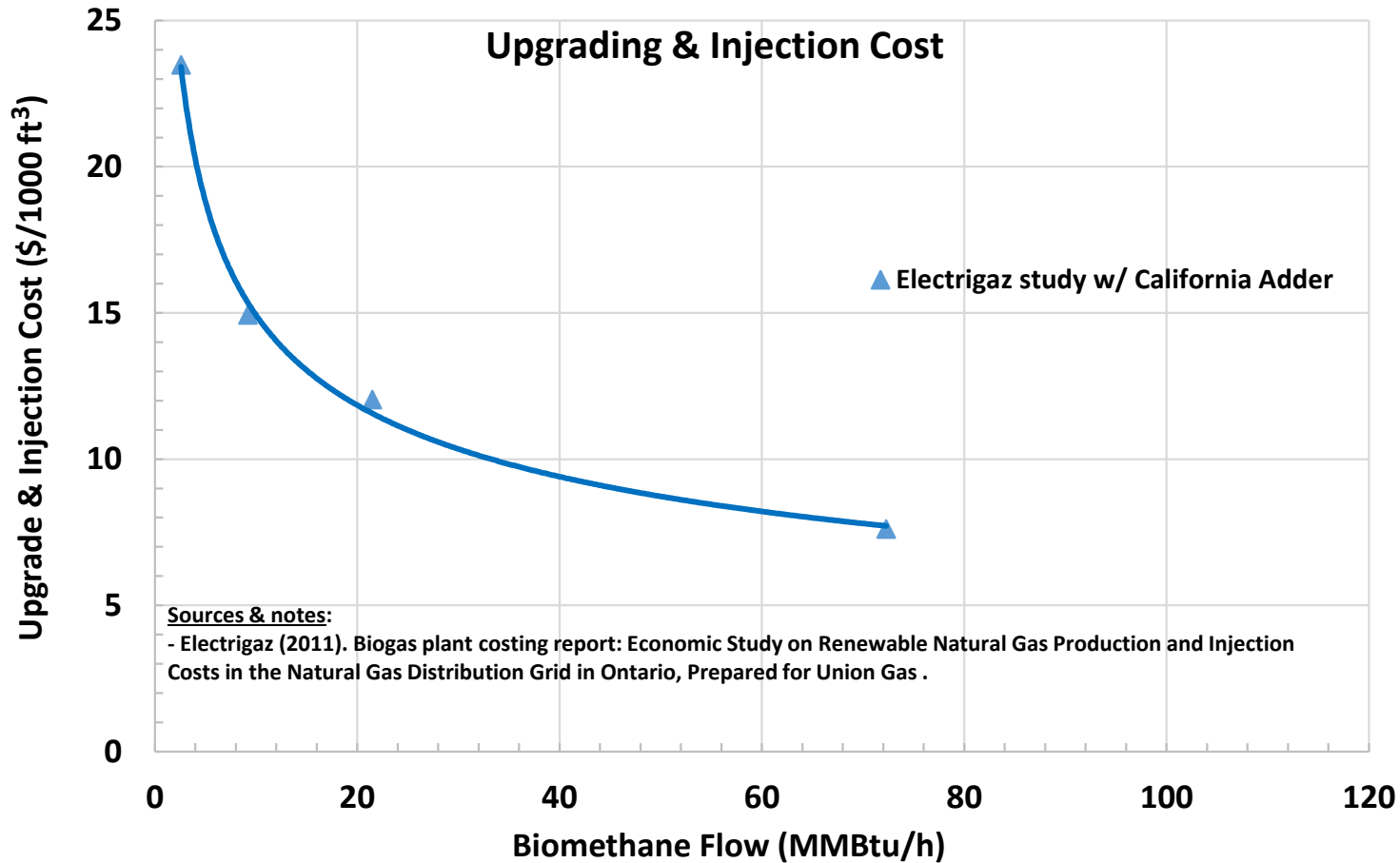
GGE = gallon gasoline equivalent

RNG/CNG Cost Estimate

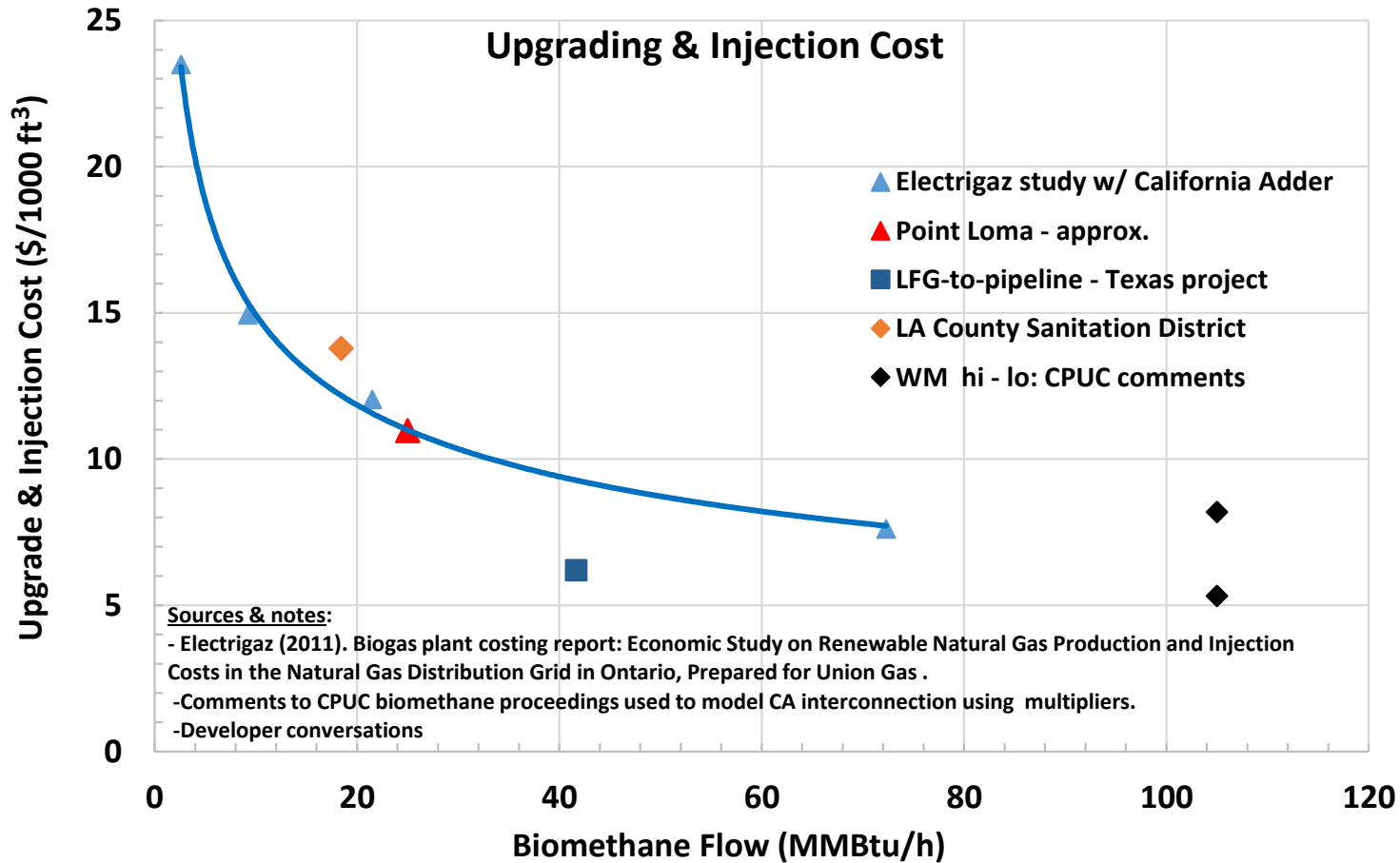


