#### Reducing Emissions from Compressor Seals

Lessons Learned from Natural Gas STAR



#### **Transmission Technology Transfer Workshop**

Duke Energy Gas Transmission Interstate Natural Gas Association of America (INGAA) and EPA's Natural Gas STAR Program

**September 22, 2004** 

#### **Compressor Seals: Agenda**

Methane Losses
Methane Recovery
Is Recovery Profitable?
Industry Experience
Discussion Questions



## Methane Losses from Transmission and Storage

 Transmission and storage sector responsible for 96 billion cubic feet (Bcf) in methane emissions



#### Methane Losses from Compressor Seals



## **Compressor Seals** What is the problem?

- Compressor seals account for 13% of natural gas industry emissions
  - Over 45,000 compressors in the natural gas industry
  - Over 8,500 compressors in gas transmission sector



## Methane Losses from Reciprocating Compressors

- Reciprocating compressor rod packing leaks some gas by design
  - Newly installed packing may leak 60 cubic feet per hour (cf/h)
  - Worn packing has been reported to leak up to 900 cf/h



#### Reciprocating Compressor Rod Packing

- A series of flexible rings fit around the shaft to prevent leakage
- Leakage still occurs through nose gasket, between packing cups, around the rings and between rings and shaft



# Gas STAR Partners Reduce Emission with Economic Rod Packing Replacement

#### **Decision Process**





### Methane Recovery Through Economic Rod Packing Replacement

- Step 1: Monitor and record baseline leakage and rod wear
  - Establishing baseline leak rates and monitoring rod wear can help to track leakage and evaluate economics
- Step 2: Compare current leak rate to initial leak rate to determine leak reduction expected
  - Leak Reduction Expected (LRE) = Current Leak Rate (CL)
     Initial Leak Rate (IL)
  - Example: The current leak rate is measured as 100 cf/h, the same component leaked 11.5 cf/h when first installed

LRE = 100 cf/h – 11.5 cf/h LRE = 88.5 cf/h



#### **Methane Recovery Through Economic Rod Packing Replacement**

#### \* Step 3: Assess costs of replacements

- <u>\$ 500 to \$ 800</u> ♦ A set of rings: (with cups and case) \$1500 to \$2500 \$1800 to \$3500 ◆ Rods:
- \* Step 4: Determine economic replacement threshold
  - Partners can determine economic threshold for all replacements

Economic Replacement Threshold (scfh) = CR \* DF \* 1.000

(H ∗ GP)

Where:

NaturalGas (

CR = Cost of replacement (\$)

DF = Discount factor (%) @ interest i

 $\mathsf{DF} = \frac{i(1+i)^n}{(1+i)^n - 1}$ H = Hours of compressor operation per year

GP = Gas price (\$/Mcf)

# **Is Recovery Profitable?**

# Step 5: Replace packing and rods when cost-effective

#### Example: Rings Only

Rings: Rod: Gas: Operating:	\$1,200 \$0 \$3/Mcf 8,000 hrs/yr	
Leak Reduction Expected (scfh)	Payback Period (yrs)	
55	1	
29	2	
20	3	
16	4	
13	5	

Rod and Rings				
Rings:	\$1,200			
Rod:	\$7,000			
Gas:	\$3/Mcf			
	8,000 hrs/yr			
Operating:	8,000 hrs/	'yr		
Operating: Leak Reduction Expected (scfh)	8,000 nrs/ Payback Period (yrs)	′yr		
Operating: Leak Reduction Expected (scfh) 376	8,000 hrs/ Payback Period (yrs)	′yr		

(scfh)	(yrs)
376	1
197	2
137	3
108	4
90	5



Based on 10% interest rate Mcf = thousand cubic feet, scfh = standard cubic feet per hour

# **Industry Experience**

- \* One partner reported replacing worn rod packing rings on 15 compressor units
- Estimated gas savings of 7,000 Mcf or \$21,000
   @ \$3/Mcf
- \* Cost including materials and labor of \$17,000
- \* Payback period of less than one year



### Methane Losses from Centrifugal Compressors

- Centrifugal compressor wet seals leak little gas at the seal face
  - Seal oil degassing may vent 40 to 200 cubic feet per minute (cf/m) to the atmosphere
  - A Natural Gas STAR partner reported wet seal emissions of 75 Mcf/day (52 cf/m)





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### **Centrifugal Compressor Wet Seals**

