

# MECHANICAL INTEGRITY TESTING (MIT)



**EPA Region 6**

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**(Credits to George Robin, Steve Platt & Chuck Tinsley)**

What we protect:

USDWs

(Underground Sources of  
Drinking Water)

Pronounced:

**you wess dee duh yas**

# Mechanical Integrity (MI)

## Part 1

### **Internal** Mechanical Integrity

**40 CFR §146.8(a)(1)**

## Part 2

### **External** Mechanical Integrity

**40 CFR §146.8(a)(2)**

## 146.8 Mechanical integrity.

(a) An injection well has mechanical integrity if:

### **(Internal)**

(1) There is no significant leak in the casing, tubing or packer;

(b) One of the following methods must be used to evaluate the absence of significant leaks under paragraph (a)(1) of this section:

(1) Following an initial pressure test, monitoring of the tubing-casing annulus pressure with sufficient frequency to be representative, as determined by the Director, while maintaining an annulus pressure different from atmospheric pressure measured at the surface;

(2) Pressure test with liquid or gas; or

(3) Records of monitoring showing the absence of significant changes in the relationship between injection pressure and injection flow rate for the following Class II enhanced recovery wells:

(i) Existing wells completed without a packer provided that a pressure test has been performed and the data is available and provided further that one pressure test shall be performed at a time when the well is shut down and if the running of such a test will not cause further loss of significant amounts of oil or gas; or

(ii) Existing wells constructed without a long string casing, but with surface casing which terminates at the base of fresh water provided that local geological and hydrological features allow such construction and provided further that the annular space shall be visually inspected. For these wells, the Director shall prescribe a monitoring program which will verify the absence of significant fluid movement from the injection zone into an USDW.

## (External)

(a)(2) There is no significant fluid movement into an underground source of drinking water through vertical channels adjacent to the injection well bore.

c) One of the following methods must be used to determine the absence of significant fluid movement under paragraph (a)(2) of this section:

(1) The results of a temperature or noise log; or

(2) For Class II only, cementing records demonstrating the presence of adequate cement to prevent such migration; or

(3) For Class III wells where the nature of the casing precludes the use of the logging techniques prescribed at paragraph (c)(1) of this section, cementing records demonstrating the presence of adequate cement to prevent such migration;

4) For Class III wells where the Director elects to rely on cementing records to demonstrate the absence of significant fluid movement, the monitoring program prescribed by §146.33(b) shall be designed to verify the absence of significant fluid movement.

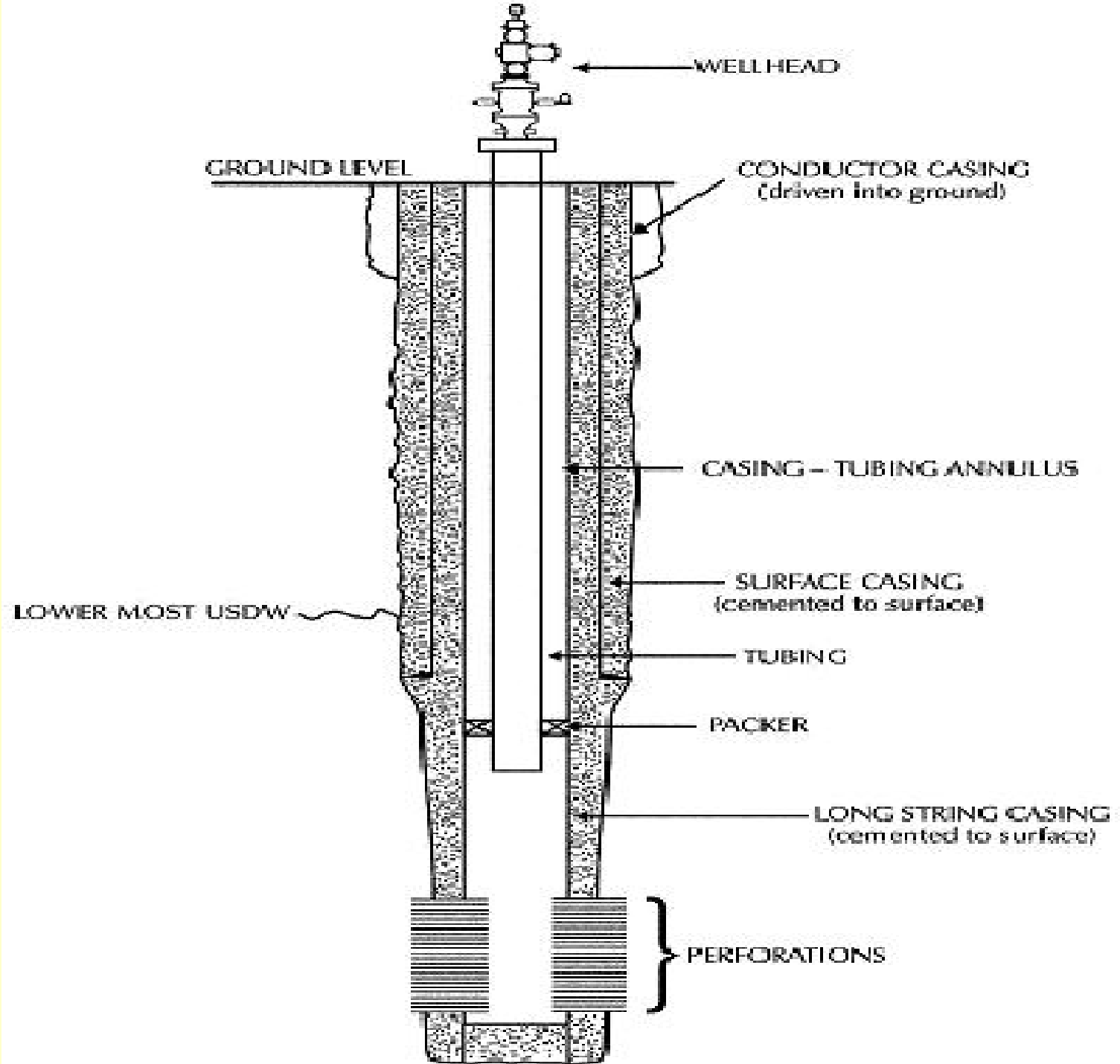
**(Alternative tests)**

(d) The Director may allow the use of a test to demonstrate mechanical integrity other than those listed in paragraphs (b) and (c)(2) of this section with the written approval of the Administrator. To obtain approval, the Director shall submit a written request to the Administrator, which shall set forth the proposed test and all technical data supporting its use. The Administrator shall approve the request if it will reliably demonstrate the mechanical integrity of wells for which its use is proposed. Any alternate method approved by the Administrator shall be published in the FEDERAL REGISTER and may be used in all States unless its use is restricted at the time of approval by the Administrator.

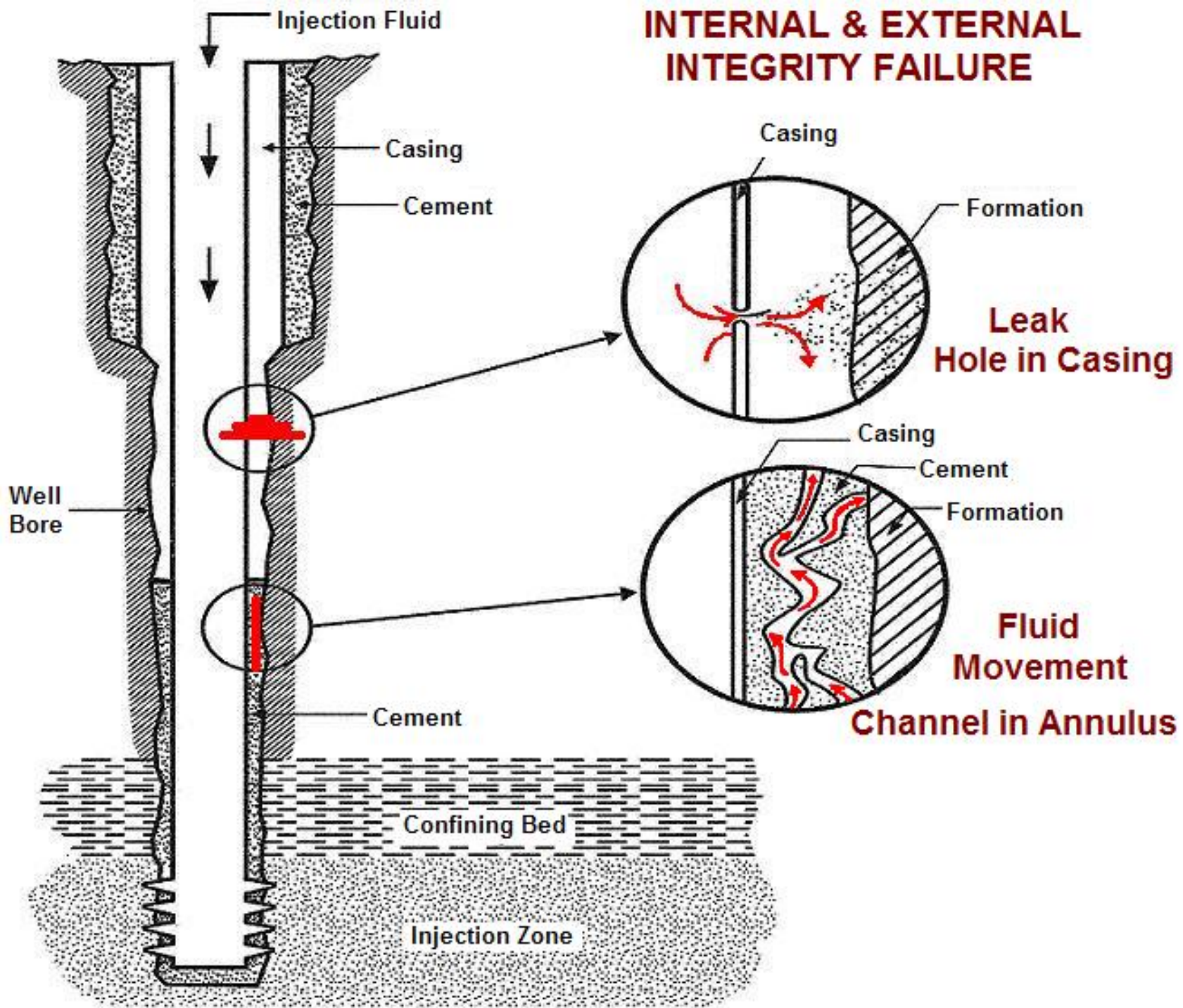
(e) In conducting and evaluating the tests enumerated in this section or others to be allowed by the Director, the owner or operator and the Director shall apply methods and standards generally accepted in the industry. When the owner or operator reports the results of mechanical integrity tests to the Director, he shall include a description of the test(s) and the method(s) used. In making his/her evaluation, the Director shall review monitoring and other test data submitted since the previous evaluation.

(f) The Director may require additional or alternative tests if the results presented by the owner or operator under §146.8(e) are not satisfactory to the Director to demonstrate that there is no movement of fluid into or between USDWs resulting from the injection activity.





# INTERNAL & EXTERNAL INTEGRITY FAILURE




# What are our main MI concerns?

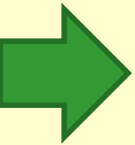
 **1** Any **leaks** in the system?

# What are our main MI concerns?

**1** Any **leaks** in the system?

 **2** Is injected fluid **entering and remaining** in the approved interval?

# What are our main MI concerns?

- 1** Any **leaks** in the system?
- 2** Is injected fluid **entering and remaining** in the approved interval?
-  **3** Is there **crossflow** of fluid into USDWs?

# What are our main MI goals?

**1** Any **leaks** in the system?

(Internal MI)

**Goal:**

Prevention of leakage through the  
“walls” of the well (casing, tubing, etc.)

# Prevention of Leakage through the “walls” of the well (casing, tubing, etc.).

## How leakage can be discovered:

- 
- **pressure tests**

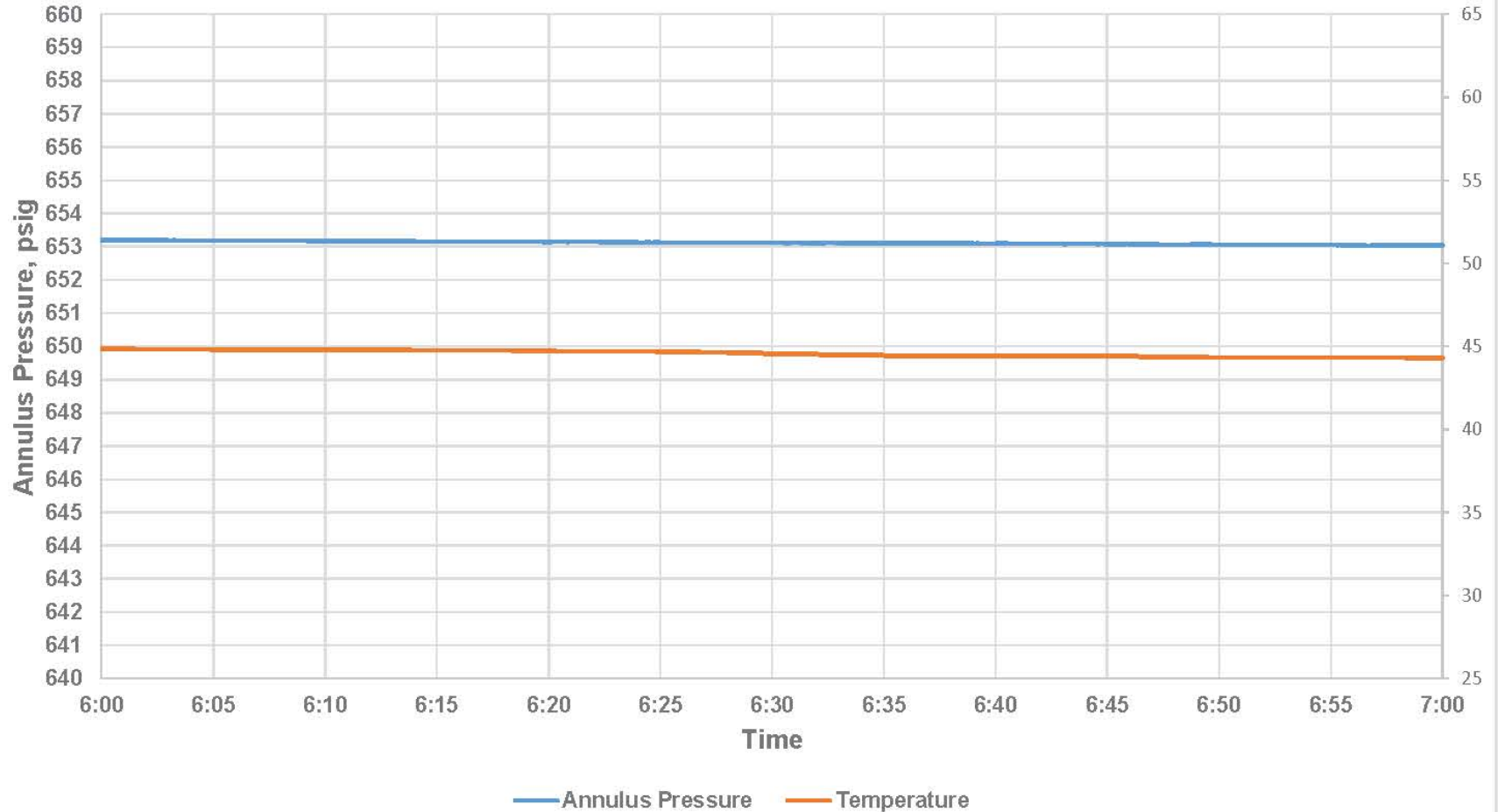
# **INTERNAL MI ANNULUS PRESSURE TEST**

- **Tests the tubing, casing and packer for leaks.**
- **Testing requirements vary by well Class and UIC program requirements. These vary by State or Tribe.**
- **Typically the casing/tubing annulus is pressured to the maximum allowable injection pressure to ensure the casing can withstand this pressure should the tubing or packer fail. Director variances can also be allowed.**
- **The test length is typically 30 minutes to 1 hour.**
- **Test failure is typically a pressure loss of  $> 5 - 10\%$**
- **It is a good practice to observe the fluid flowback when the pressure is released as this will help determine the amount of the annulus being tested and can potentially spot an obstruction or “misplaced” packer**



January 23, 2018

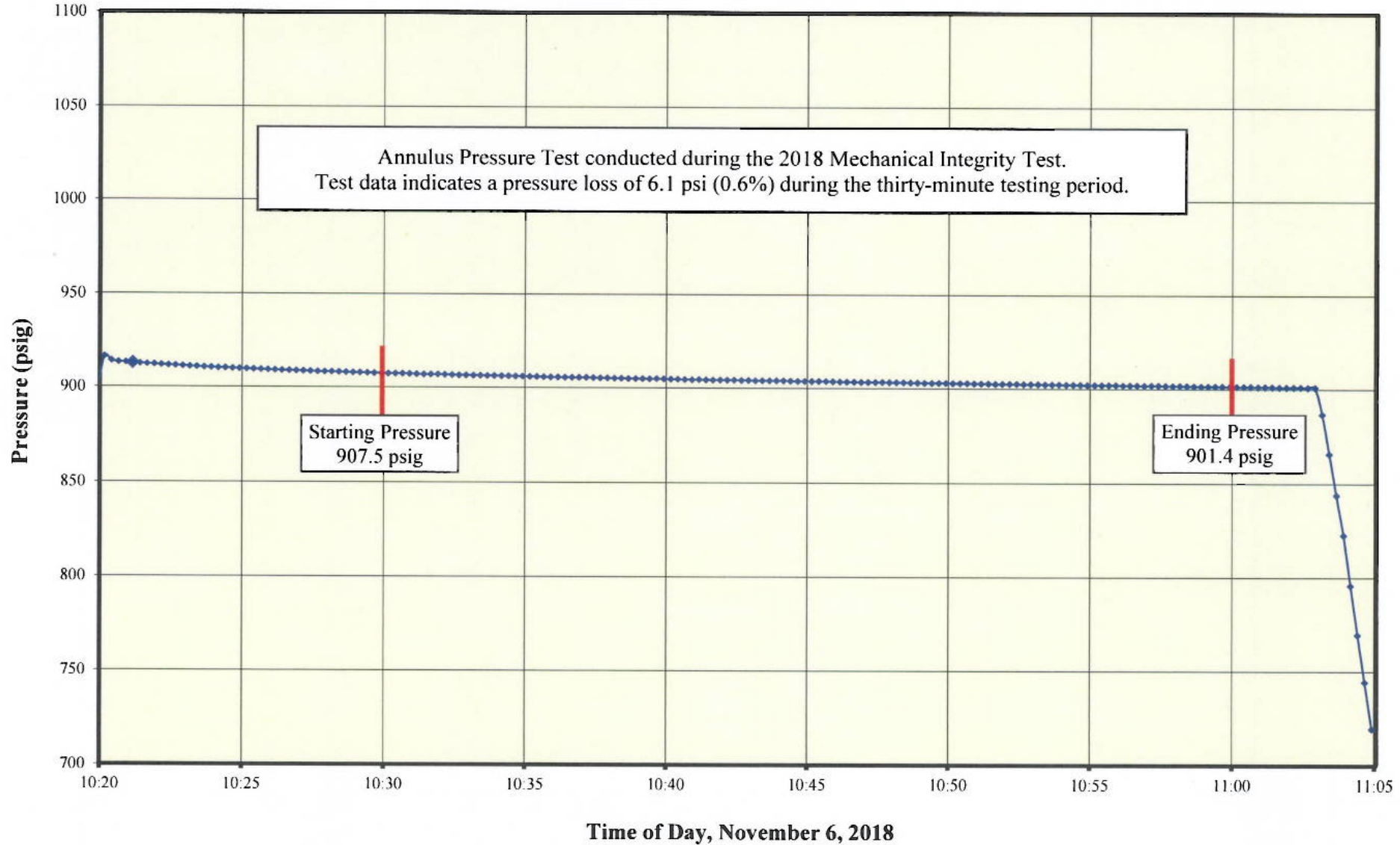
(Beginning Pressure = 653.20 psi & Ending Pressure = 653.03 psi;  
Beginning Temperature = 44.85°F & Ending Temperature = 44.30°F)



Revised 01-31-18

### Annulus Pressure Test

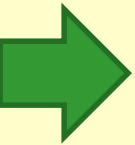
Annulus Pressure Test conducted during the 2018 Mechanical Integrity Test.  
Test data indicates a pressure loss of 6.1 psi (0.6%) during the thirty-minute testing period.