GGE = gallon gasoline equivalent

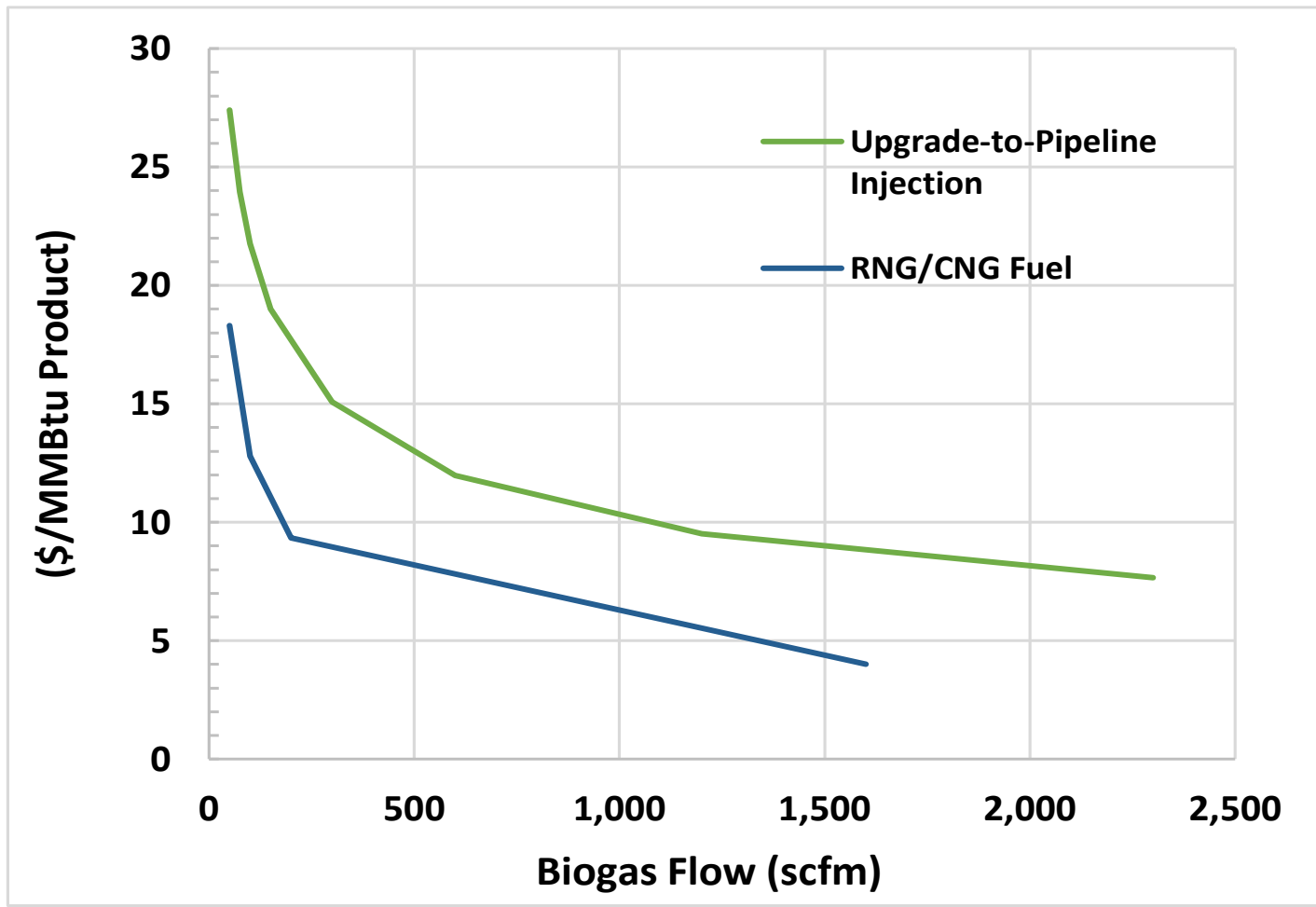
Upgrading & Injection Cost



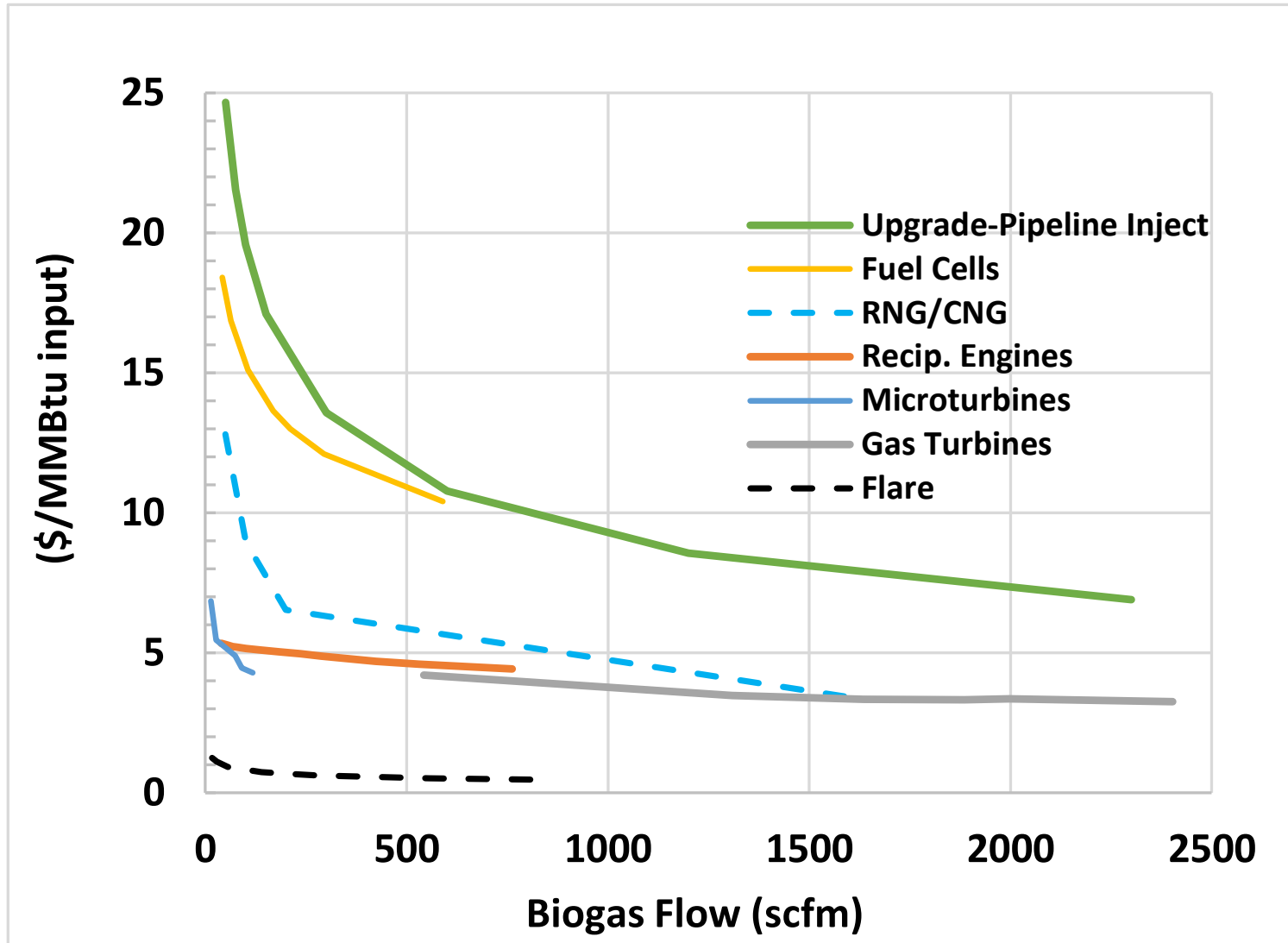