- High pressure seal oil is circulates between rings around the compressor shaft
- \* Gas absorbs in the oil on the inboard side
- \* Little gas leaks through the oil seal
- Seal oil degassing vents methane to the atmosphere





# Gas STAR Partners Reduce Emissions with Dry Seals

- Dry seal springs press the stationary ring in the seal housing against the rotating ring when the compressor is not rotating
- \* At high rotation speed, gas is pumped between the seal rings creating a high pressure barrier to leakage
- Only a very small amount of gas escapes through the gap
- 2 seals are often used in tandem





#### **Methane Recovery with Dry Seals**

 Dry seals typically leak at a rate of only 0.5 to 3 cf/m

 Significantly less than the 40 to 200 cf/m emissions from wet seals

 These savings translate to approximately \$48,960 to \$279,360 in annual gas value





#### **Other Benefits with Dry Seals**

- Aside from gas savings and reduced emissions, dry seals also:
  - Lower operating cost
    - Dry seals do not require seal oil make-up
  - Reduced power consumption
    - Wet seals require 50 to 100 kiloWatt hours (kW/hr) for ancillary equipment while dry seals need only 5 kW/hr
  - Improve reliability
    - More compressor downtime is due to wet seals
  - Eliminate seal oil leakage into the pipelines
    - Dry seals lower drag in pipelines (and horsepower to overcome)



## Gas STAR Partners Reduce Emissions with Dry Seal Replacement

#### **Decision Process**





### **Decision Process to Replace Seals**

- \* Step 1: Identify candidates for replacement
  - Dry seals are routinely used for compressors operating up to 1,500 pounds per square inch (psi), up to 400° Fahrenheit
- \* Step 2: Estimate savings from a dry seal
  - ♦ Gas savings between 34 to 196 cf/m
  - ♦ Other dry seal benefits ≈ \$63,000/yr
    - 1. Reduced seal power losses = \$13,900
    - 2. Reduced oil pump/fan losses= \$4,000
    - Increased pipeline flow efficiency = \$26,600
    - 4. Reduced oil losses = \$3,500
    - 5. Reduced O&M, downtime = \$15,000



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### **Decision Process to Replace Seals**

#### \* Step 3: Determine dry seal conversion costs

- Dry seals cost \$5,000 to \$6,000 per inch of shaft diameter or \$8,000 to \$10,000 for tandem seals
- Beam compressors require two seals, one at each end
- Overhung compressors require one seal at the inboard end



#### **Decision Process to Replace Seals**

#### Step 4: Compare costs and savings for a 6-inch shaft beam compressor

Cost Category	Dry Seal (\$)	Wet Seal (\$)
Implementation Costs		
Seal costs (2 dry @ \$10,000/shaft-inch, w/testing)	120,000	
Seal costs (2 wet @ \$5,000/shaft-inch)		60,000
Other costs (engineering, equipment installation)	120,000	0
Total Implementation Costs	240,000	60,000
Annual O&M	10,000	73,000
Annual methane emissions⁴ (@ \$3.00/Mcf; 8,000 hrs/yr)		
2 dry seals at a total of 6 scfm	8,640	
2 wet seals at total 100 scfm		144,000
Total Costs Over 5-Year Period (\$):	333,200	1,145,000
Total Dry Seal Savings Over 5 Years:		
Savings (\$)	811,800	
Methane Emissions Reductions (Mcf) (at 45,120 Mcf/yr)	225,600	



Flowserve Corporation

# **Is Recovery Profitable?**

Replacing wet seals in a 6 inch shaft beam compressor operating 8,000 hr/yr

- Net Present Value = \$531,940
  - Assuming a 10% discount over 5 years
- Internal Rate of Return = 86%
- Payback Period = 14 months
  - Ranges from 8 to 24 months based on wet seal leakage rate

#### \* Economics are better for new installations

 Vendors report that 90% of compressors sold to the natural gas industry are centrifugal with dry seals



# **Industry Experience**

- \* One Gas STAR partner replaced a wet seal with a dry seal and reduced emissions by 97%
- \* Dry seal leaked 2 Mcf/d versus wet seal emissions of 75 Mcf/d



#### **Discussion Questions**

- \* To what extent have you replaced rod packing or seals in your reciprocating and centrifugal compressors?
- How can the Lessons Learned study be improved upon or altered for use in your operation(s)?
- \* What are the barriers (technological, economic, lack of information, regulatory, etc.) that are preventing you from implementing this technology?