# Prevention of Leakage through the “walls” of the well (casing, tubing, etc.).

## How leakage can be discovered:

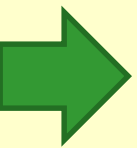
- **pressure tests**
- **downhole logging** (discussed later)



# Prevention of Leakage through the “walls” of the well (casing, tubing, etc.).

## How leakage can be discovered:

- **pressure tests**
- **downhole logging**
- **monitoring** of injection activities.
  - Annulus pressure
  - Injection pressure/rate relationship



# What are our main MI Goals?

## Prevention of Fluid Movement through Casing/Wellbore Annular Space

- 
- 2** Is injected fluid **entering and remaining** in the approved interval?  
(External MI)

# What are our main MI Goals?

## Prevention of Fluid Movement through Casing/Wellbore Annular Space

**2** Is injected fluid **entering and remaining** in the approved interval?

**(External MI)**

 **3** Is there **crossflow** of fluid into USDWs?

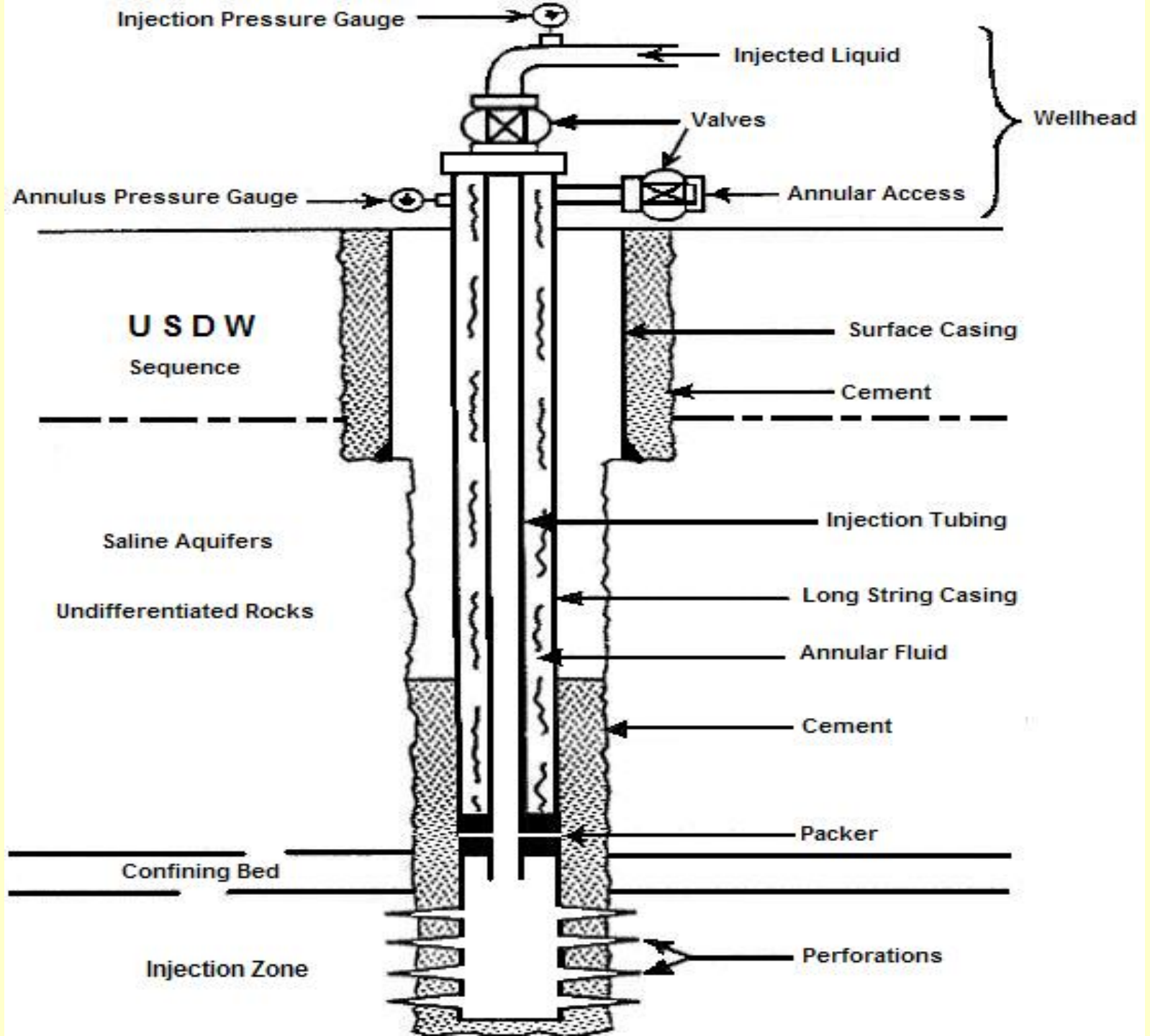
**(External MI)**

# What are our main MI Goals?

Prevention of Fluid Movement through  
Casing/Wellbore Annular Space



**Proper cementing and construction**





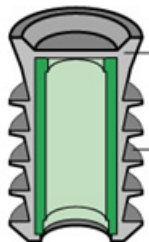
# Casing Cementing Operations

Top plug



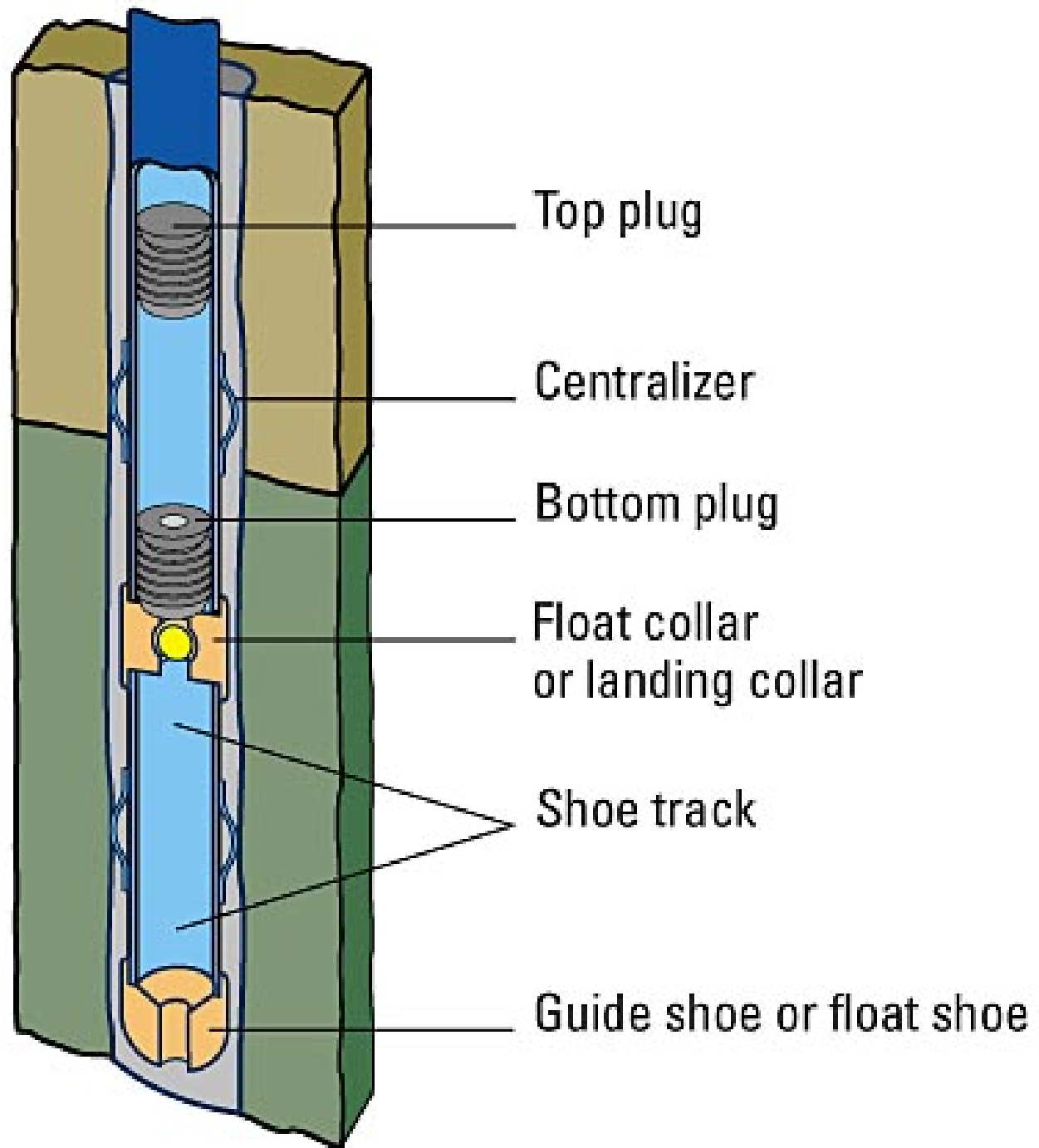
Solid core

Bottom plug



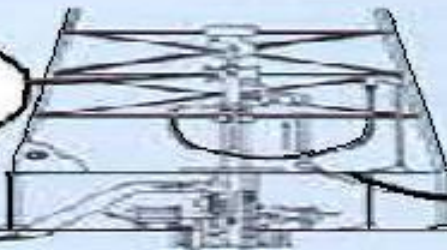
Rupture disk

Hollow core





PLUG CONTAINER



DENSOMETER

SURFACE CASING  
PRODUCTION CASING  
DISPLACEMENT FLUID

JET MIXER AND HOPPER  
DRY CEMENT

WATER  
UNDER  
PRESSURE



TOP PLUG



BOTTOM PLUG



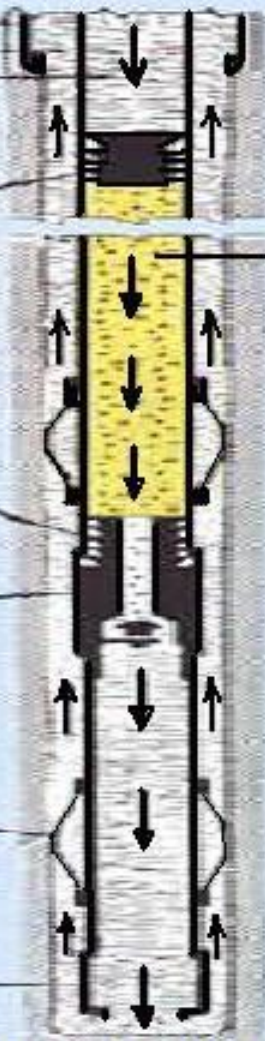
FLOAT COLLAR



CENTRALIZER



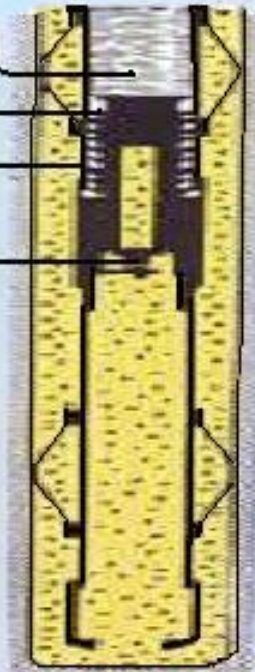
GUIDE SHOE



JOB IN PROCESS

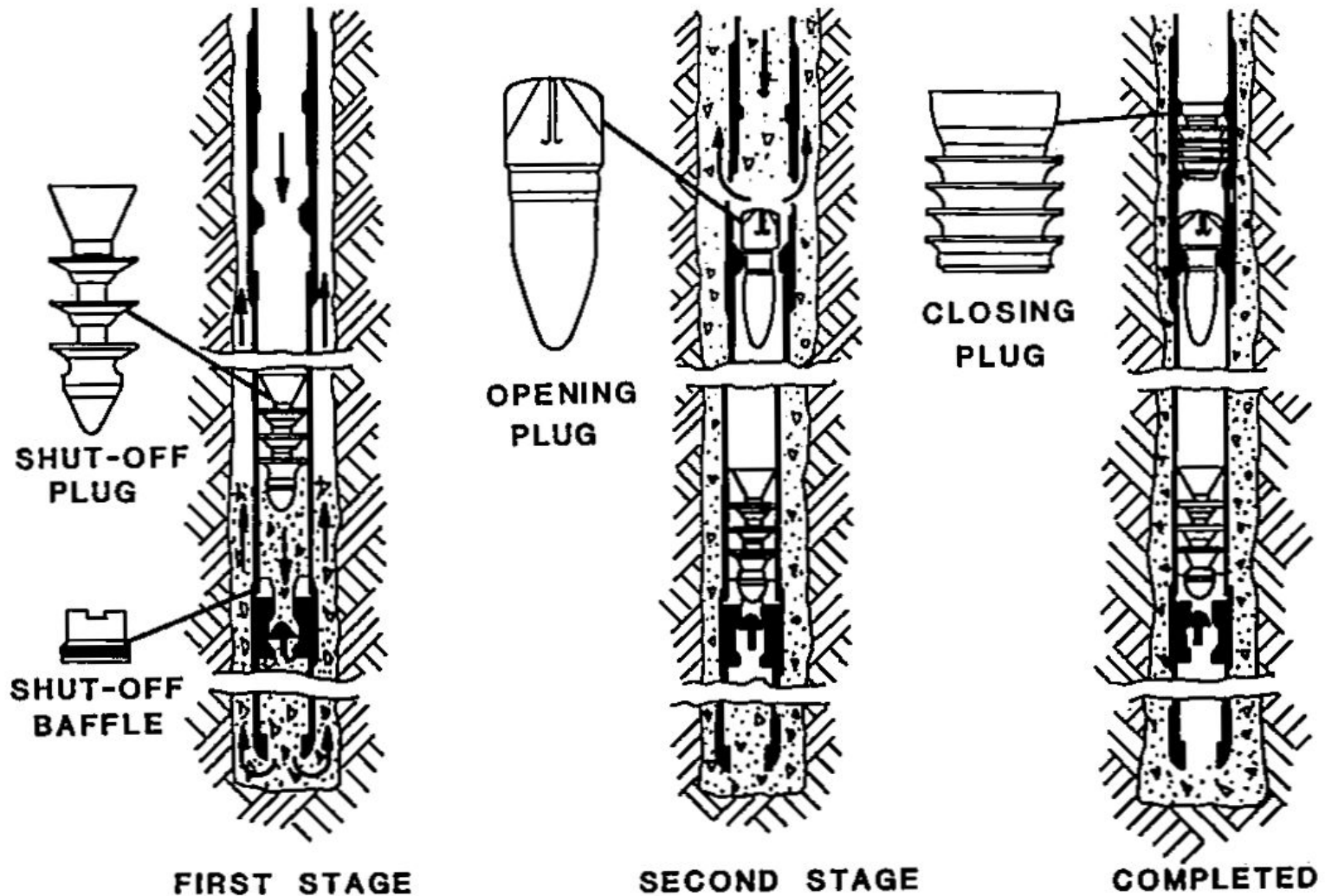
CEMENT SLURRY

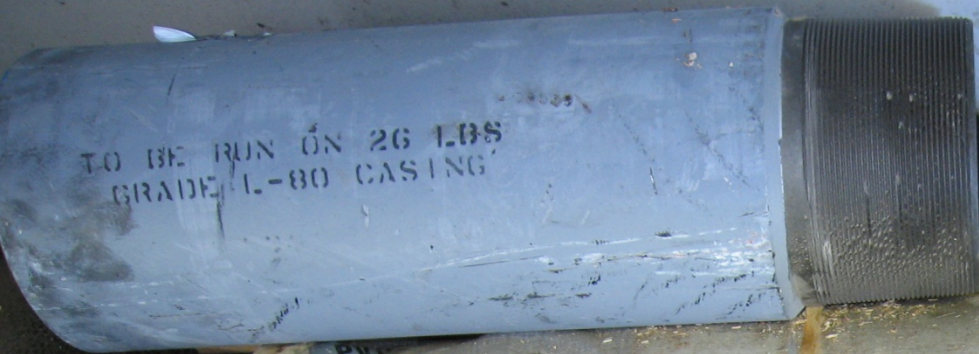
DISPLACEMENT FLUID  
TOP PLUG  
SEATED  
BOTTOM PLUG  
SEATED  
VALVE  
CLOSED



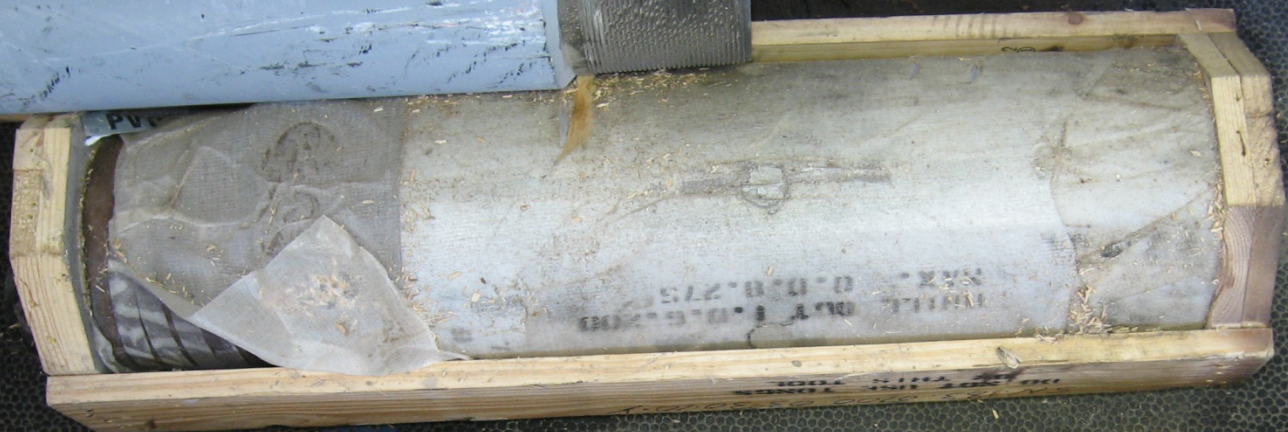
JOB FINISHED

# Two-stage Cementing Tools: (Float Collar, DV tool, and Plugs)





Float Collar near TD



DV tool @ 4000 ft



3<sup>rd</sup> - Closing Plug  
(Closes DV tool)

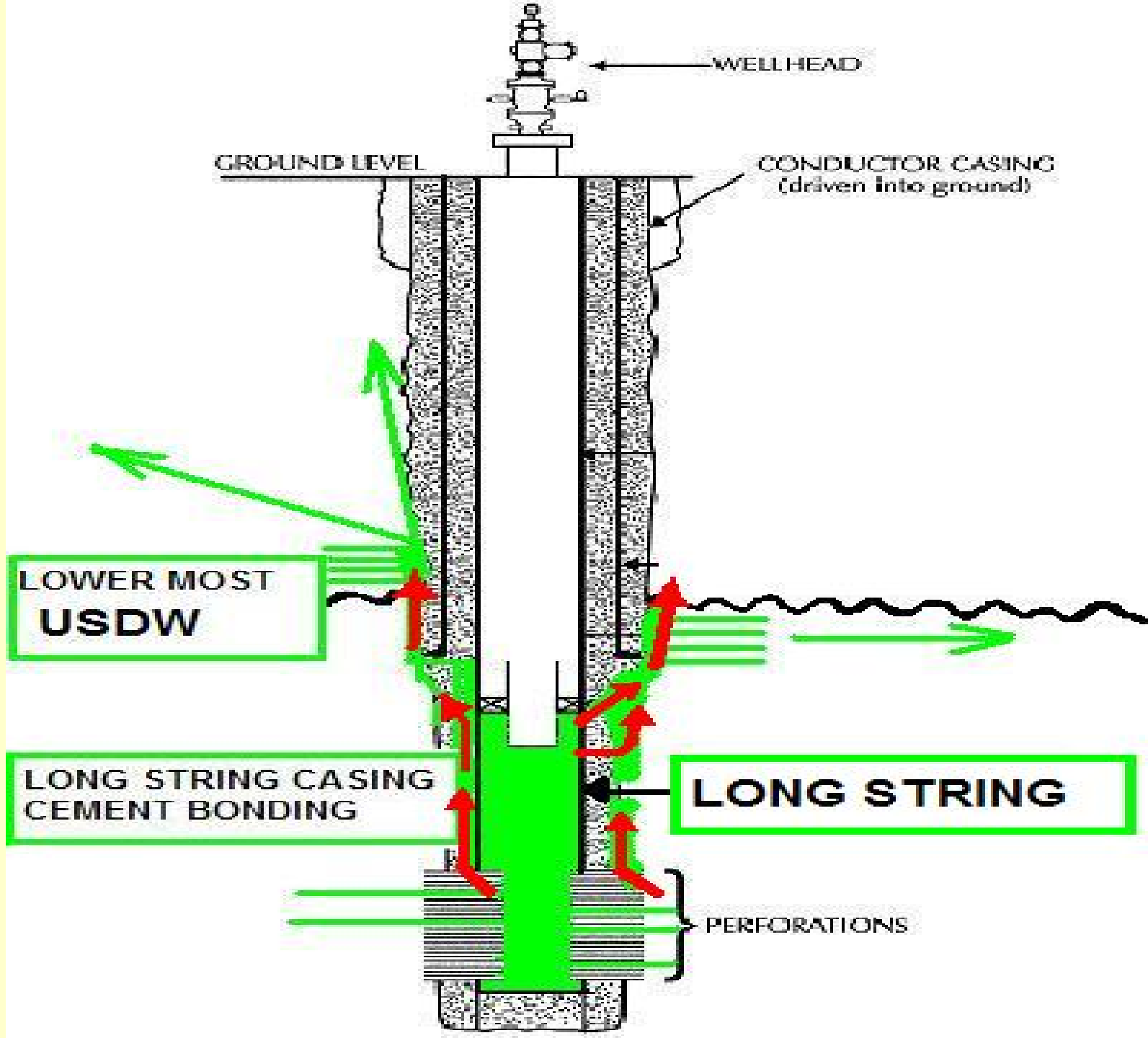
2<sup>nd</sup> - Opening Plug  
(Opens DV tool)

1<sup>st</sup> - Shut-off Plug  
(Ends first stage)