Upgrading & Injection Cost



Pipeline Injection & RNG/CNG



Cost to process Biogas – All technologies shown



Criteria Pollutants

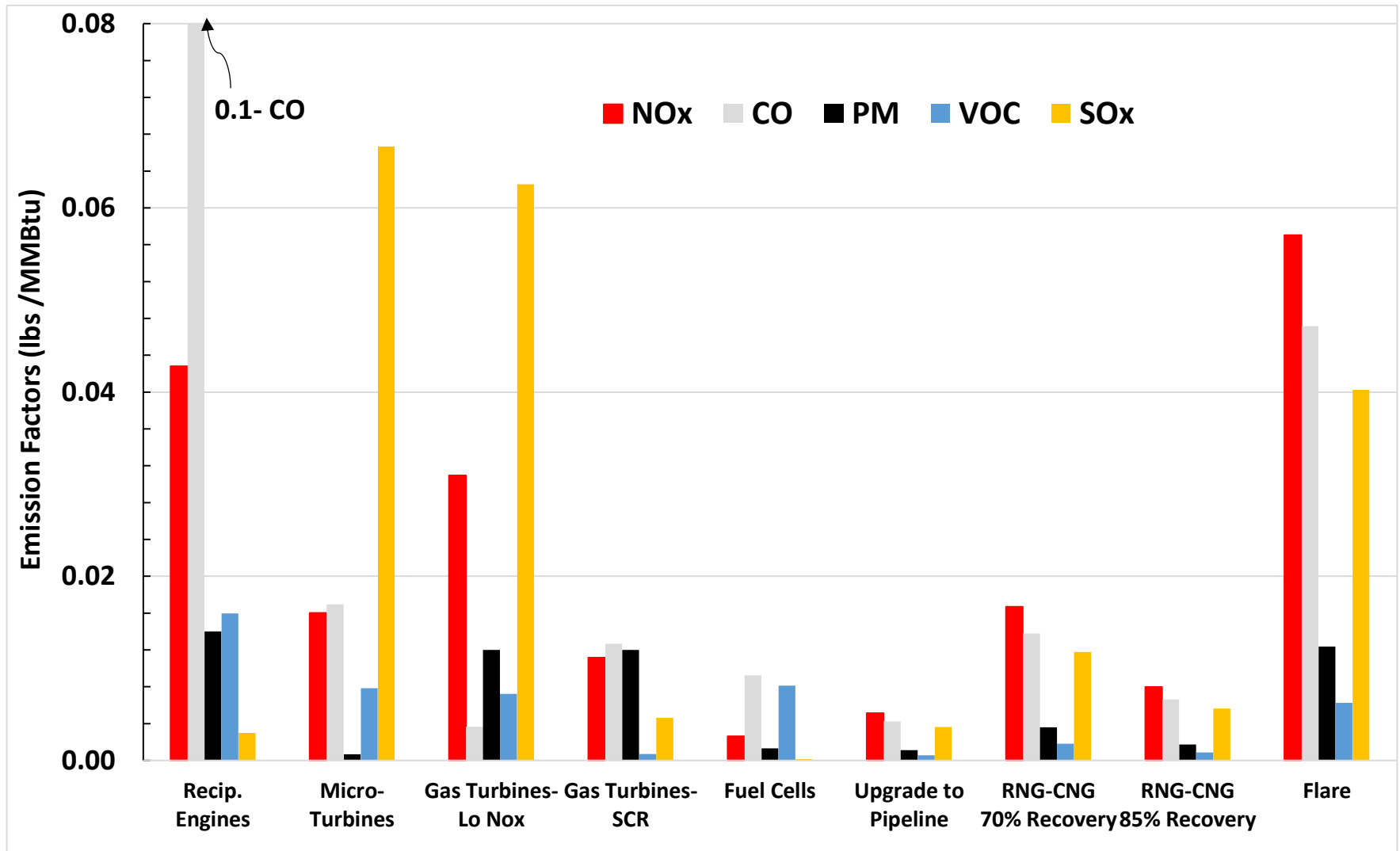
- Nitrogen Oxides (NO_x), Carbon Monoxide (CO), Volatile Organic Compounds (VOC), Sulphur Oxides (SO_x), and Particulate Matter (PM)
- Reviewed a large number of air permits and source tests
- Used 54 source tests to develop some emission factors