# Centralizers



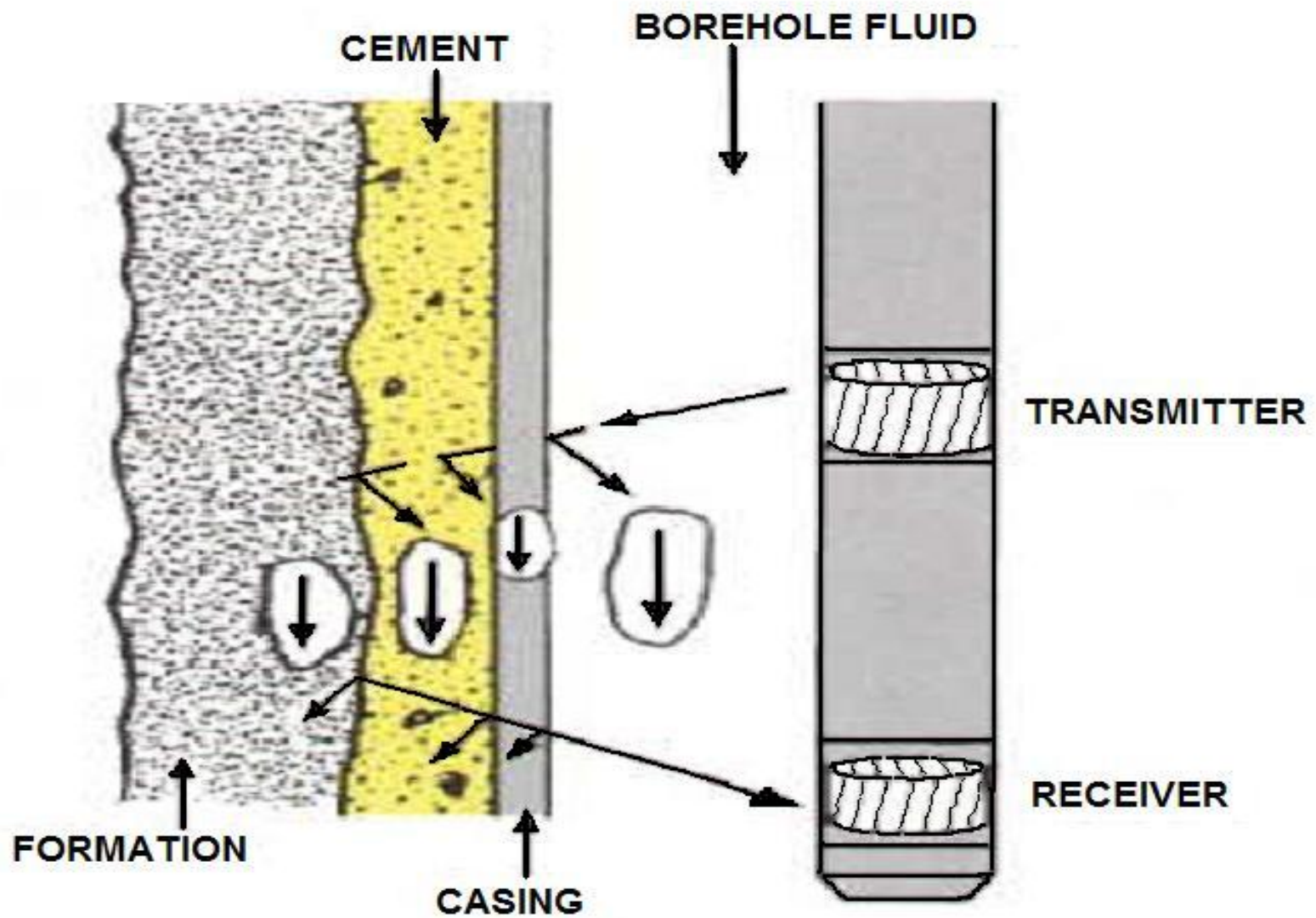


**Cement  
Bond  
Log  
  
(CBL)**

- **Cement needs to set properly before a cement integrity log is run. This can take from 10 to 50 hours for typical cement jobs.**
- **Full compressive strength is reached in 7 to 10 days. The setting time depends on the type of cement, temperature, pressure, and the use of setting accelerants.**
- **Excess pressure on the casing should be avoided during the curing period so that the cement bond to the pipe is not disturbed.**



- **Cement bond logs were run as early as 1958 with early sonic logs and the temperature log was used to find the cement top beginning in 1933.**
- **Cement integrity logs are run to determine the quality of the cement bond to the casing, to evaluate cement fill-up between the casing and the wellbore rock and to evaluate the cement bond to the wellbore rock.**
- **A poor cement bond may allow unwanted fluids to enter the wellbore or injected fluid to leave the injection interval.**



## CEMENT LOGGING PRINCIPLES



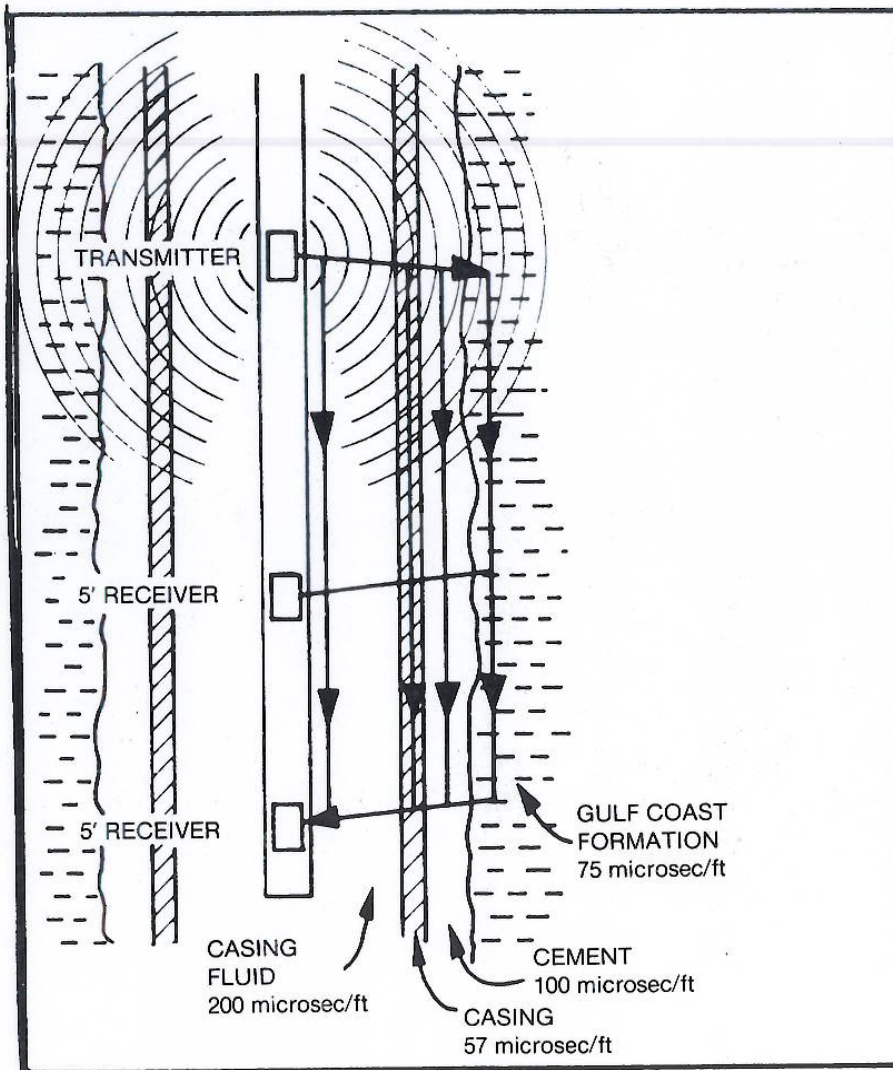


Figure 78. Typical transit times for various media inspection by the cement bond tool (Schlumberger, no date).

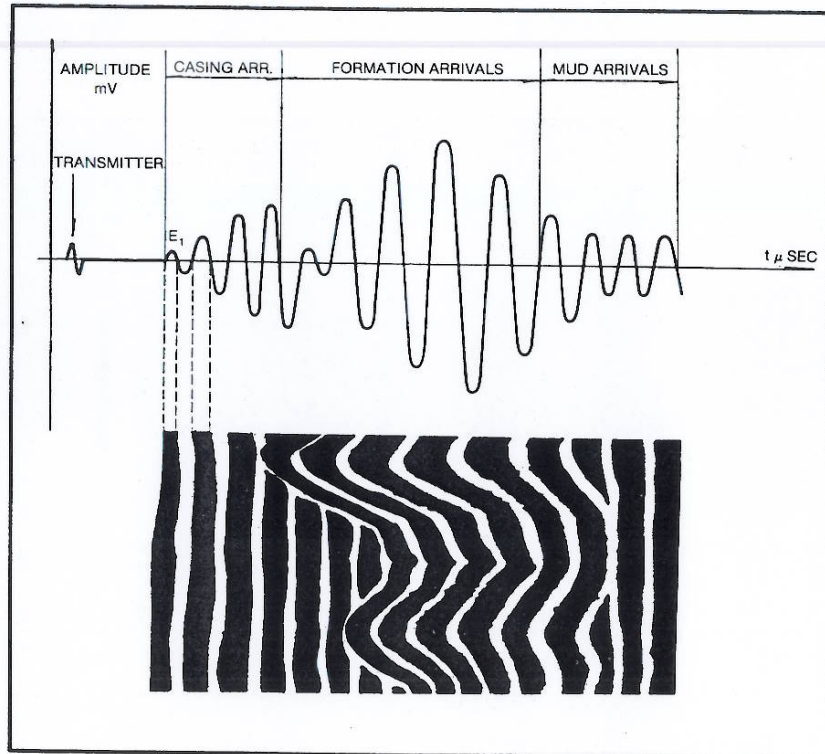
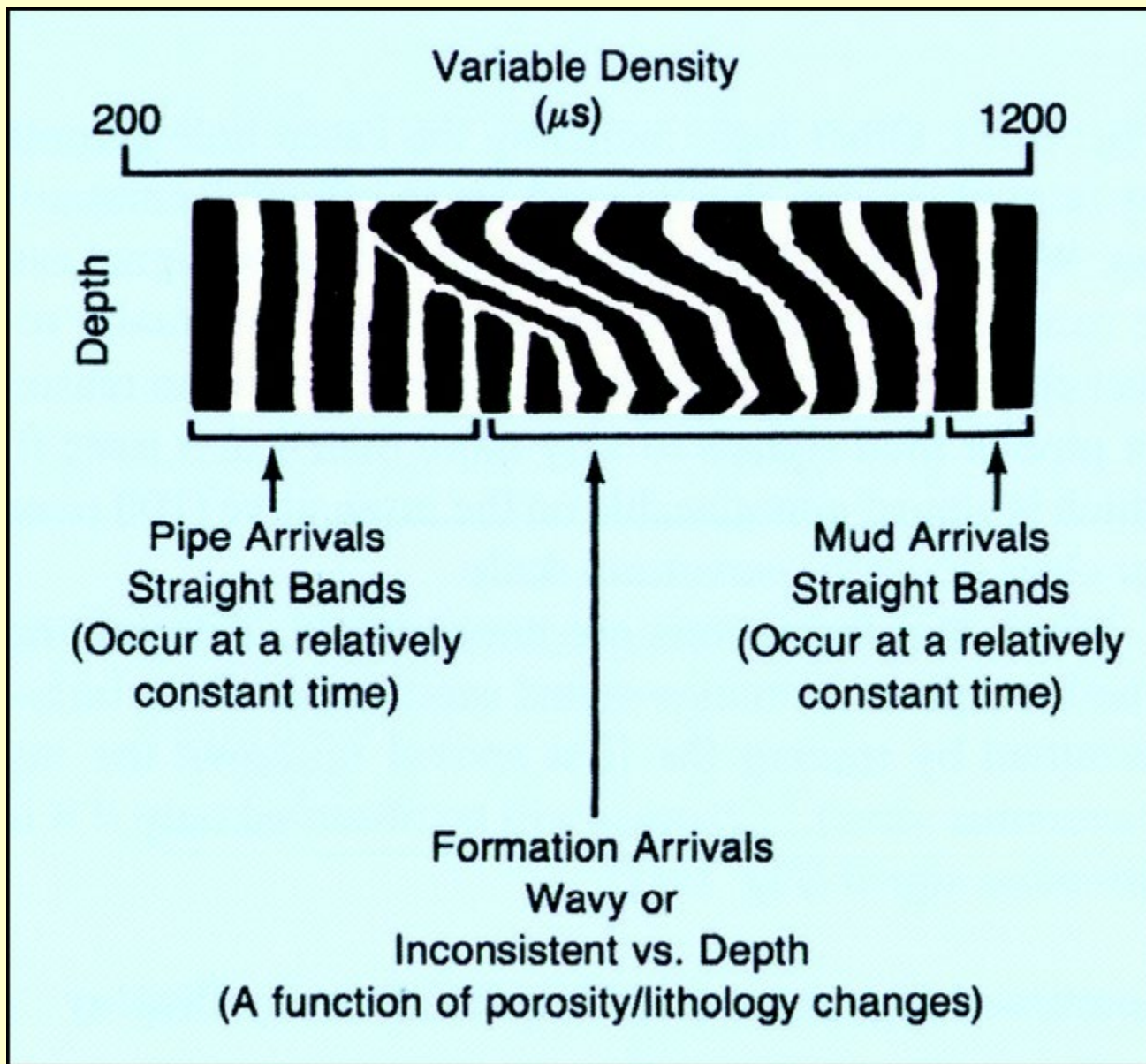


Figure 80. Principle of operation of the variable density log (Schlumberger, 1976).

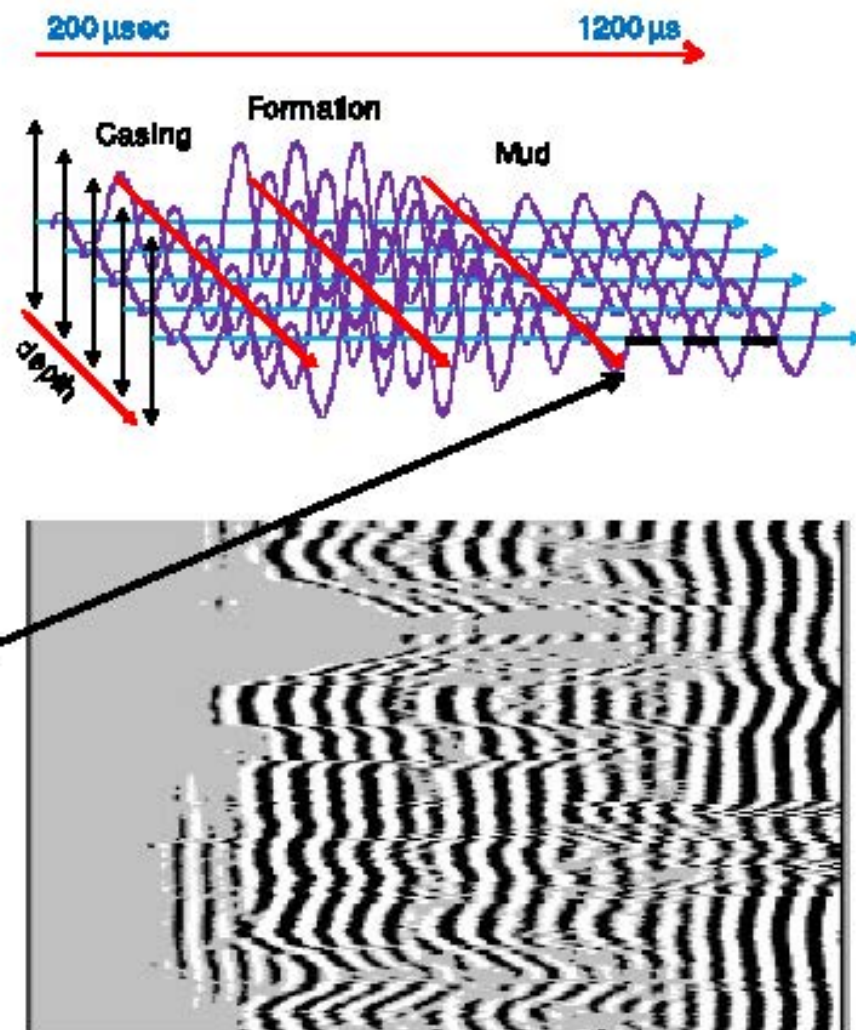


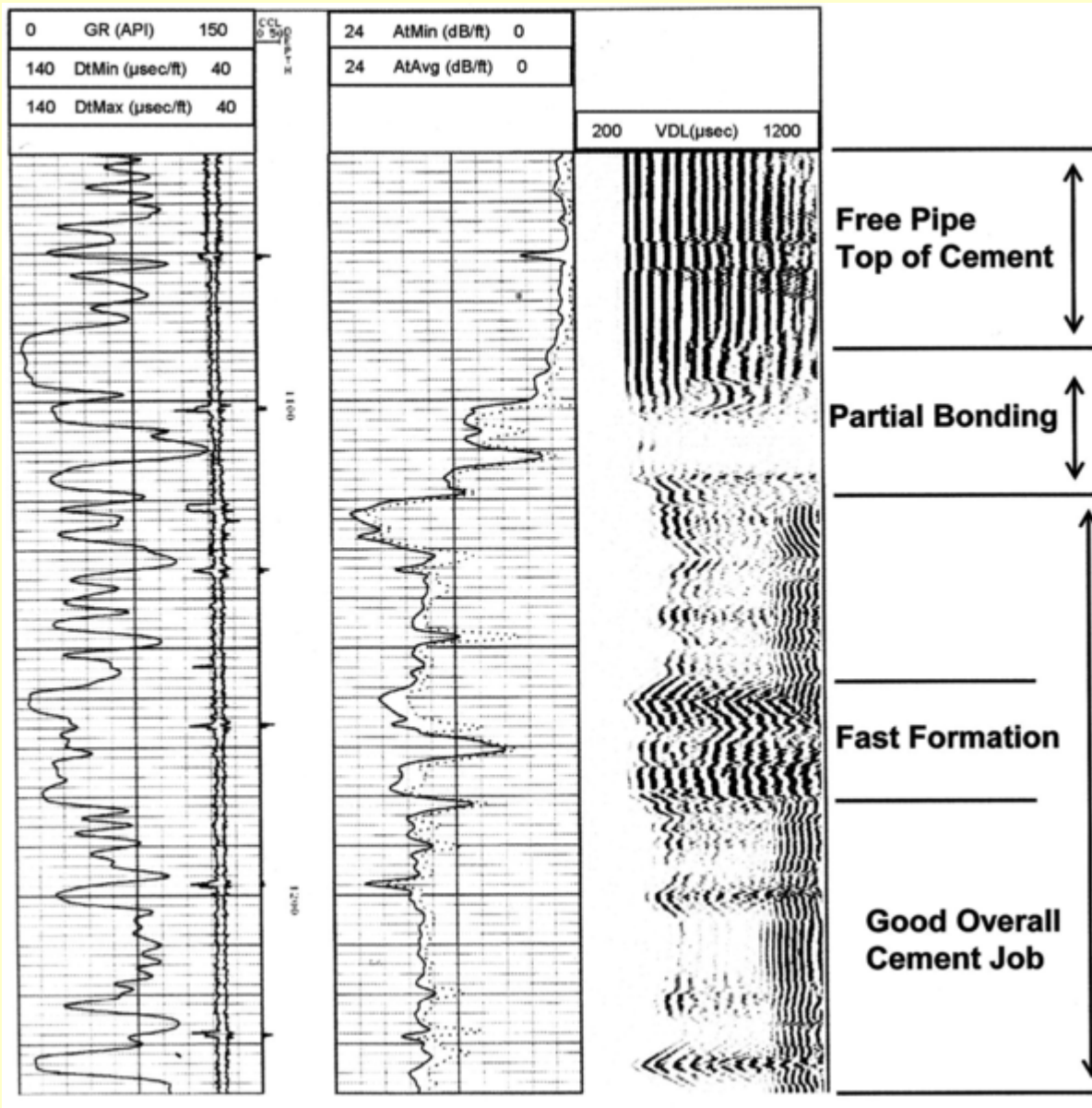
Identification of important features on a variable-density log (VDL) (courtesy of Baker Atlas).

# VDL

## Variable Density Log

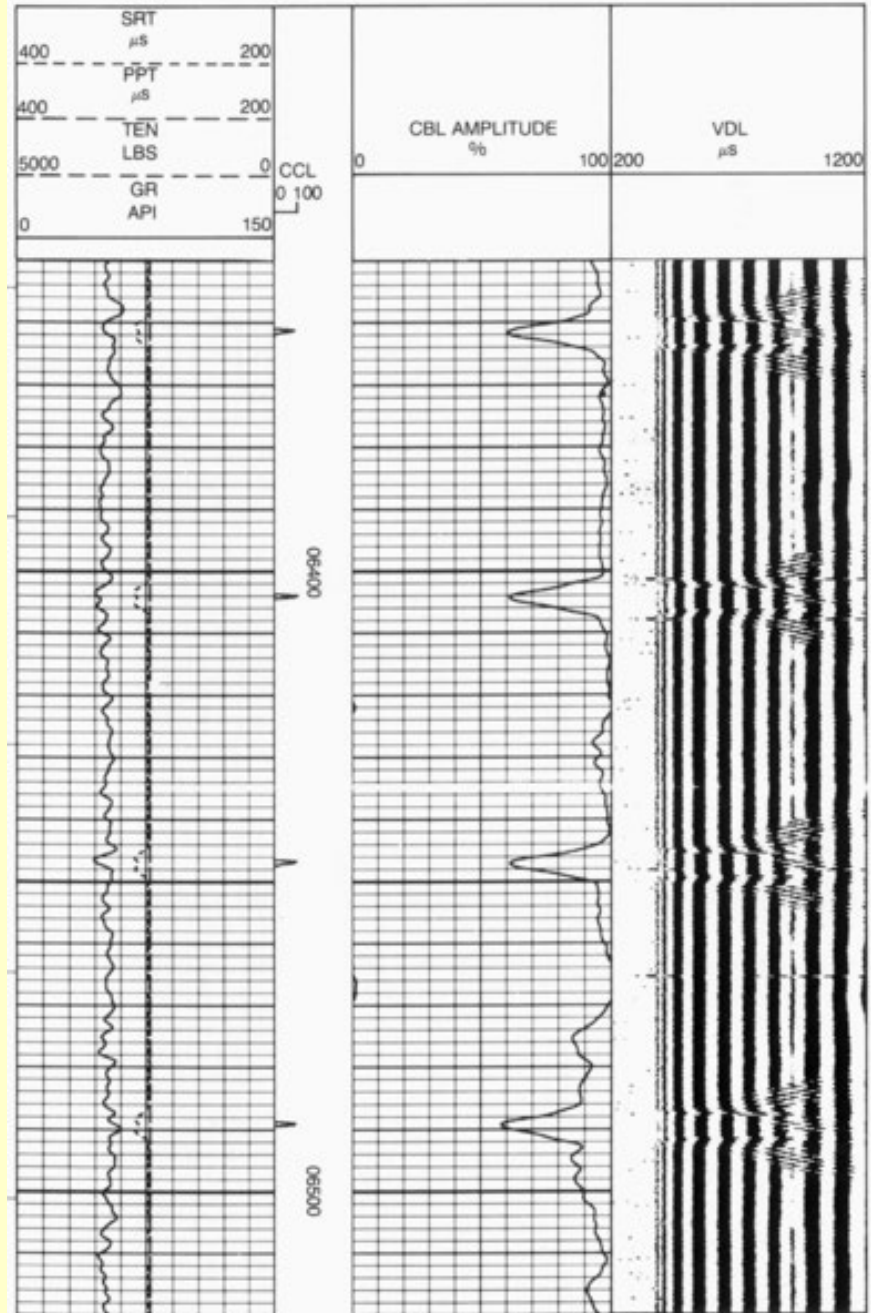
- VDL displays multiple “slices of data” side by side
  - 200 – 1200  $\mu$ s for 3' VDL
- Arrival patterns start to become apparent
- To make a 2D picture of the 3D image:
  - Positive peaks are shaded black
  - Negative peaks are shaded white
- Casing arrivals should be consistent but formation arrivals “*should*” change with lithology





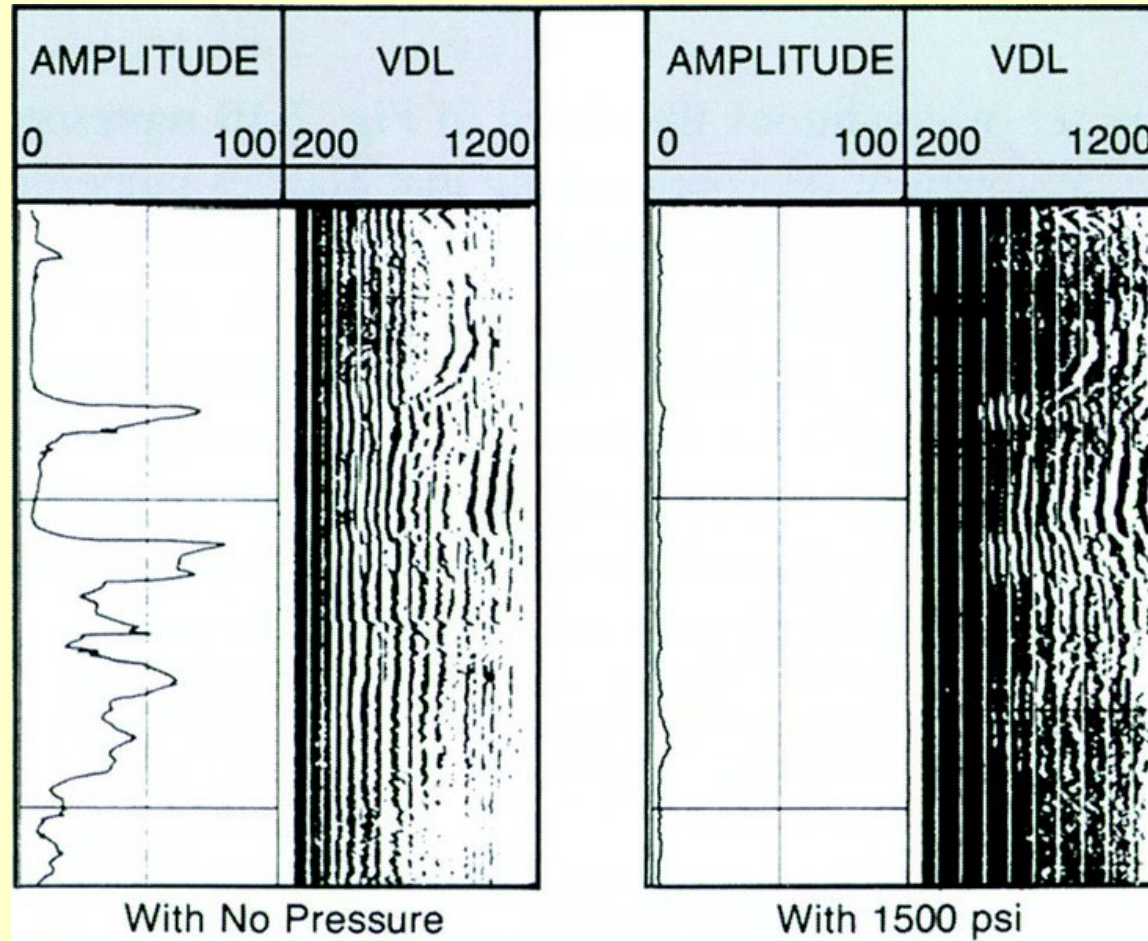
Typical cement-bond log presentation (courtesy of Baker Atlas).

In cases of poor bonding, casing-collar signals may also be identified as "w" patterns (anomalies)





# Field example showing microannulus effect on amplitude and VDL log displays (courtesy of Baker Atlas).



Pressuring the casing improves the acoustic coupling to the formation and the casing signal will decrease and the formation signal will become more obvious

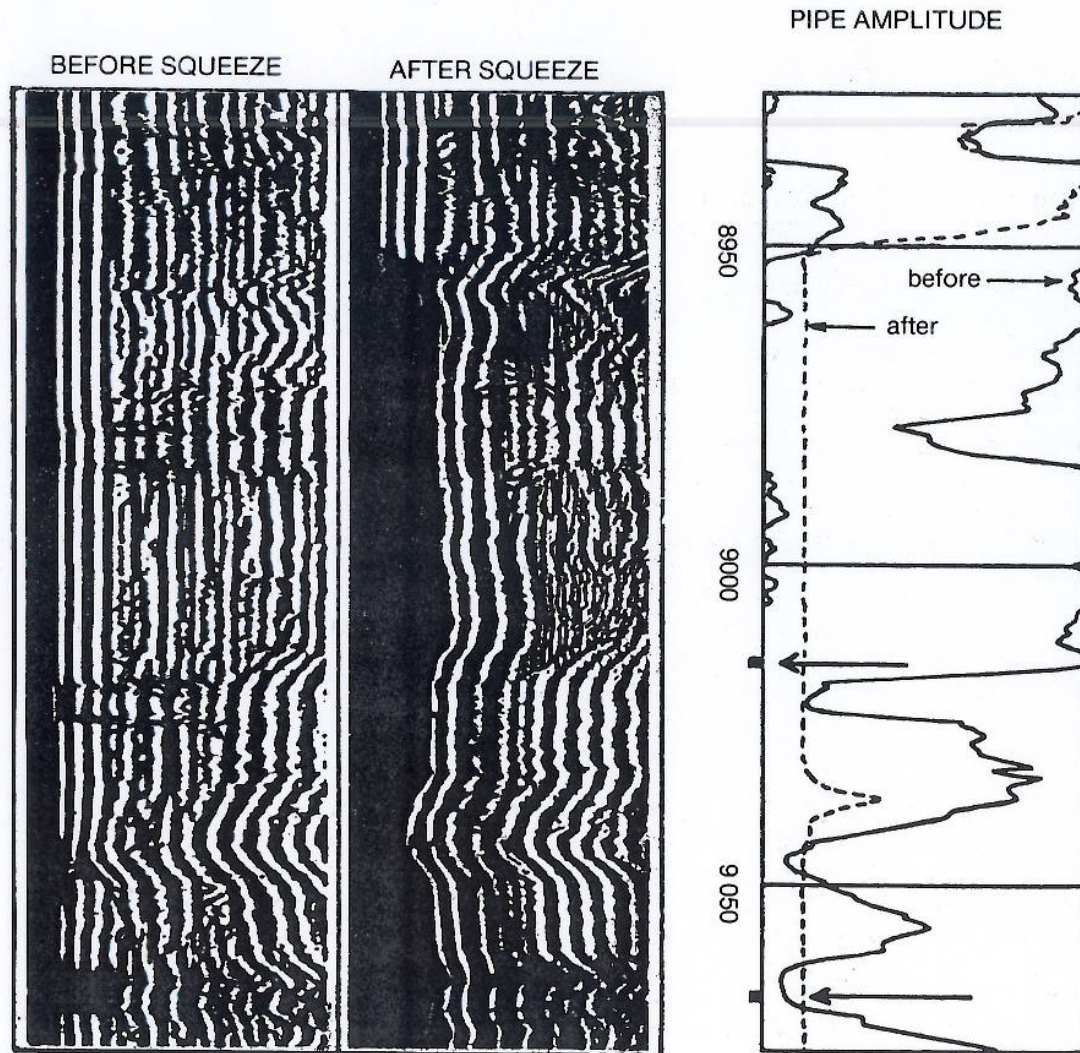
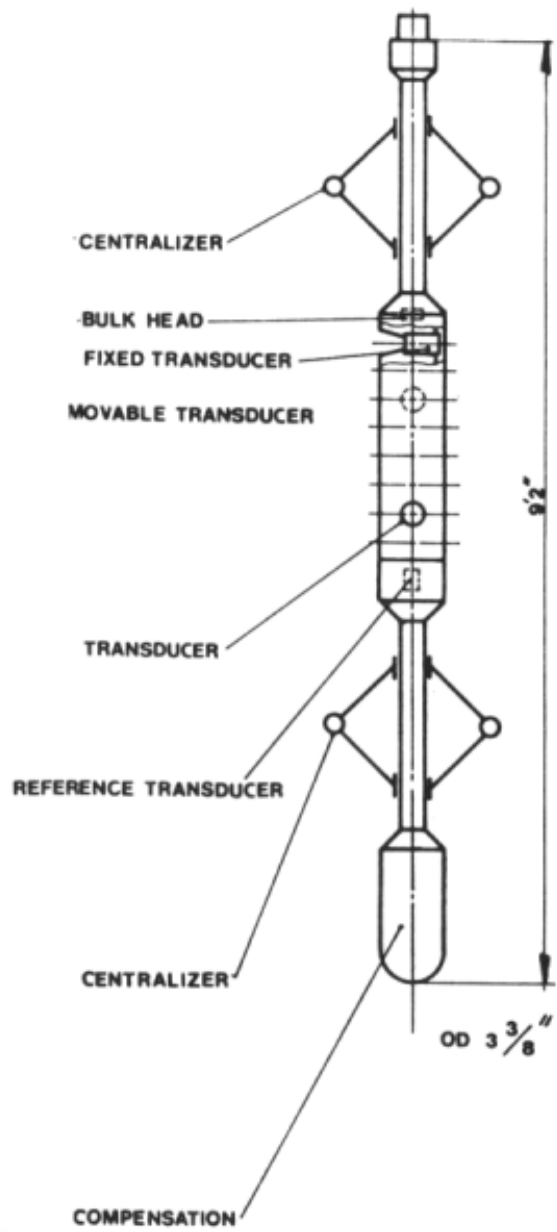


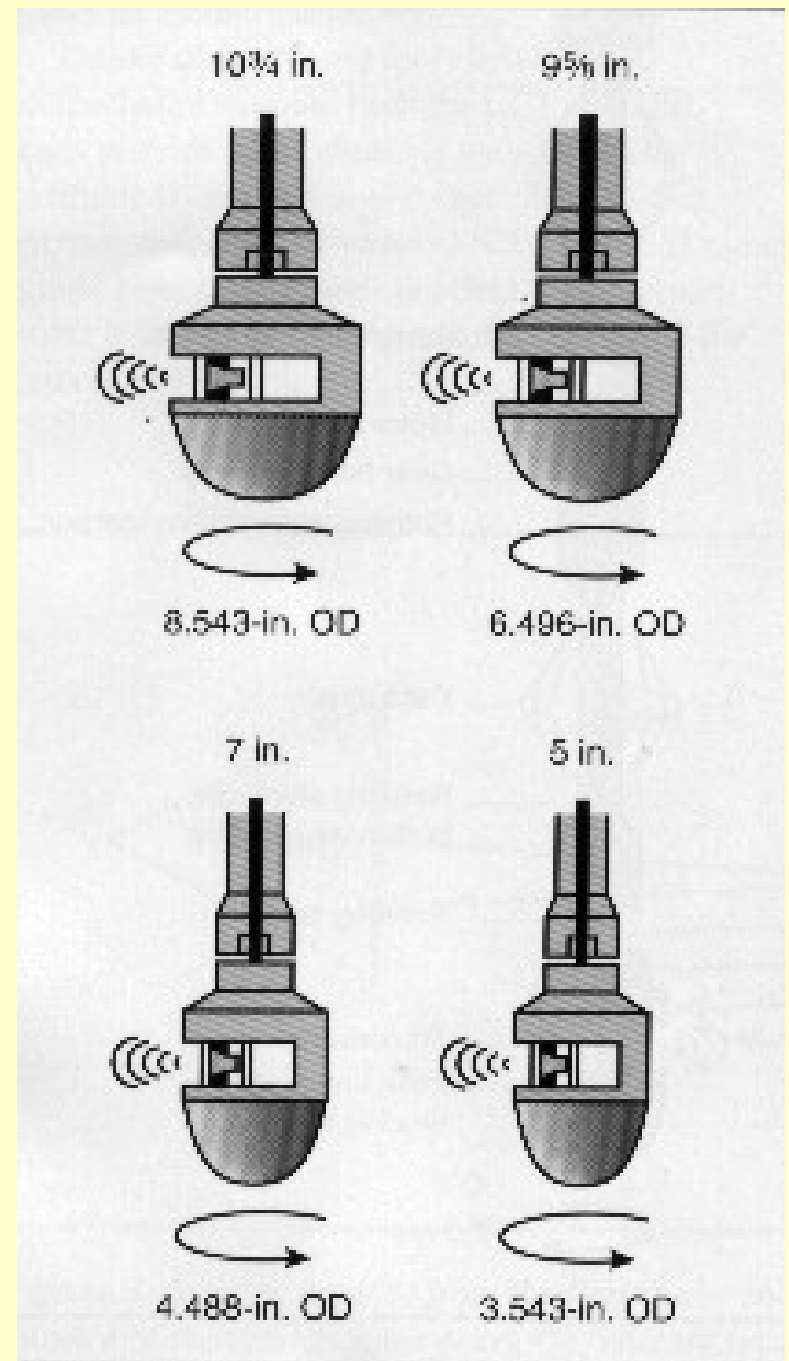
Figure 90. Elimination of a channel by cement squeezing (Walker, 1968).

# **CEMENT EVALUATION TOOL**

**(CET)**



**Cement Evaluation Tool**  
*(Courtesy of Schlumberger)*



# CET PURPOSE

- SAME AS **CEMENT BOND LOG (CBL)**  
ONLY MORE ADVANCED PRINCIPLE
- INVESTIGATES CEMENT **RADIALLY**
- MEASURES CASING **DIAMETER**, CASING **ROUNDNESS**, AND TOOL **ECCENTERING**

# CET

## PRINCIPLE OF OPERATION

- ULTRA SONIC ENERGY MAKES CASING **RESONATE**
- **RATE OF DAMPENING** IS MEASURED
- RADIAL INVESTIGATION IS ACHIEVED WITH **9 TRANSDUCERS**

# CET

## FACTORS AFFECTING MEASUREMENT

- TYPE OF **FLUID** IN WELL
- **THICKNESS** OF CASING WALL
- AMOUNT OF **CEMENT BONDED** TO CASING
- **COMPRESSIVE STRENGTH** OF CEMENT

# CET EQUIPMENT

- 8 TRANSDUCERS IN **HELICAL PATTERN**
- 1 TRANSDUCER (MEASURES **FLUID SOUND VELOCITY**)
- **TOOL SIZE** = 3-3/8 inches to 4 inches



# CET PROCEDURE

- REMOVE **TUBING**
- ENSURE TOOL IS **CENTRALIZED**
- LOG ONLY IN **LIQUID FILLED** CASING
- RUN WITH CASING **COLLAR LOCATOR**  
AND **GAMMA RAY**

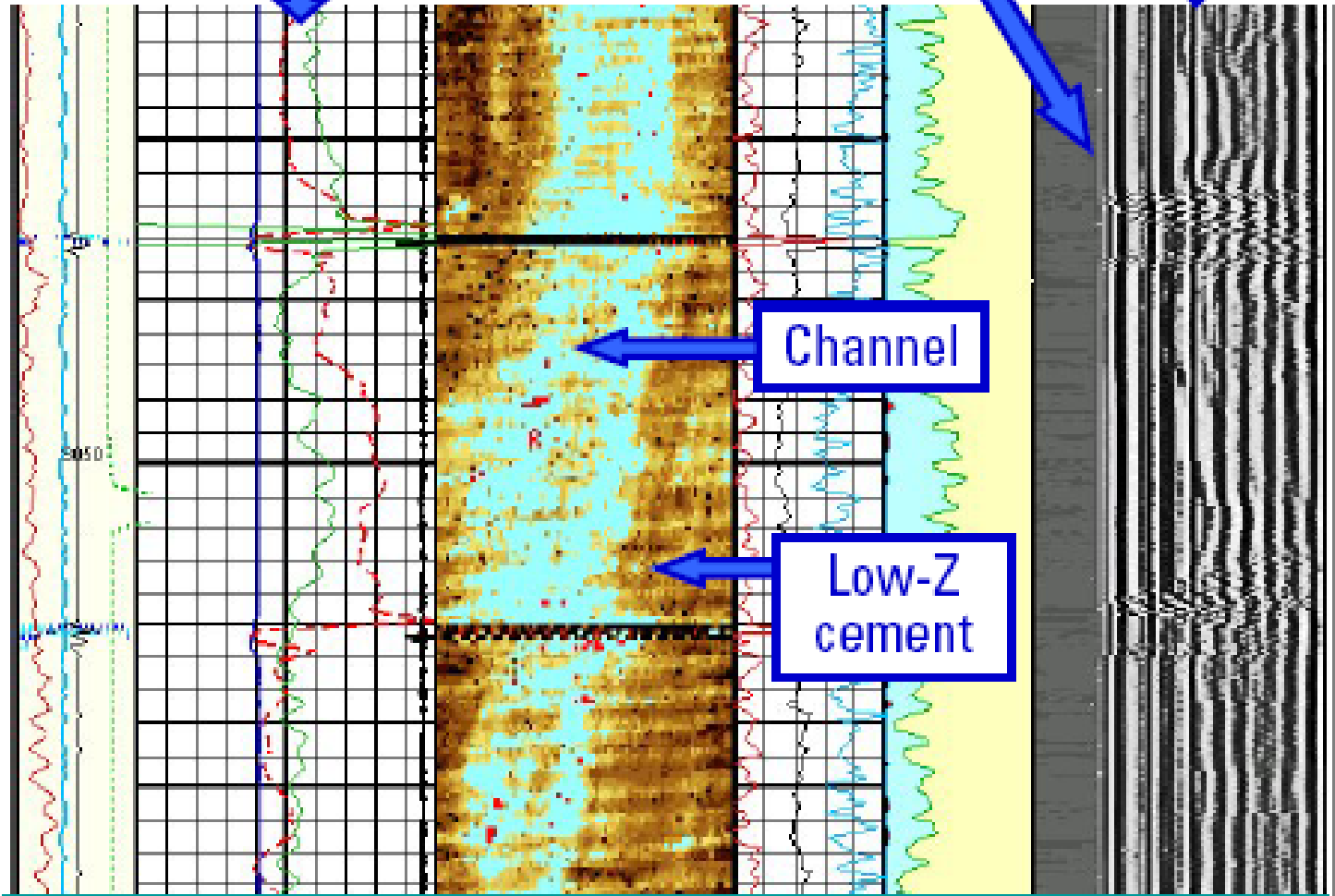
# CET ADVANTAGES

- **RADIAL** CEMENT EVALUATION
- CEMENT **CHANNEL IDENTIFICATION**
- IMMUNE TO **MICROANNULUS**
- NOT AFFECTED BY **“FAST FORMATIONS”**
- **“EASIER” TO INTERPRET**

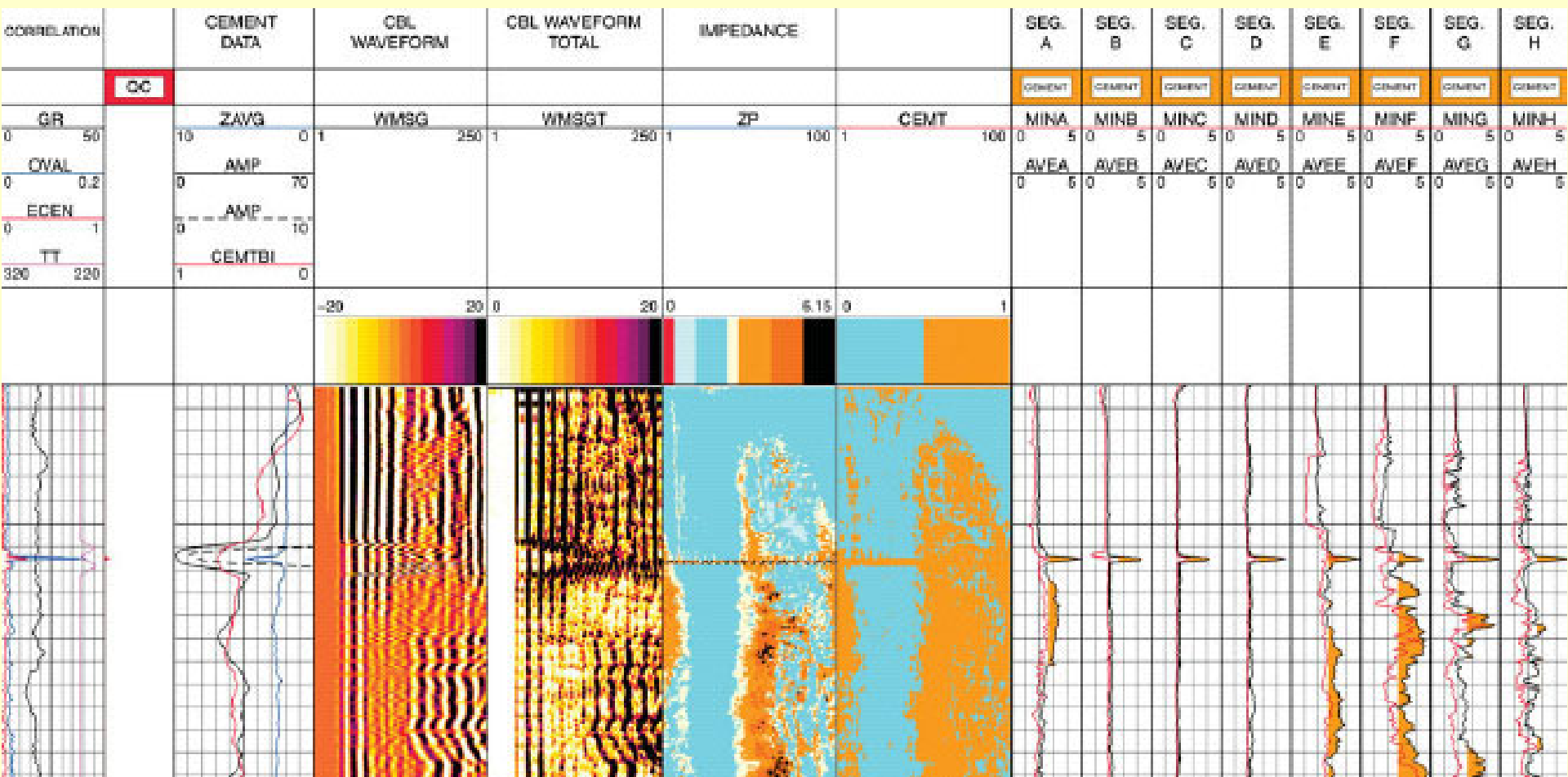
CBL variable, high

Strong casing arrival

Weak formation arrival



QC CBL USI VDL



**CASING  
INSPECTION  
LOG  
ULTRA SONIC PULSE ECHO**

37.80'