Application*	No. of Source Tests Reviewed	Biogas Source Type	Source Test Air District
Reciprocating Engine	35	6 @ Landfill, 26 @ WRRF, 3 @ Dairy Digester	<ul style="list-style-type: none"> – South Coast – Bay Area – San Joaquin Valley – Yolo-Solano – Mojave Desert
Microturbine	4	1 @ WRRF, 3 @ Food Waste Digester	<ul style="list-style-type: none"> – South Coast – Bay Area
Combustion Turbine	10	5 @ Landfill, 5 @ WRRF	<ul style="list-style-type: none"> – South Coast – Bay Area – San Joaquin Valley
Fuel Cells	3 (2 permits)	3 @ WRRF	<ul style="list-style-type: none"> – South Coast – San Joaquin Valley
Flare	4	1 @ Landfill, 3 @ WRRF	<ul style="list-style-type: none"> – South Coast – San Joaquin Valley

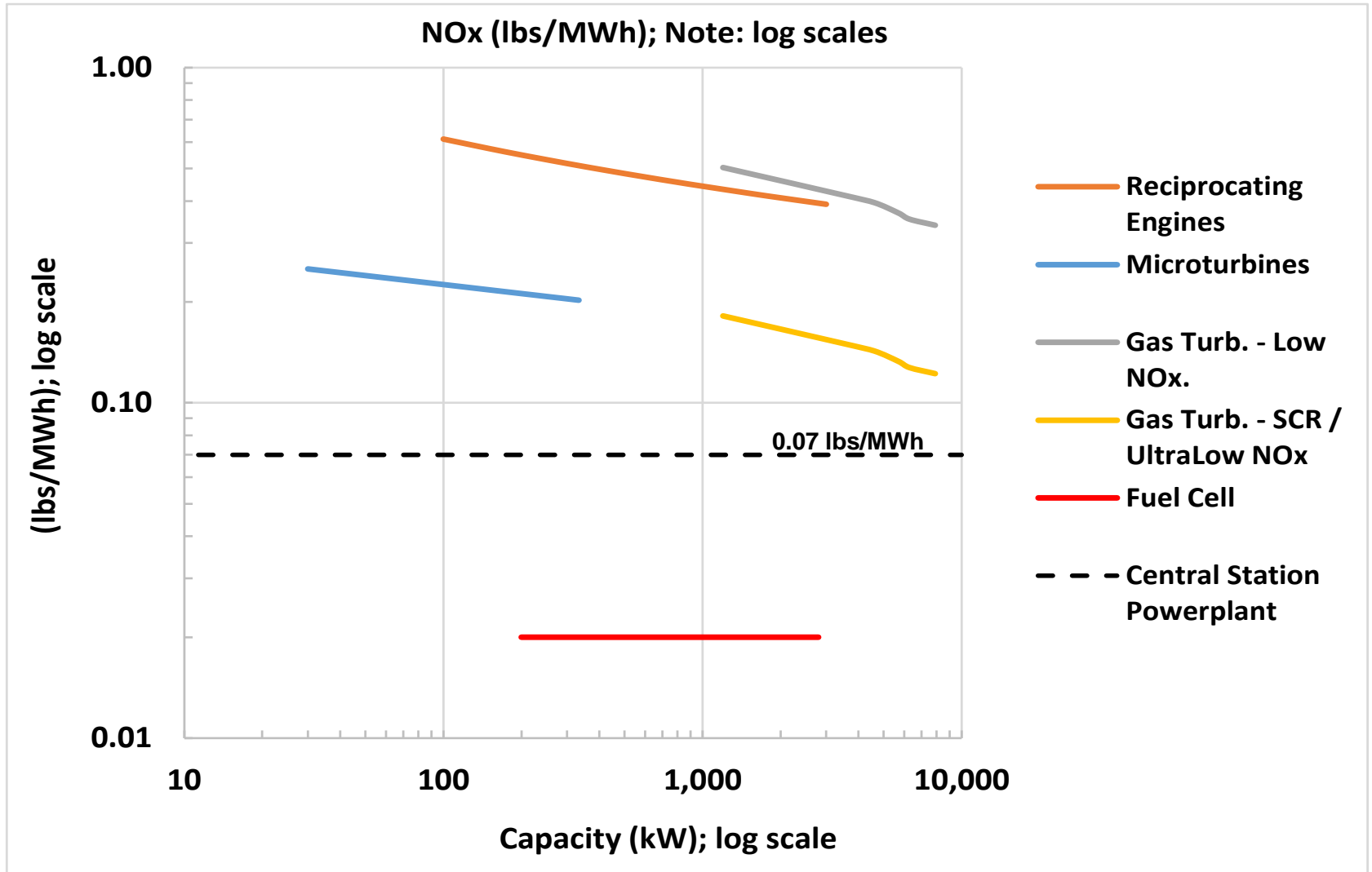
Criteria Pollutants

- Emission Factors:
 - Pounds of pollutant per MMBtu of biogas **input** (lb/MMBtu)
- Reciprocating Engines
 - NO_x: Emission factor is based on the South Coast Air Quality Management District (SCAQMD) Rule 1110.2 (11 ppm NO_x)
 - VOC, SO_x & CO: Based on source test results with SCR NO_x control and catalytic oxidation (CatOx) exhaust treatment
 - PM: From US EPA AP-42
- Microturbines, Combustion Turbines and Flares
 - Source Test Results plus AP-42 for some PM
- Fuel cell emissions are based on permit values and one source test report
- RNG/CNG and Pipeline Quality Gas (Biomethane)
 - Emission factors are based on flaring the tailgas, a process byproduct gas which contains some methane that needs to be destroyed.
 - Downstream emissions from use of biomethane (fuel or pipeline gas) are not included

Emission Factors by Technology (lbs/MMBtu input)



Output Based NOx Emissions (lbs/MWh)