**AS CABLEHEAD**  
Diameter : 1.37"  
**STEEL SINGLE CONDUCTOR**  
Diameter : 5.15"

**HVTM ELECTROMECS**  
Diameter : 3.33"  
Length : 4.83"  
Weight : 141 lbs  
Series : 4892A  
Acoustic : HVTM

**HVTM 7.0 - 9.625" UPPER MODULE**  
Diameter : 5.50"  
Length : 6.83"  
Weight : 351 lbs  
Series : 4897A  
Acoustic : HVTM  
Measure Point: 4.92' : DISCRIM  
Measure Point: 4.05' : RADIAL  
Measure Point: 4.04' : AXIAL  
Measure Point: 4.03' : CIRCUM

DISCRIM : 28.16'  
RADIAL : 27.29'  
AXIAL : 27.28'  
CIRCUM : 27.27'

**HVTM 7.0 - 9.625" LOWER MODULE**  
Diameter : 5.50"  
Length : 6.85"  
Weight : 355 lbs  
Series : 48970A  
Acoustic : HVTM  
Measure Point: 4.89' : DISCRIM  
Measure Point: 4.03' : RADIAL  
Measure Point: 4.02' : AXIAL  
Measure Point: 4.01' : CIRCUM

DISCRIM : 21.28'  
RADIAL : 20.42'  
AXIAL : 20.41'  
CIRCUM : 20.40'

**WIGGLE JOINT**  
Diameter : 2.88"

**STEEL BAR 3.15" - STEEL**  
Diameter : 3.38"  
Length : 15.21'  
Weight : 180 lbs  
Series : 5914M  
Acoustic : SMB

**BULL PLUG 3.38"**

0.00'

TOTAL LENGTH : 37.80'  
TOTAL WEIGHT : 1077 lbs  
MAX DIAMETER : 0'5.50"



120	3717.27	3748.78	31.51	Class 4	86.0%	3734.99	OD
121	3748.78	3780.85	32.07	Class 2	37.0%	3769.98	OD
122	3780.85	3812.51	31.66	Class 1	-	-	-
123	3812.51	3842.32	29.81	Class 2	35.0%	3831.18	OD
124	3842.32	3872.46	30.14	Class 1	-	-	-
125	3872.46	3903.25	30.79	Class 1	-	-	-
126	3903.25	3934.20	30.95	Class 2	21.0%	3933.02	OD
127	3934.20	3964.22	30.02	Class 2	27.0%	3936.23	OD
128	3964.22	3995.68	31.46	Class 2	25.0%	3983.94	OD
129	3995.68	4026.51	30.83	Class 2	34.0%	3998.32	OD
130	4026.51	4058.66	32.15	Class 1	-	-	-
131	4058.66	4089.46	30.80	Class 1	-	-	-
132	4089.46	4118.75	29.29	Class 1	-	-	-
133	4118.75	4150.33	31.58	Class 1	-	-	-
134	4150.33	4182.43	32.10	Class 2	25.0%	4151.22	OD
135	4182.43	4214.13	31.70	Class 2	27.0%	4183.00	OD
136	4214.13	4244.49	30.36	Class 4	91.0%	4225.45	OD
137	4244.49	4275.98	31.49	Class 1	-	-	-
138	4275.98	4307.03	31.05	Class 1	-	4307.96	OD
139	4307.03	4338.36	31.33	Class 2	36.0%	-	-
140	4338.36	4369.93	31.57	Class 1	-	-	-
141	4369.93	4399.55	29.62	Class 2	31.0%	4376.39	OD
142	4399.55	4431.63	32.08	Class 2	25.0%	4412.97	OD
143	4431.63	4462.94	31.31	Class 1	-	-	-
144	4462.94	4492.40	29.46	Class 3	49.0%	4463.44	OD
145	4492.40	4524.61	32.21	Class 4	70.0%	4493.28	OD
146	4524.61	4555.95	31.34	Class 1	-	-	-
147	4555.95	4576.27	20.32	Class 1	-	-	-

File 20190308\_11065A\_RSP\_0\_0\_0\_0\_0\_0\_0\_0.mvl

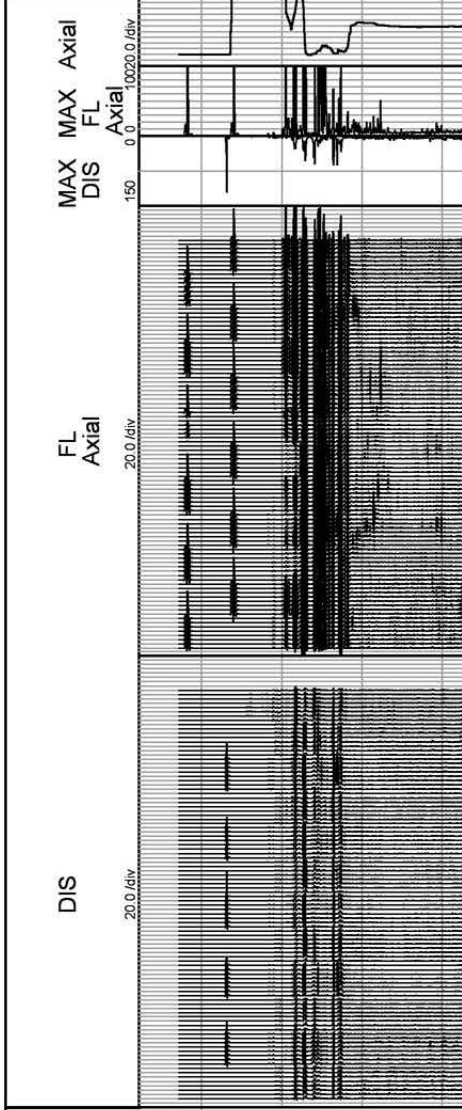
### Main Section 5in / 100ft - Scale

Class 1  
0 - 20%

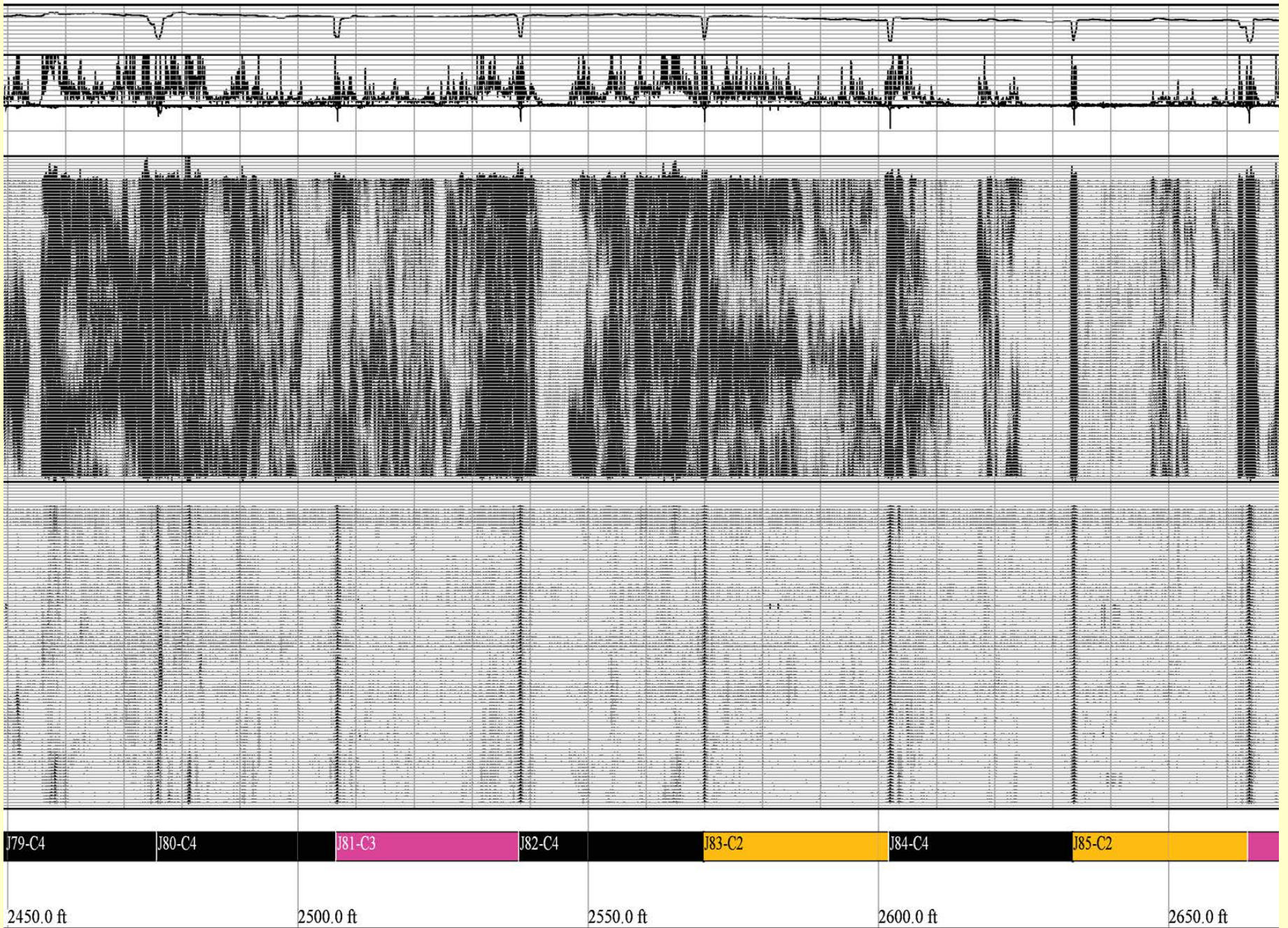
Class 2  
20 - 40%

Class 3  
40 - 60%

Class 4  
60 - 100%



0.0 ft





**CASING  
INSPECTION  
LOG  
CALIPER LOG**

# JOINT ANALYSIS REPORT WITH PIPE GRADE

PIONEER

**Company:** \_\_\_\_\_  
**Well:** \_\_\_\_\_  
**Field:** \_\_\_\_\_ N  
**County:** \_\_\_\_\_  
**State:** TEXAS  
**Date:** 9/23/2018

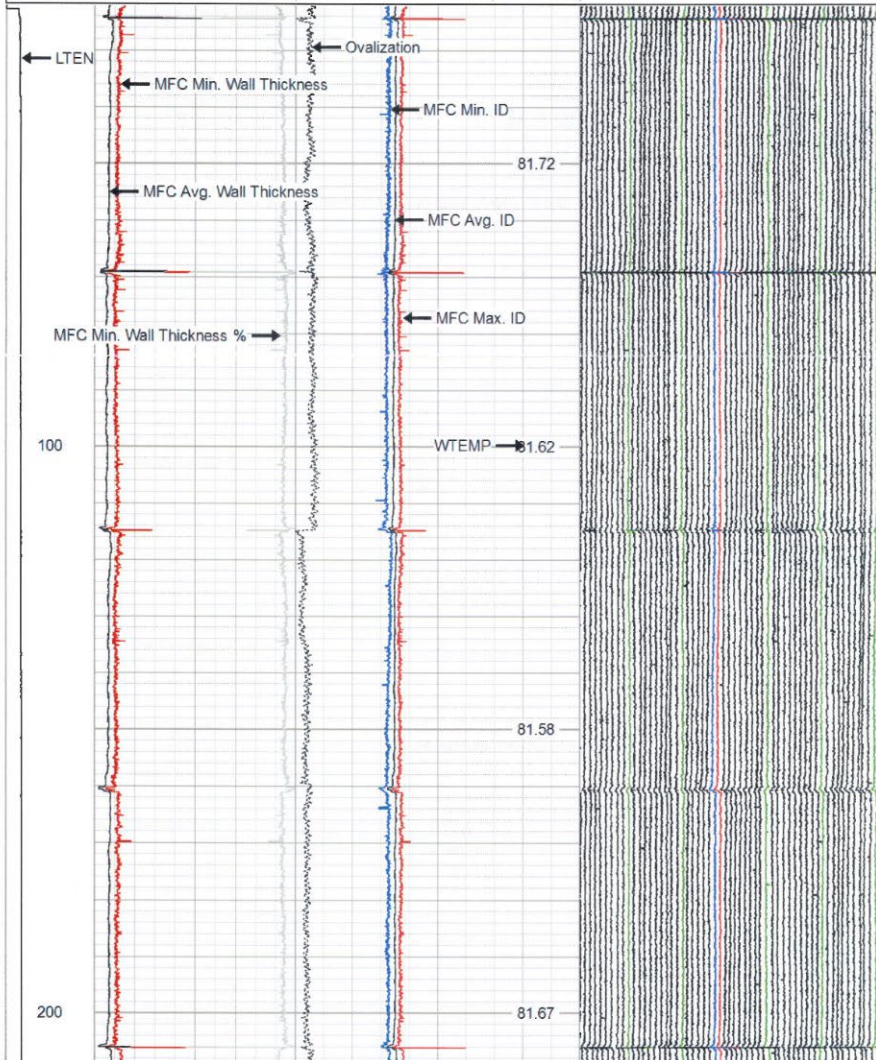
9.625" - 47#		Other WT	GRADE
0.0%	15.0%	0% to 15%	A
15.0%	30.0%	15.1% to 30%	B
30.0%	50.0%	30.1% to 50%	C
	50.0%	> 50.1%	F

**Comment:**

Joint No.	Depth Feet	Length Feet	Max Pen %	Max Pen Depth	Max ID Inches	Min Wall Inches	Nominal ID Inches	Weight lb/ft	Pipe Grade	Theoretical Burst Press	Comment
113	4957.22	44.12	14.5%	4988.30	8.818	0.404	8.681		A		
114	5002.34	43.27	11.5%	5005.07	8.790	0.418	8.681		A		
115	5046.62	44.28	12.6%	5048.55	8.800	0.412	8.681		A		
116	5091.90	43.90	12.3%	5134.69	8.797	0.414	8.681		A		
117	5136.80	44.90	13.1%	5166.99	8.805	0.410	8.681		A		
118	5182.70	46.15	15.5%	5182.69	8.827	0.399	8.681		B		
119	5229.85	43.67	14.9%	5261.47	8.822	0.402	8.681		A		
120	5274.52	44.20	15.0%	5309.10	8.823	0.401	8.681		B		
121	5319.71	44.69	10.2%	5351.12	8.777	0.424	8.681		A		
122	5365.40	43.10	12.8%	5401.94	8.802	0.411	8.681		A		
123	5409.50	43.35	12.8%	5427.32	8.802	0.411	8.681		A		
124	5453.85	33.73	13.1%	5454.34	8.805	0.410	8.681		A		
125	5488.58	46.18	12.8%	5499.85	8.802	0.411	8.681		A		
126	5535.75	44.12	15.4%	5559.70	8.826	0.399	8.681		B		
127	5580.88	44.25	16.8%	5590.40	8.840	0.392	8.681		B		
128	5626.12	43.88	13.7%	5664.59	8.810	0.407	8.681		A		
129	5671.00	42.93	10.6%	5702.37	8.781	0.422	8.681		A		
130	5714.92	44.31	15.8%	5751.77	8.830	0.398	8.681		B		
131	5760.23	43.09	14.2%	5801.64	8.815	0.405	8.681		A		
132	5804.32	46.09	11.2%	5825.69	8.787	0.419	8.681		A		
133	5851.41	43.63	11.1%	5892.57	8.786	0.419	8.681		A		
134	5896.04	43.61	14.9%	5899.09	8.822	0.402	8.681		A		
135	5940.64	43.73	12.2%	5959.35	8.796	0.415	8.681		A		
136	5985.37	45.05	16.6%	6014.52	8.838	0.393	8.681		B		
137	6031.42	43.16	14.2%	6044.40	8.815	0.405	8.681		A		
138	6075.58	41.89	14.9%	6076.39	8.822	0.402	8.681		A		
139	6118.47	44.44	17.2%	6140.34	8.843	0.391	8.681		B		
140	6163.91	44.98	18.5%	6203.24	8.856	0.385	8.681		B		
141	6211.37	42.89	18.4%	6245.07	8.855	0.385	8.681		B		DV Tool 6208' - 6211'
142	6255.25	8.42	15.3%	6259.62	8.825	0.400	8.681		B		
143	6264.67	11.15	13.6%	6269.25	8.809	0.408	8.681		A		
144	6276.82	15.56	14.9%	6281.57	8.822	0.402	8.681		A		
145	6293.38	14.66	12.6%	6307.64	8.800	0.412	8.681		A		
146	6309.04	15.53	12.0%	6313.95	8.794	0.416	8.681		A		
147	6325.58	13.92	13.9%	6336.62	8.812	0.406	8.681		A		
148	6340.50	15.49	17.4%	6341.59	8.845	0.390	8.681		B		
149	6356.98	13.82	12.2%	6367.69	8.796	0.415	8.681		A		
150	6371.81	15.45	14.0%	6375.14	8.813	0.406	8.681		A		
151	6388.26	14.03	13.8%	6401.94	8.811	0.407	8.681		A		
152	6403.29	15.40	14.7%	6407.20	8.820	0.403	8.681		A		
153	6419.69	15.40	13.3%	6433.27	8.807	0.409	8.681		A		
154	6436.09	7.84	16.1%	6442.52	8.833	0.396	8.681		B		

Database File: ...\_mipd.db  
 Dataset Pathname: ...  
 Presentation Format: dc\_mfc\_56arm\_8-10in\_3in\_p1  
 Dataset Creation: Tue Sep 25 09:58:06 2018  
 Charted by: Depth in Feet scaled 1:240

LTEN	MFC Min. Wall Thickness	8	MFC Min. ID (in)	10	56 RADII 0.0536 INC. 3" SCALE
0 (lb2000)	0.5 (in)	0	MFC Avg. ID (in)	10	FINGER 01
	MFC Min. Wall Thickness	8	MFC Max. ID (in)	10	FINGER 56
	0	100	Ovalization (in)	0.5	
	MFC Avg. Wall Thickness		WTEMP		
	0.5 (in)	0	(degF)		



# **Temperature, Radioactive Tracer, and Noise Logging for Injection Well Integrity**

by

**R. M. McKinley**  
Exxon Production Research

**Cooperative Agreement No. CR-818926**

**Project Officer**

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Ada, Oklahoma 74820

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ADA, OKLAHOMA 74820**

**A GOOD  
MANUAL  
TO HAVE  
ON  
HAND**

# **RADIOACTIVE TRACER SURVEYS**

**(RATS or RTS)**

# RADIOACTIVE TRACER SURVEY PURPOSE

- FLOW **PROFILING** (volumetric)
- DETERMINE FLUID **MIGRATION**
  - **BOTTOMHOLE CEMENT CHANNELS**  
(Time Drive)
  - **CASING, TUBING, PACKER LEAKS**  
(Internal MI)(Slug Chase)

# RATS

## OPERATION PRINCIPLES


- **USE RADIOACTIVE IODINE** (1/2 life = 8 days)
- **EJECT TRACER @** surface or downhole
- **FOLLOW TRACER** as it travels
- **USE GAMMA RAY TOOL** as detector
- **DETECT MIGRATION** OF TRACER through tubing and/or casing

# RATS EQUIPMENT

- Radioactive material **EJECTOR**  
Surface or downhole
- 2 or more Gamma Ray **DETECTORS**
- Ejector/Detector **CONFIGURATION** varies depending on objective
- Tool **DIAMETER** as small as 1-1/2 inches



# RATS PROCEDURE

- **LOAD TRACER** at surface
  - **RUN** tool in tubing or casing
  - **RUN BASE LOG** with well on injection
  - **EJECT** tracer at or near surface if running in casing
  - **EJECT** tracer above the packer if in tubing
  - **FOLLOW** tracer to injection zone, while checking for leaks
  - **LOG ABOVE PERFORATIONS/SCREEN** for channels outside casing
  - Can check **FLOW PROFILE** with Spinner
  - Run with **CASING COLLAR LOCATOR**
- 

# FACTORS AFFECTING GAMMA-RAY MEASUREMENT

- **RADIOACTIVE (HOT) formations**
- **INJECTION RATE**
- **Ejector/Detector CONFIGURATION**
- **PIPE SCALE**

1-3/8" O.D.

RESERVOIR &  
POSITIVE  
DISPLACEMENT  
EJECTOR

EJECTOR  
MOTOR

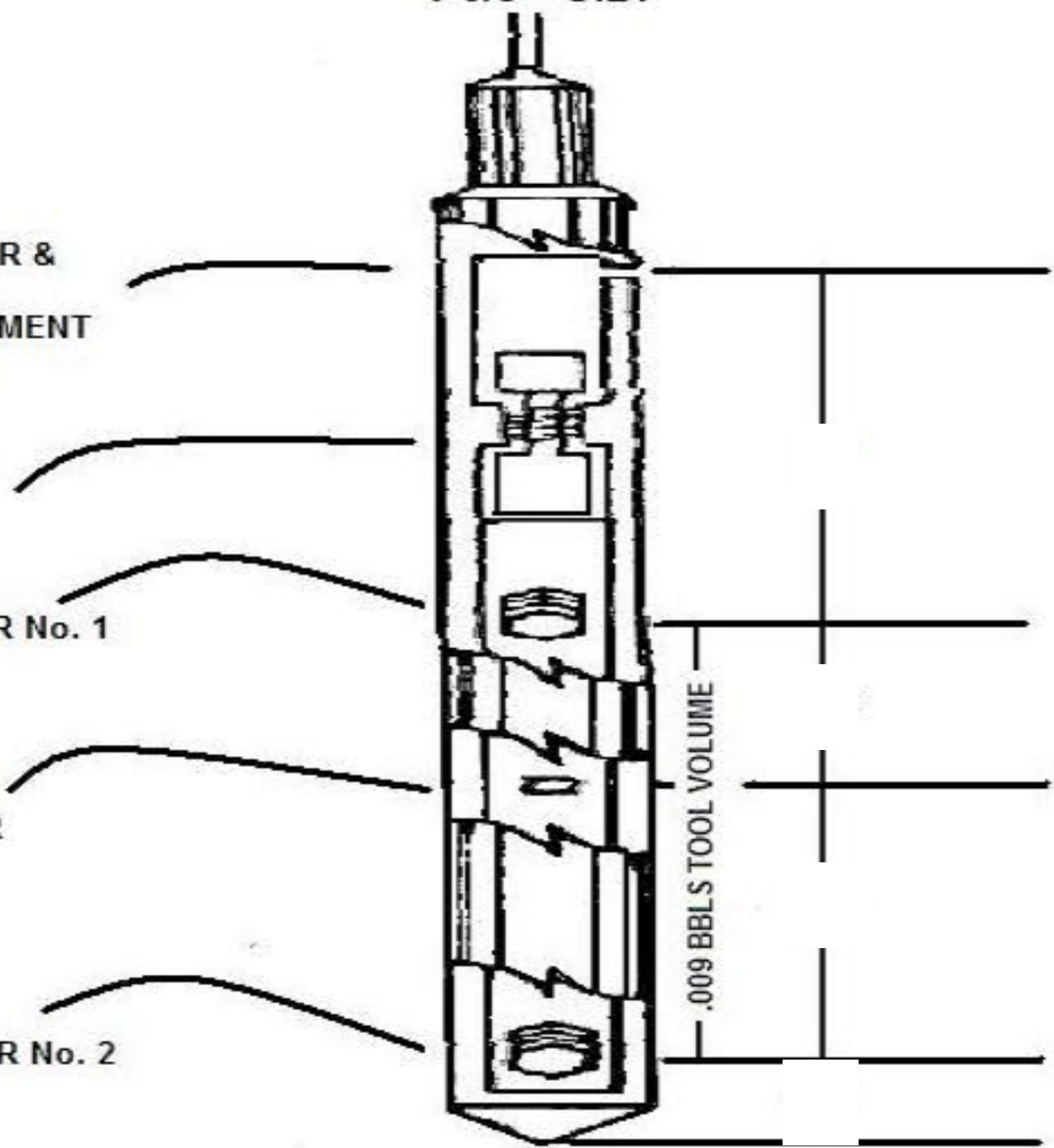
GAMMA  
DETECTOR No. 1

CASING  
COLLAR  
LOCATOR

GAMMA  
DETECTOR No. 2

.009 BBLS TOOL VOLUME

***SCHEMATIC OF RADIOACTIVE TRACER FOR INJECTION LOGGING***



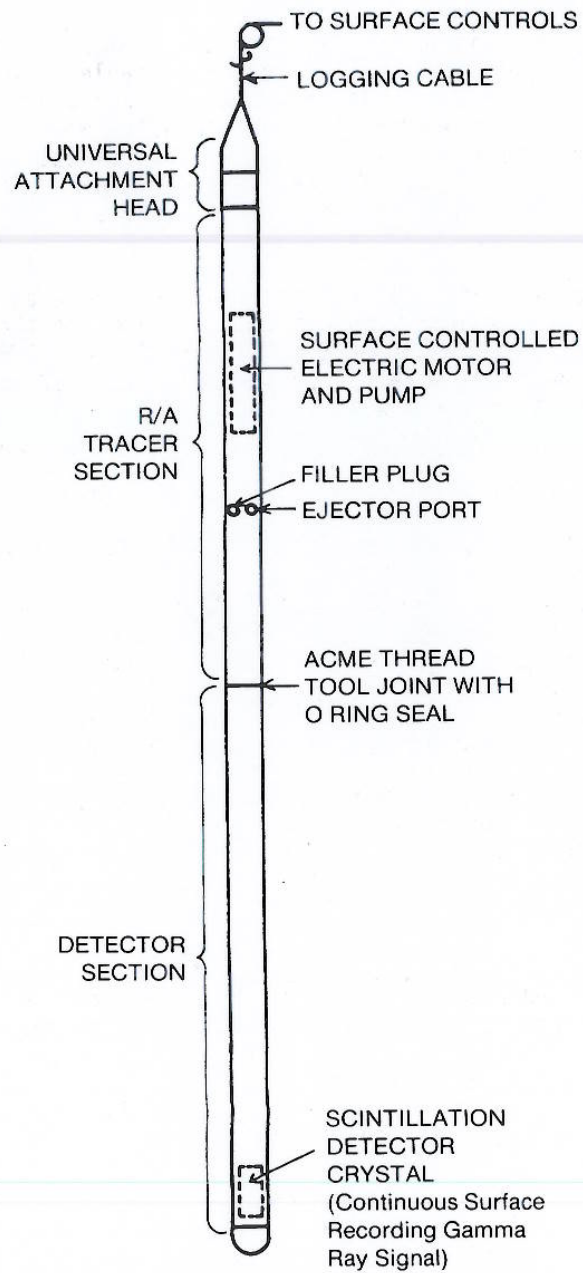


Figure 73. Radioactive tracer tool (Ford, 1962).

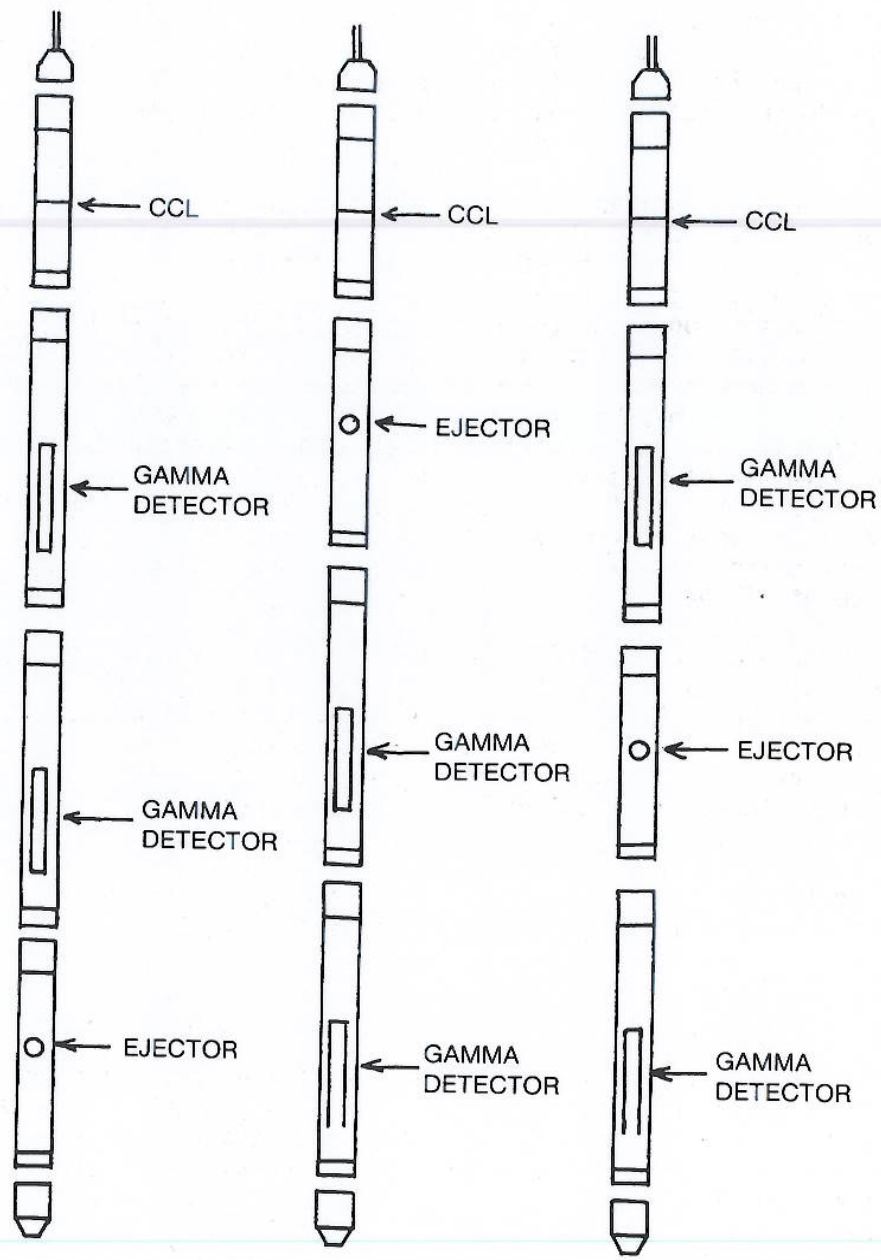
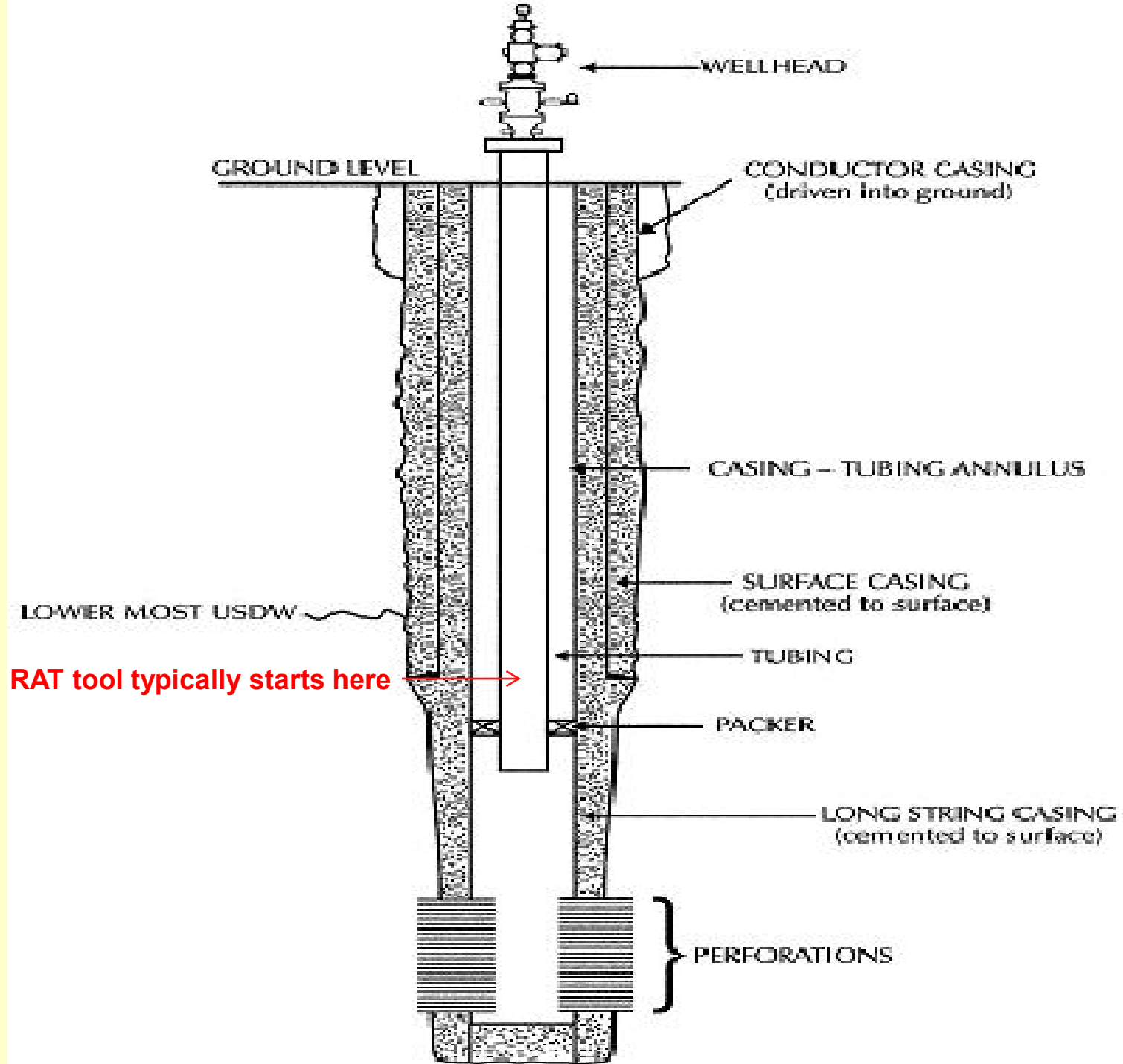


Figure 74. Three possible configurations of a radioactive tracer tool (courtesy Schlumberger) (Dewan, 1982).

# Slug Chase (Internal MI)



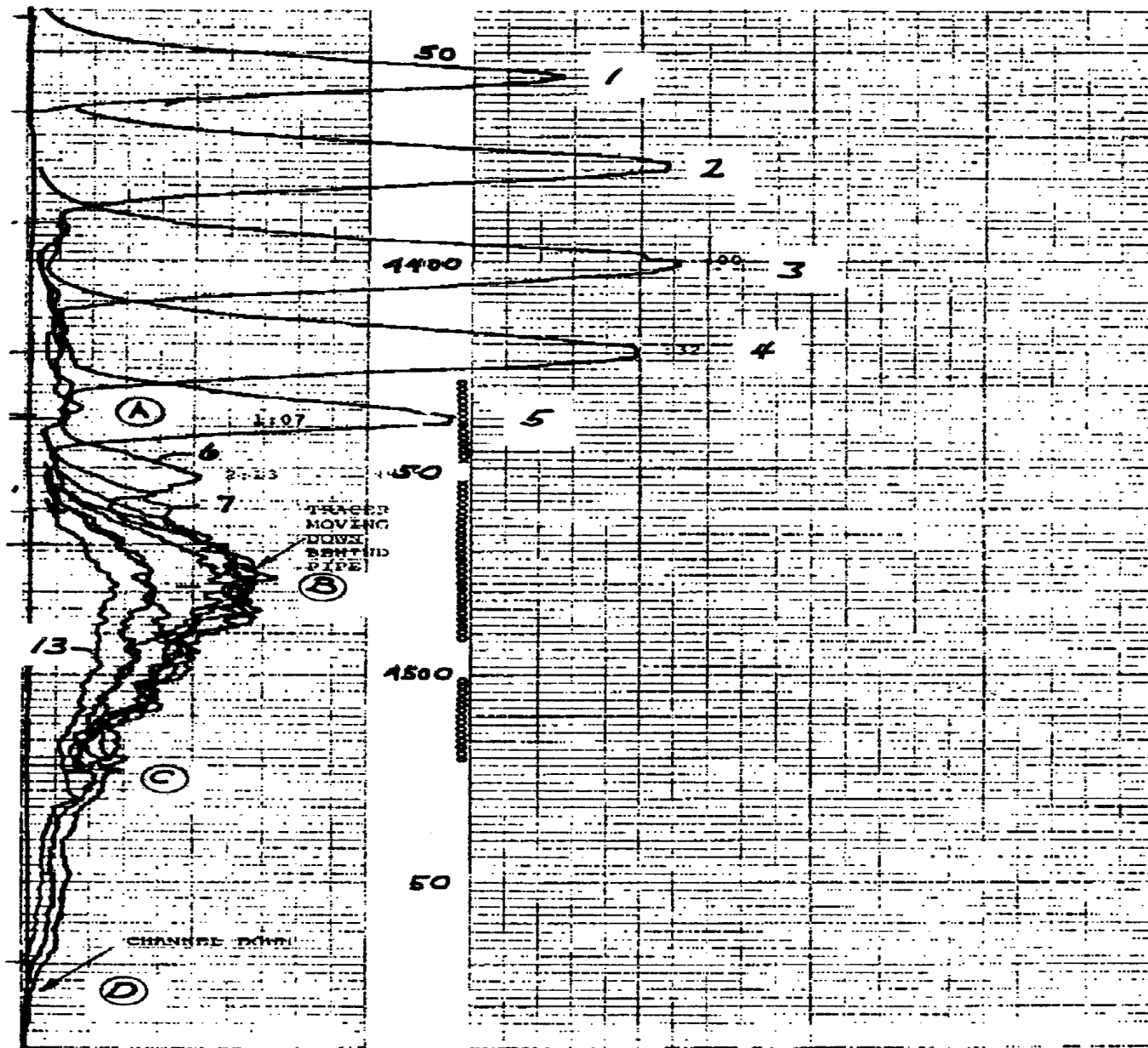


Figure 41. Slug-tracking survey from well on injection at 950 BPD



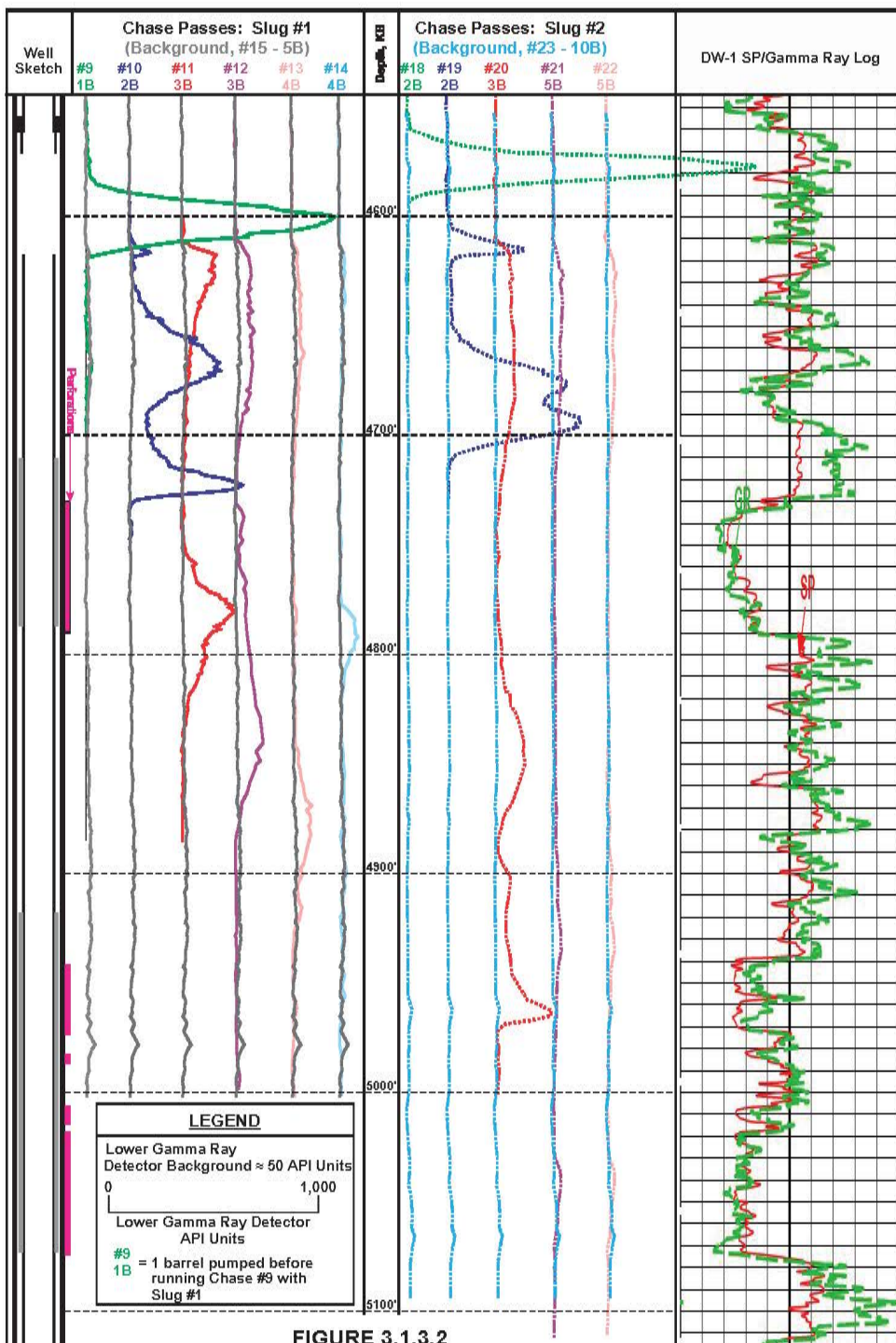
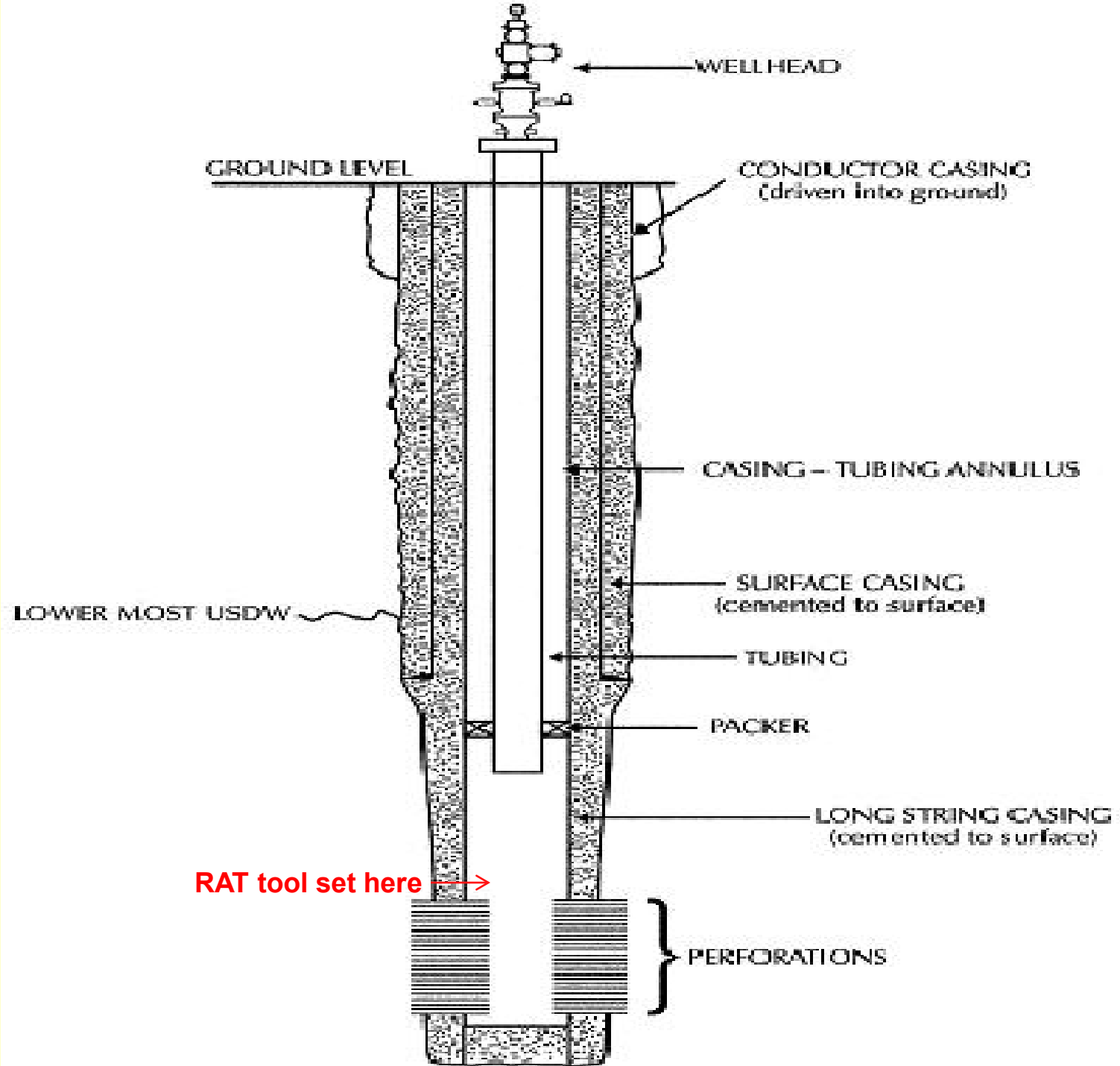