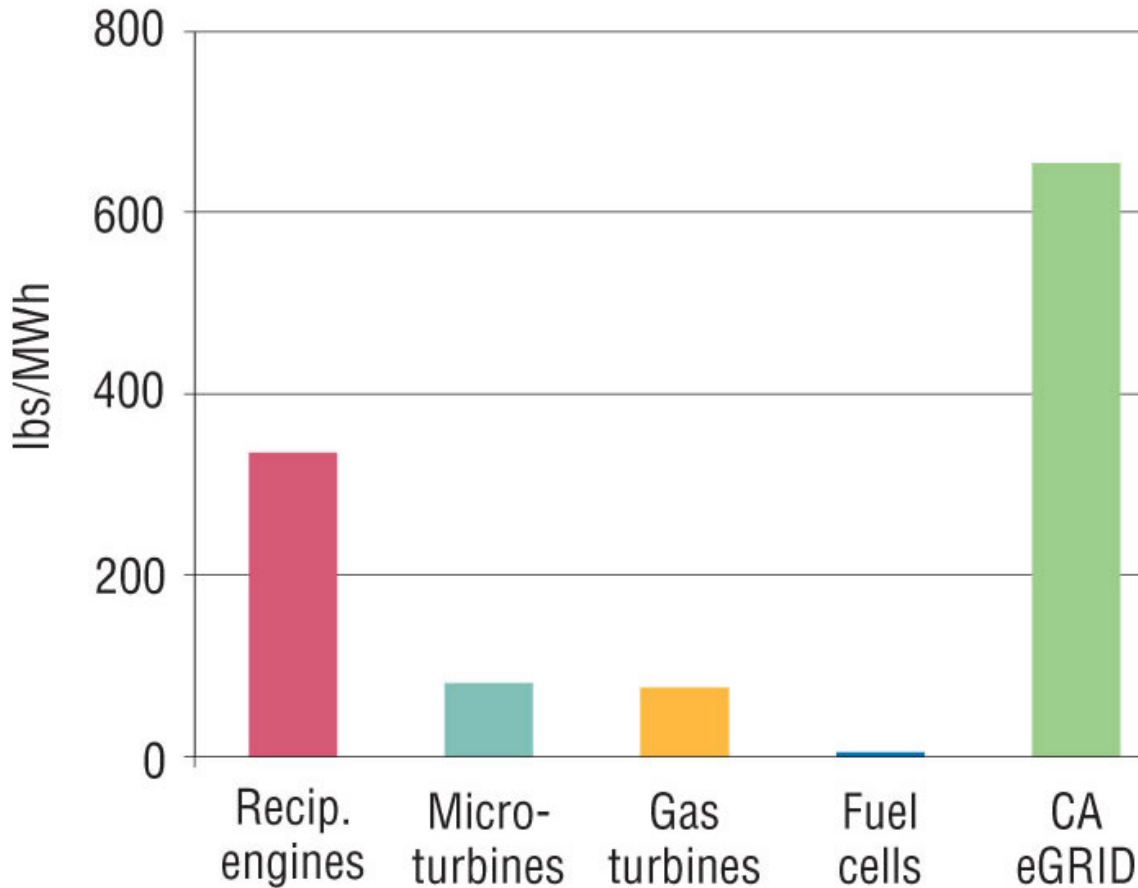
GHG Emissions

- Evaluated:
 - Methane (CH_4)
 - Nitrous Oxide (N_2O)
 - Carbon Dioxide (CO_2)
- Methane Emissions (methane “Slip” & fugitive)
 - 0.2 – 2.0% Methane Slip (or unburned methane) from combustion devices (engines, gas turbines, flares)
 - 1% Fugitive Methane loss (leaks) from processing & upgrading systems (pipeline injection and RNG/CNG) was assumed (Han, Mintz et al. 2011)
- N_2O emissions are taken from source-specific literature when found or default factors from IPCC Guidelines
- CO_2 emissions are calculated based on stoichiometric (or complete) combustion of biogas
 - For biogas with 60% methane content, the CO_2 emission factor is 191.3 lb/MMBtu

GHG Emission Factor Summary

Technology	GHG Emission Factor (lb/MMBtu)			Notes
	CH ₄	N ₂ O	CO ₂	
Recip. Engines	0.838	1.92E-03	191.3	Average of SCS (2007) & Mintz (ANL), N ₂ O & ~ 97.99% CH ₄ destruction efficiency (2% slip).
Micro-Turbines	0.167	2.56E-04	191.3	Average SCS (2007) & CAR (2011): CH ₄ 99.6% destruction efficiency, N ₂ O Emission Factor from Table 2.2 in 2006 IPCC Guidelines.
Gas Turbines	0.167	2.56E-04	191.3	Average SCS (2007) & CAR (2011): CH ₄ 99.6% destruction efficiency, N ₂ O Emission Factor from Table 2.2 in 2006 IPCC Guidelines.
Fuel Cell	0.003	2.56E-04	191.3	CH ₄ & N ₂ O Emission Factor from 2006 IPCC Guidelines.
Flare	0.07	2.43E-03	191.3	Mintz et al., (2010) CH ₄ 99.8% destruction efficiency, N ₂ O also from Mintz (2010).
RNG/CNG (70% recovery)	0.437	7.03E-04	106.5	1% CH ₄ leakage in upgrade process + flare emissions from tailgas combustion. No vehicle or downstream combustion emissions included.
RNG/CNG (85% recovery)	0.427	3.40E-04	88.3	
Upgrade-Injection	0.436	2.18E-04	86.1	

CO₂eq emissions for the bio-power technologies & CA eGRID



- California electricity grid carbon footprint values (CA eGRID) are from (USEPA 2012)
- Biogenic CO₂ emissions are not counted in eGRID (neutral in eGRID)
- Only CH₄ and N₂O emissions from biopower are converted to CO₂eq here