FIGURE 3.1.3.2

# **TIME DRIVES**

**(Test Bottomhole Cement)**



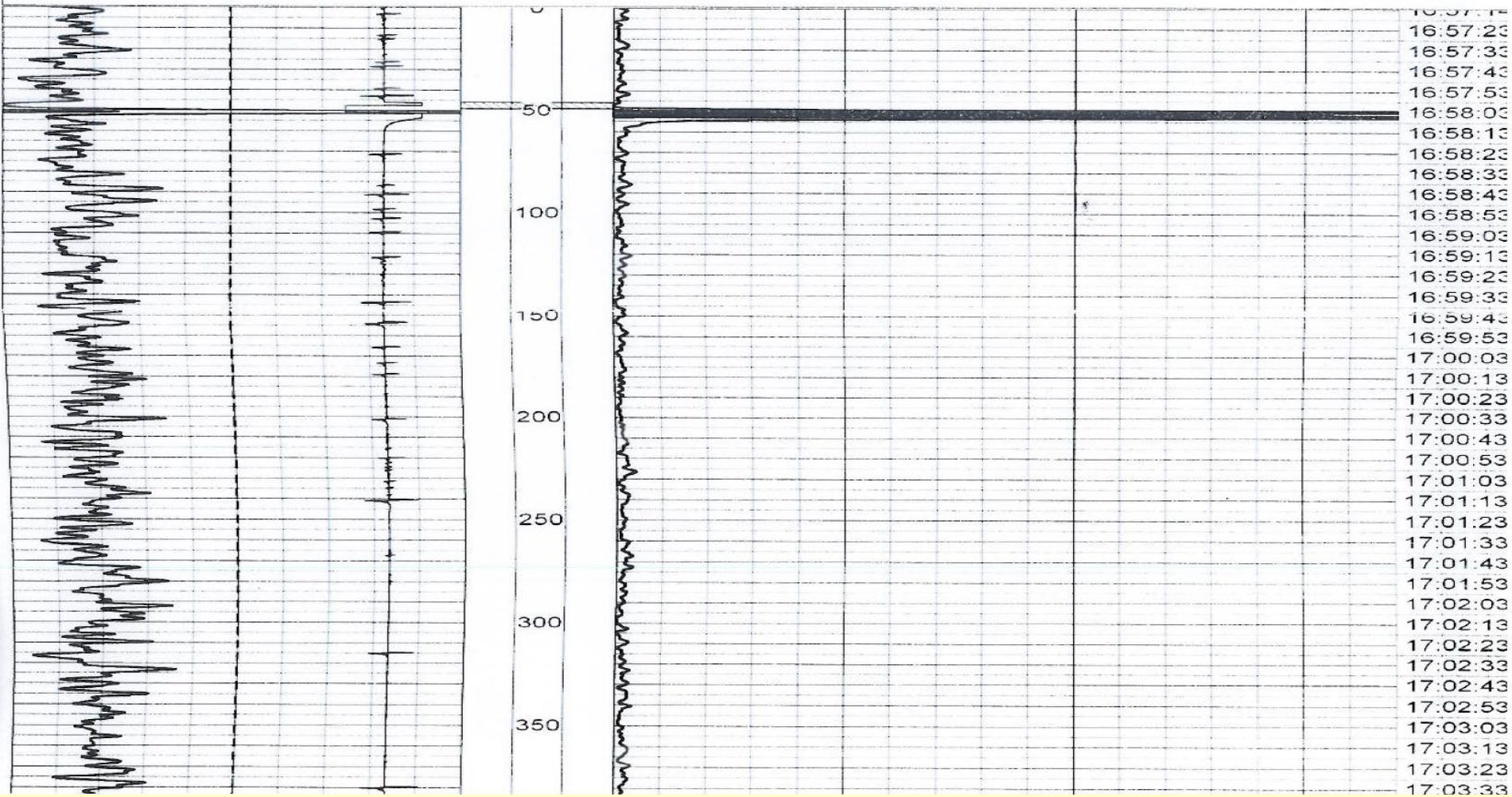
# Gulf Coast Well Analysis

TIME DRIVE # 2 EJECTED AT 7395' AT 16:58

UPPER DETECTOR AT 7392' LOWER DETECTOR AT 7400'  
INJECTION RATE 200 GPM AT 180 PSI

Database File: XXXXXXXXXX  
 Dataset Pathname: pass20  
 Presentation Format: tracer  
 Dataset Creation: Fri Jul 13 16:57:14 2012 by Log PIP Casedhole Loggi  
 Charted by: Time scaled 72"/hour

0	GAMMA RAY (GAPI)	100	0	EJECT	1	0	LOWER DETECTOR (GAPI)	100
500	CCL	-100						TOD (sec)
-100	LSPD (ft/min)	100						

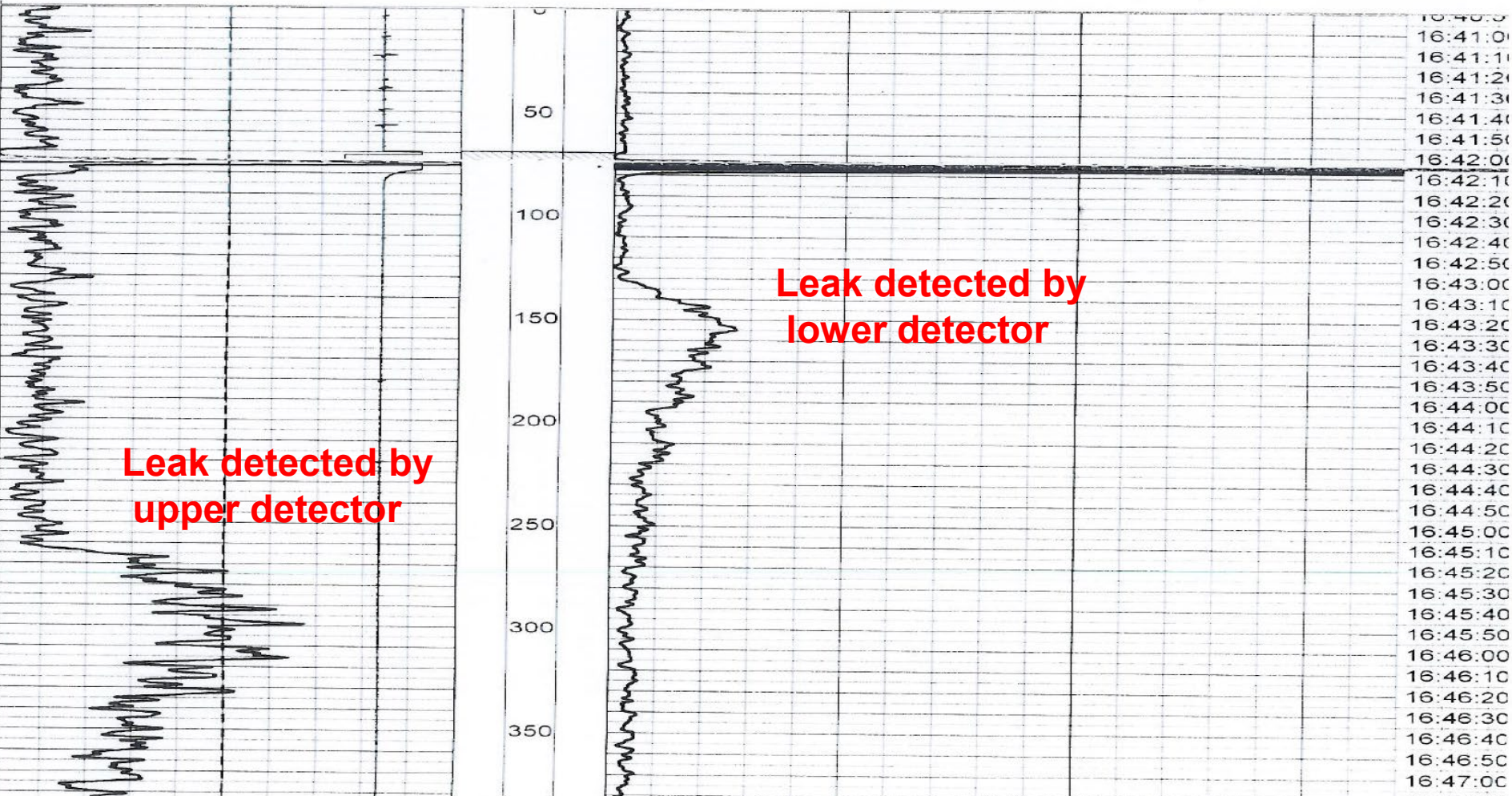


# Gulf Coast Well Analysis

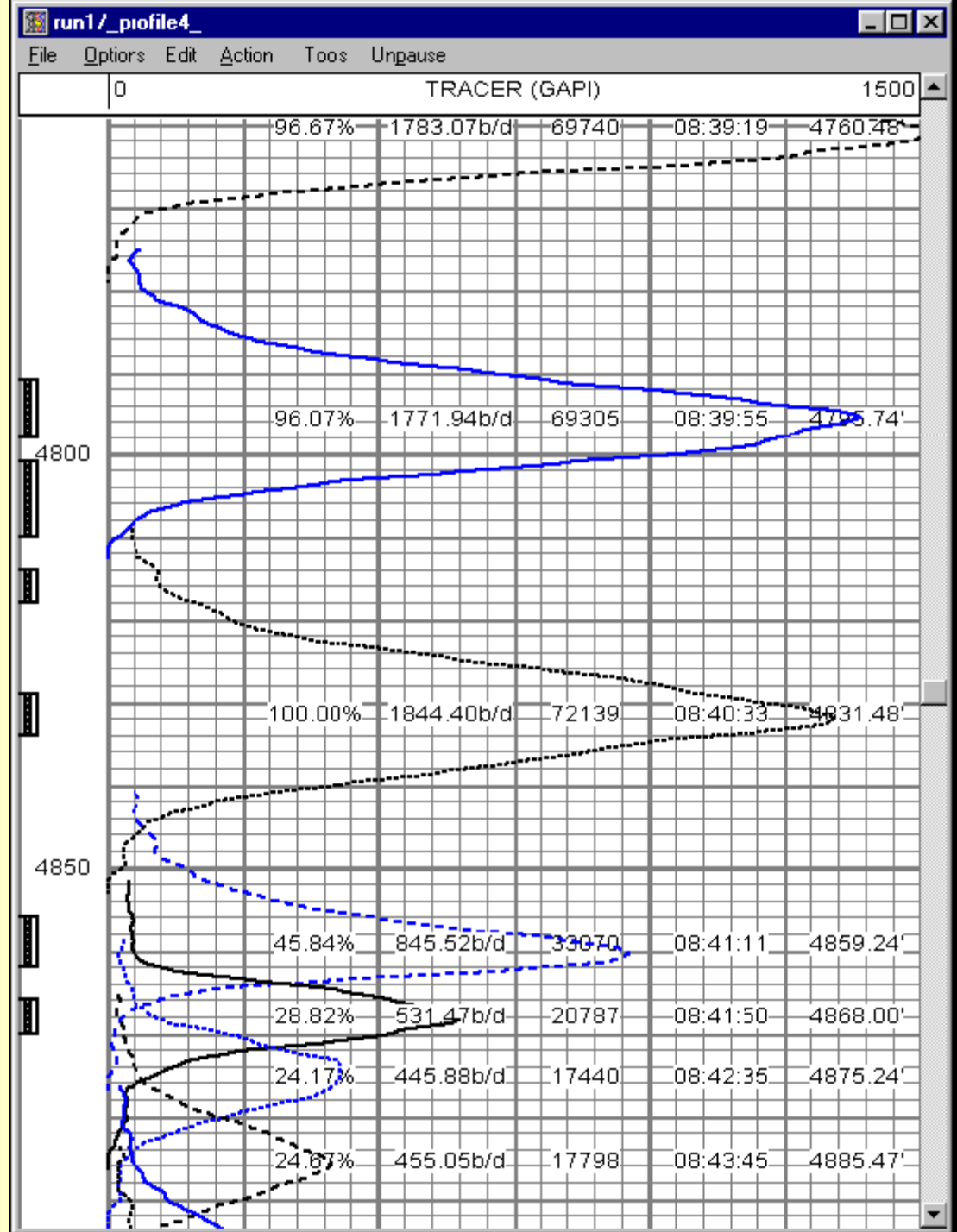
TIME DRIVE # 1 EJECTED AT 7435' AT 16:42  
 UPPER DETECTOR AT 7432' LOWER DETECTOR AT 7440'  
 INJECTION RATE 200 GPM AT 100 PSI

Database File: [REDACTED]  
 Dataset Pathname: pass18  
 Presentation Format: tracer  
 Dataset Creation: Fri Jul 13 16:40:50 2012 by Log PIP Casedhole Loggi  
 Charted by: Time scaled 72"/hour

0	GAMMA RAY (GAPI)	100	0 EJECT	1 0	LOWER DETECTOR (GAPI)	10
500	CCL	-100				TOD (se
-100	LSPD (ft/min)	100				



# Flow Profiles

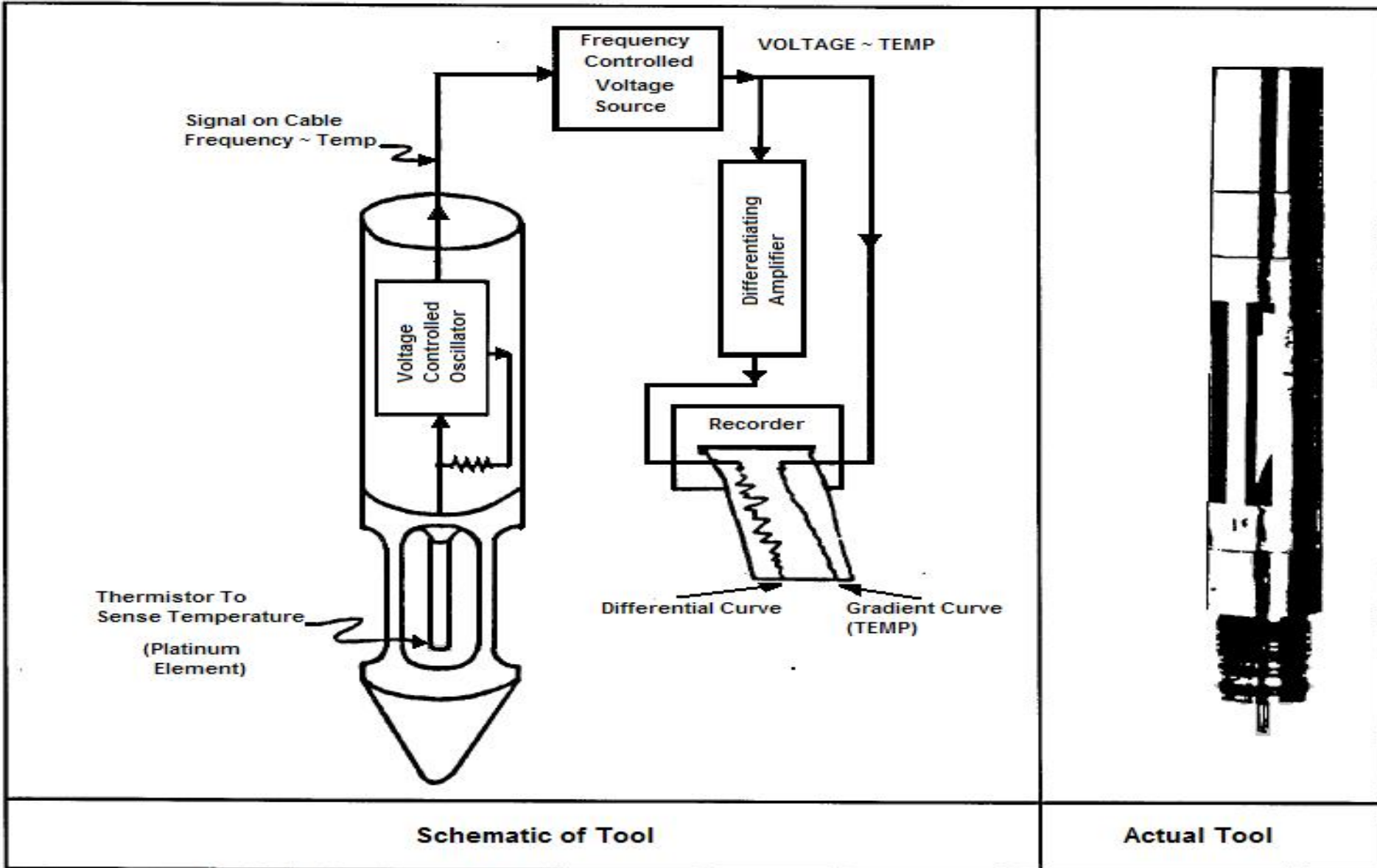


# TEMPERATURE SURVEYS (External MI)

# TEMPERATURE SURVEYS

- Oldest of the Production Surveying Instruments (mid 1930s)
  - Mercury/piston
  - Vapor pressure/bourdon type element (Bottomhole temperature measurements)
  - Thermistor – platinum element – resolves temperature changes of 0.05 deg F
    - » **Analog Logging Units**
    - » **Digital Logging Units**





**A surface recording, continuous thermometer**



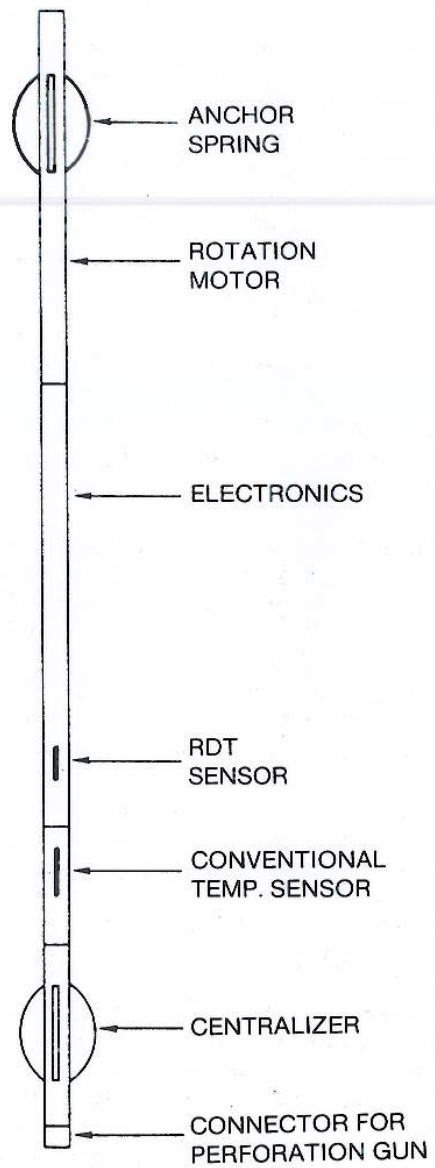


Figure 16. Schematic of RDT logging tool (Cooke, 1978).