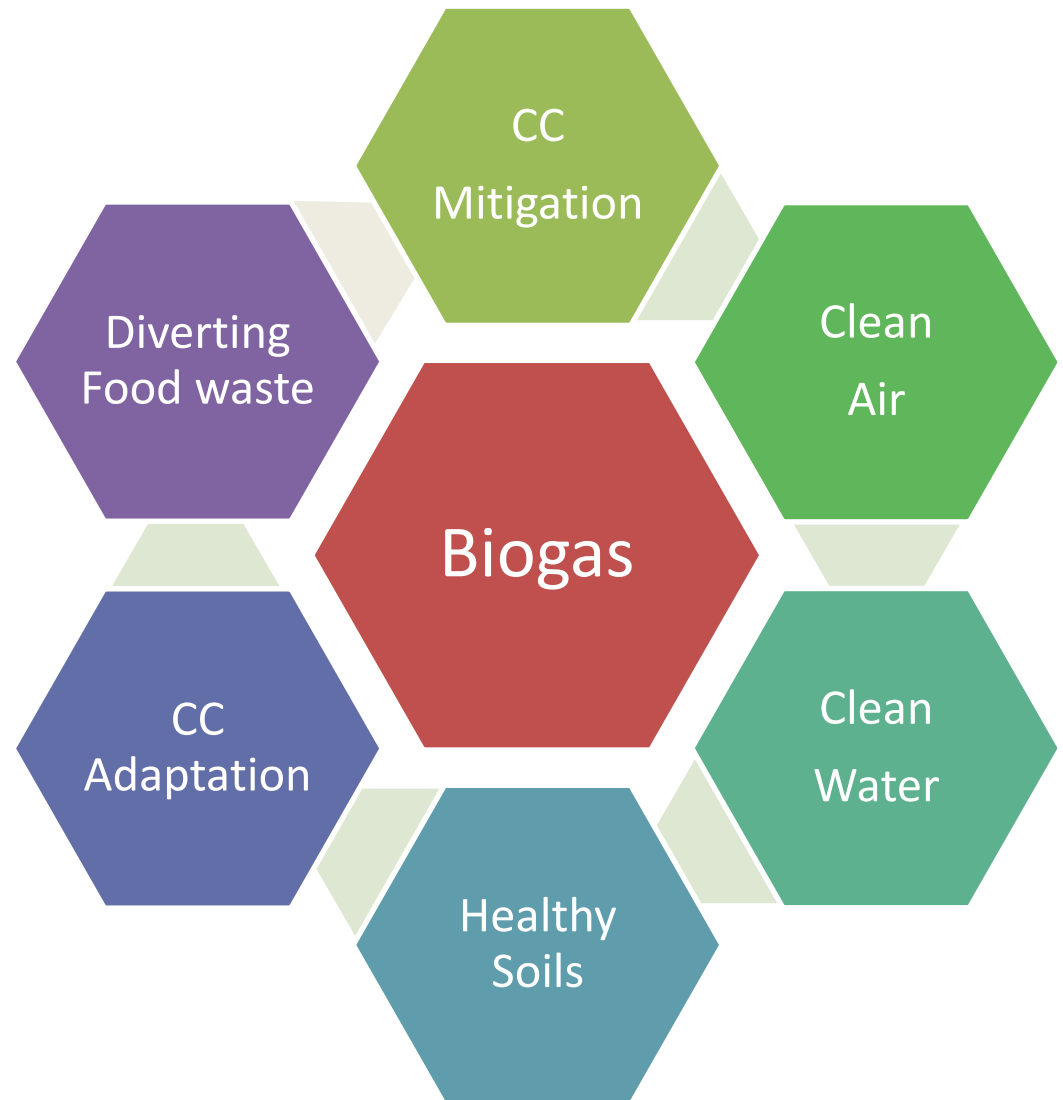
GWP₁₀₀ : CH₄ = 34, N₂O = 298, CO₂ = 1

Technology Summary

- Examined seven biogas utilization technologies
- Evaluated and compared
 - Cost and performance
 - Criteria pollutants
 - Greenhouse gas emissions
- See EPA report, EPA/ORD/R-16/099, for details (link not yet available- email Rob Williams for copy : rbwilliams@ucdavis.edu)

Conclusions

- Additional research needed:
 - Sources of biogas
 - Geography
 - Offsetting costs
 - Net enviro. benefit
- What did we do?
 - Baseline



Thank you

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