# TEMPERATURE SURVEY PURPOSE

- LOCATE **CEMENT TOPS** AFTER PRIMARY CEMENTING (HEAT FROM EXOTHERMIC REACTION)
- **FLUID MIGRATION** DETERMINATION
  - CASING SHOE BEHIND PIPE
  - TUBING, CASING, PACKER LEAKS
  - INTERFORMATIONAL FLUID FLOW
- **FLOW** (VOLUMETRIC) **PROFILING** (RARE)
- **IDENTIFICATION OF** INTERVALS PRODUCING **GAS** (COOLING EFFECT FROM EXPANSION)

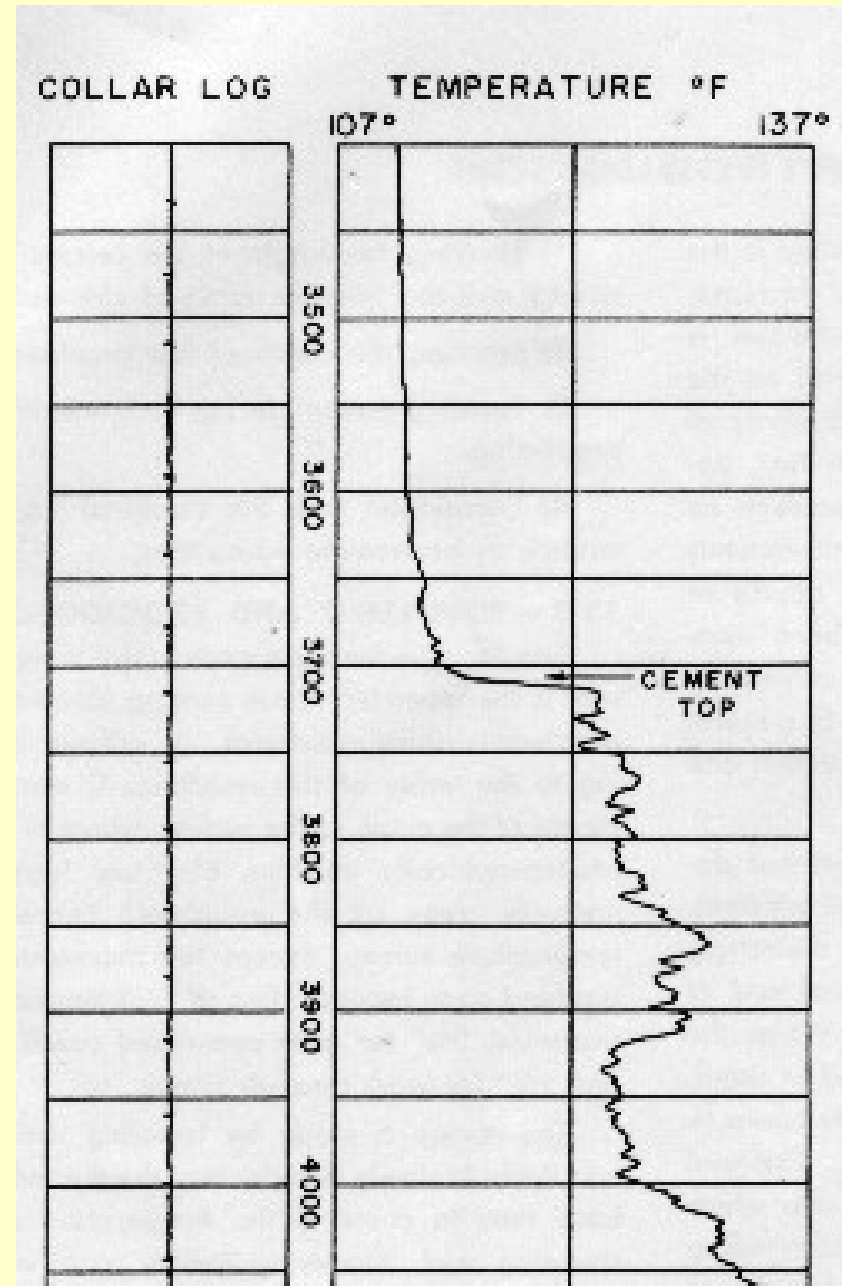
# TEMPERATURE SURVEY OPERATION PRINCIPLE

- DOWNHOLE TEMPERATURE GOVERNED BY **GEOHERMAL GRADIENT**
- INJECTION OF FLUID WITH LARGE **TEMPERATURE DIFFERENCE** (FROM GRADIENT)
- **ZONES** (OR LEAKS) TAKING INJECTED FLUIDS WILL **RETURN** TO GEOHERMAL GRADIENT AT A **SLOWER RATE**

- Since cement gives off heat as it cures, the temperature log was used to provide evidence that the well was actually cemented to a level that met expectations. An example is shown at right.

- The top of cement is located where the temperature returns to geothermal gradient.

- The log must be run during the cement curing period as the temperature anomaly will fade with time.



# TEMP SURVEY – A BASIC PROCEDURE

- LET WELL **STAND IDLE** AT LEAST 24 HOURS
- RUN “**BASE LOG**” – GEOTHERMAL GRADIENT
- ENSURE INJECTION FLUID **TEMPERATURE IS SIGNIFICANTLY DIFFERENT** FROM BOTTOM-HOLE TEMPERATURE
- START **INJECTION WHILE LOGGING** HOLE (OPTIONAL)
- **SHUT-IN** AFTER PREDETERMINED VOLUME IS INJECTED
- LOG HOLE **AFTER 0, 12, AND 24 HOURS** SHUT-IN

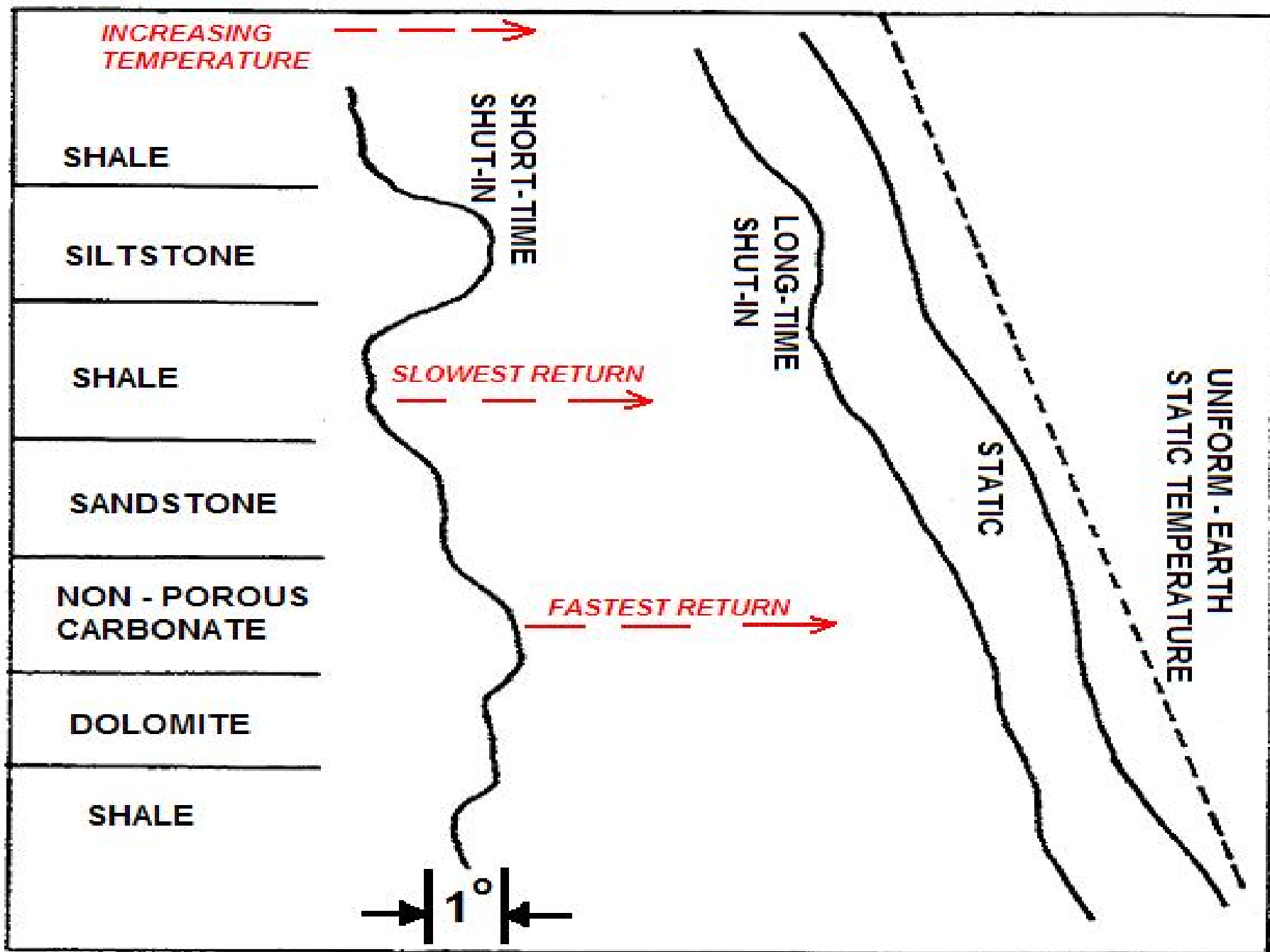
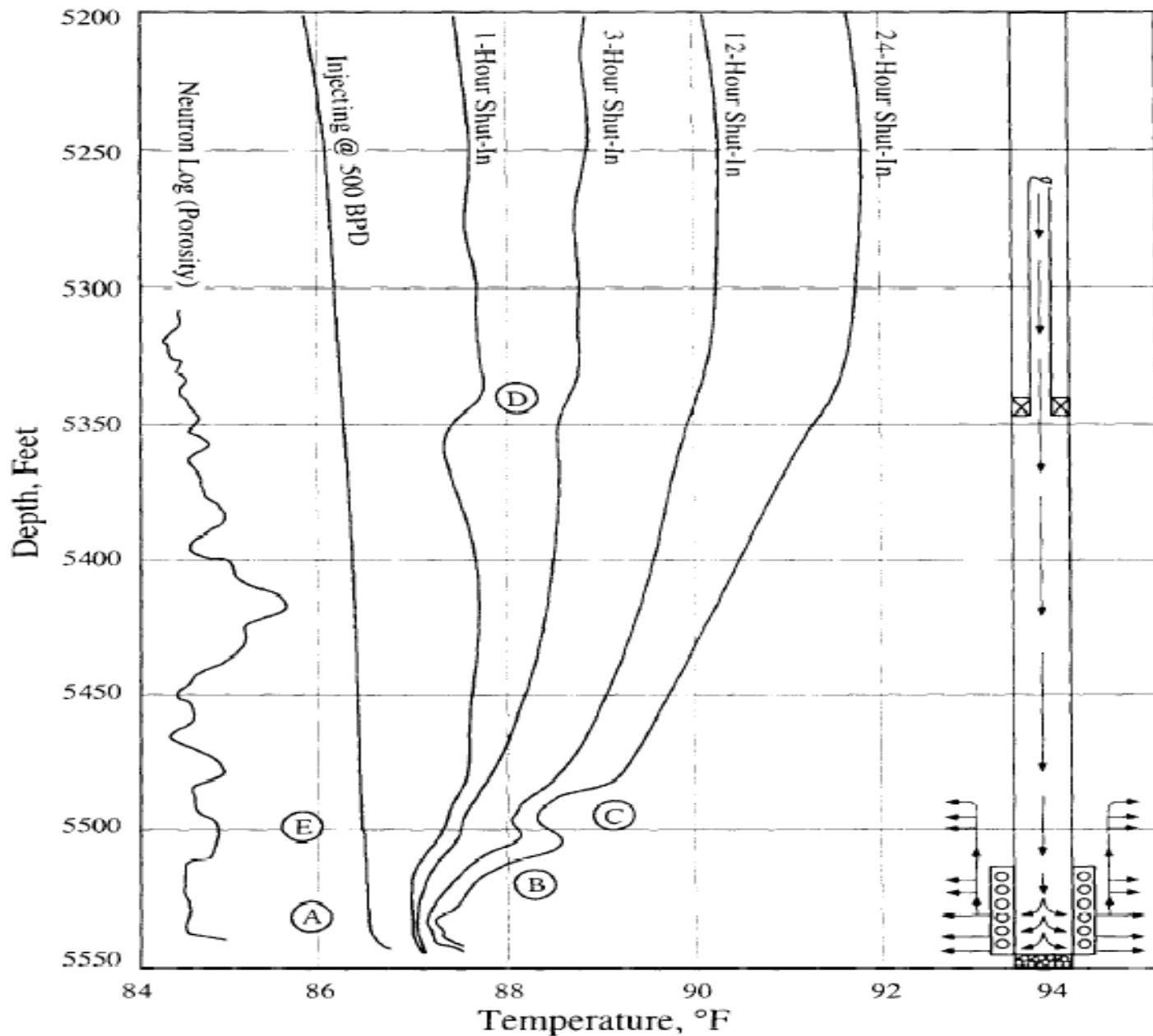


Figure 8 Hypothetical Influence of lithology on wellbore temperature warming with time to static conditions



**Figure 20. Injecting and shut-in temperature surveys from well on continuous injection at about 500 BPD for almost one year.**



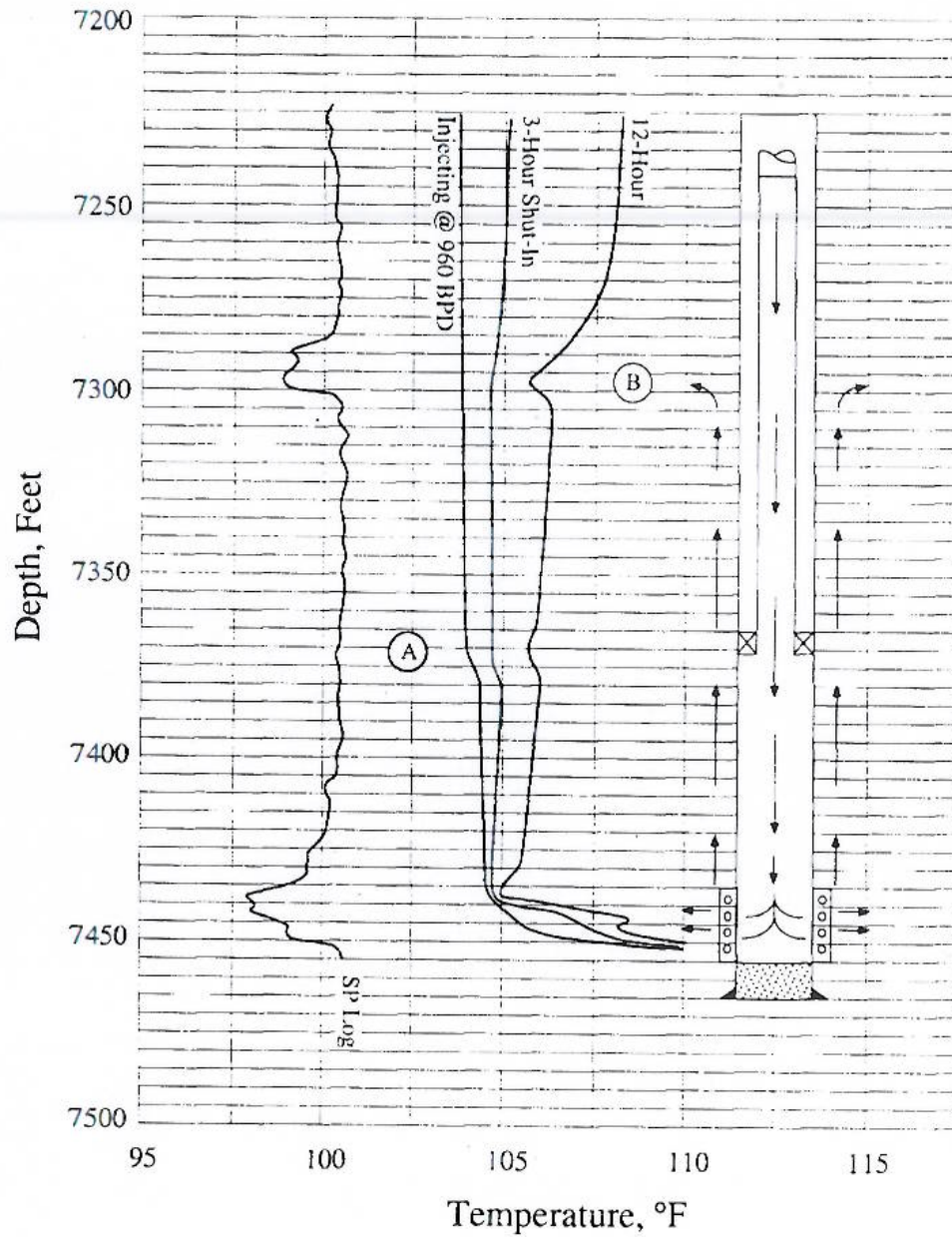


Figure 22. Temperature surveys from a well on injection at 960 BPD with flow behind pipe even on shut-in status.

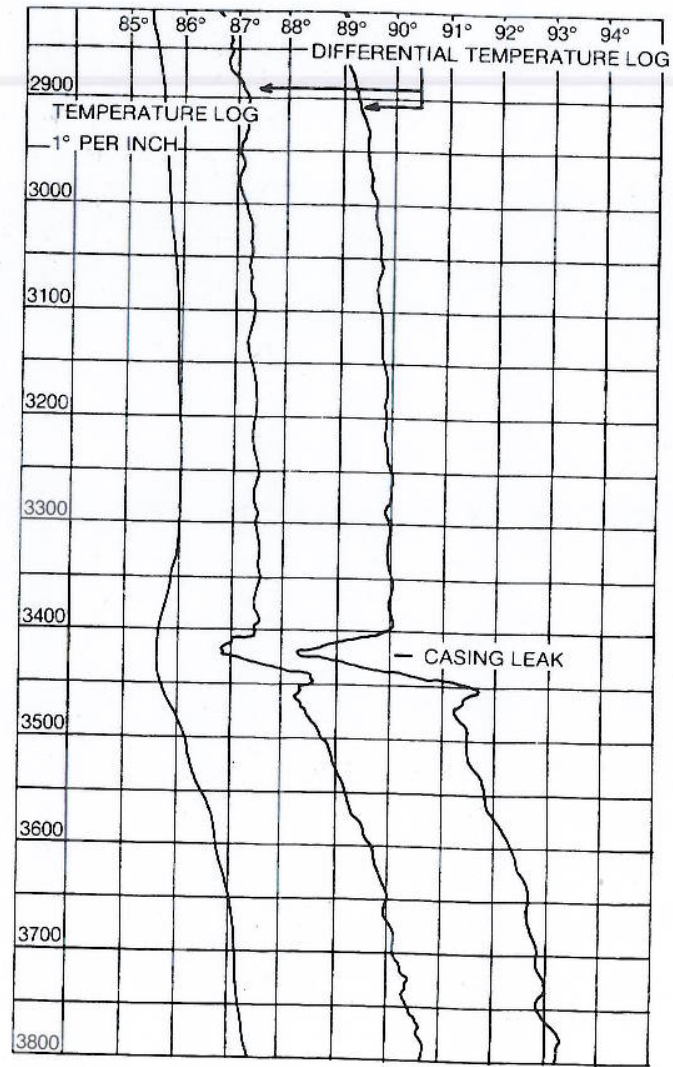
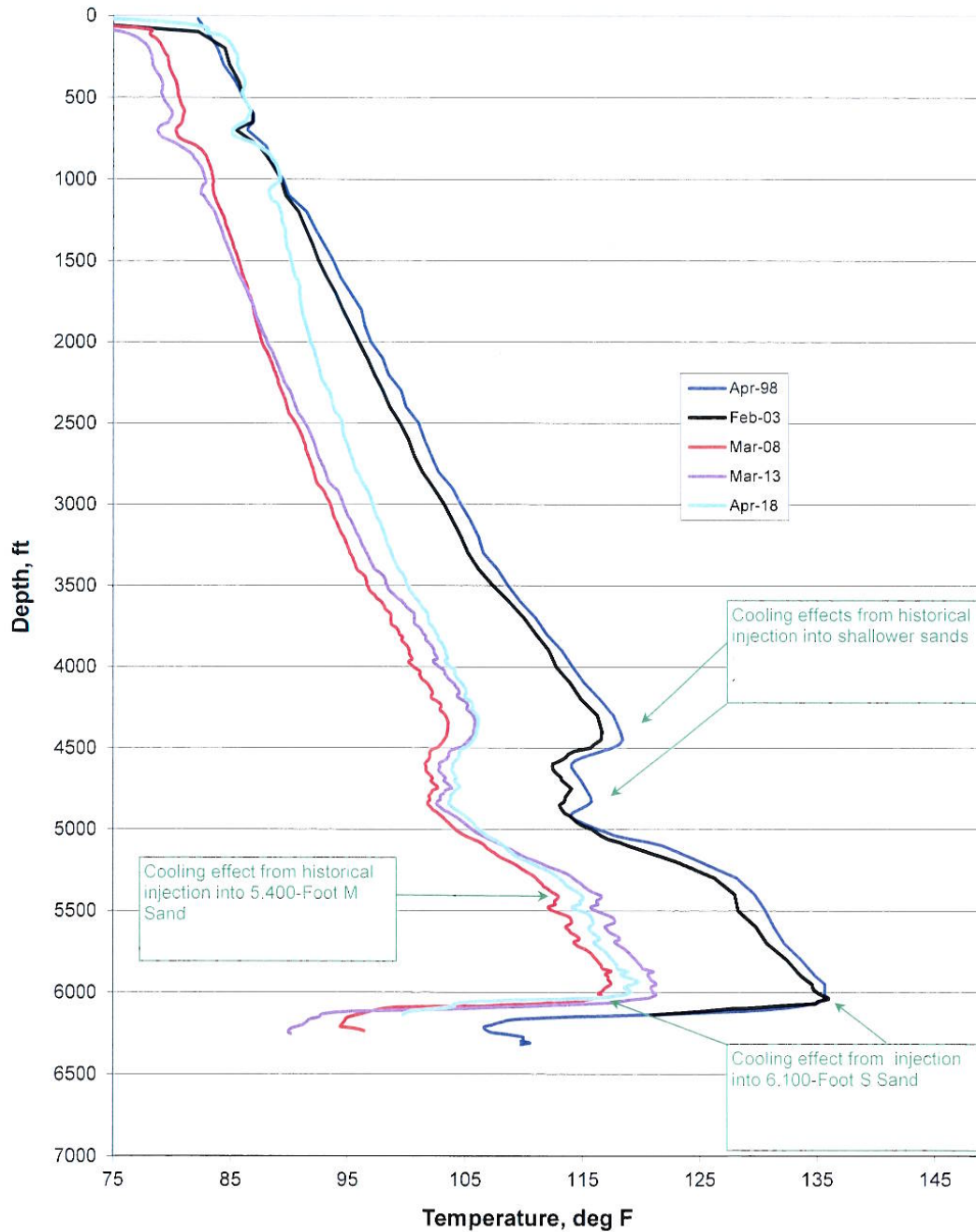
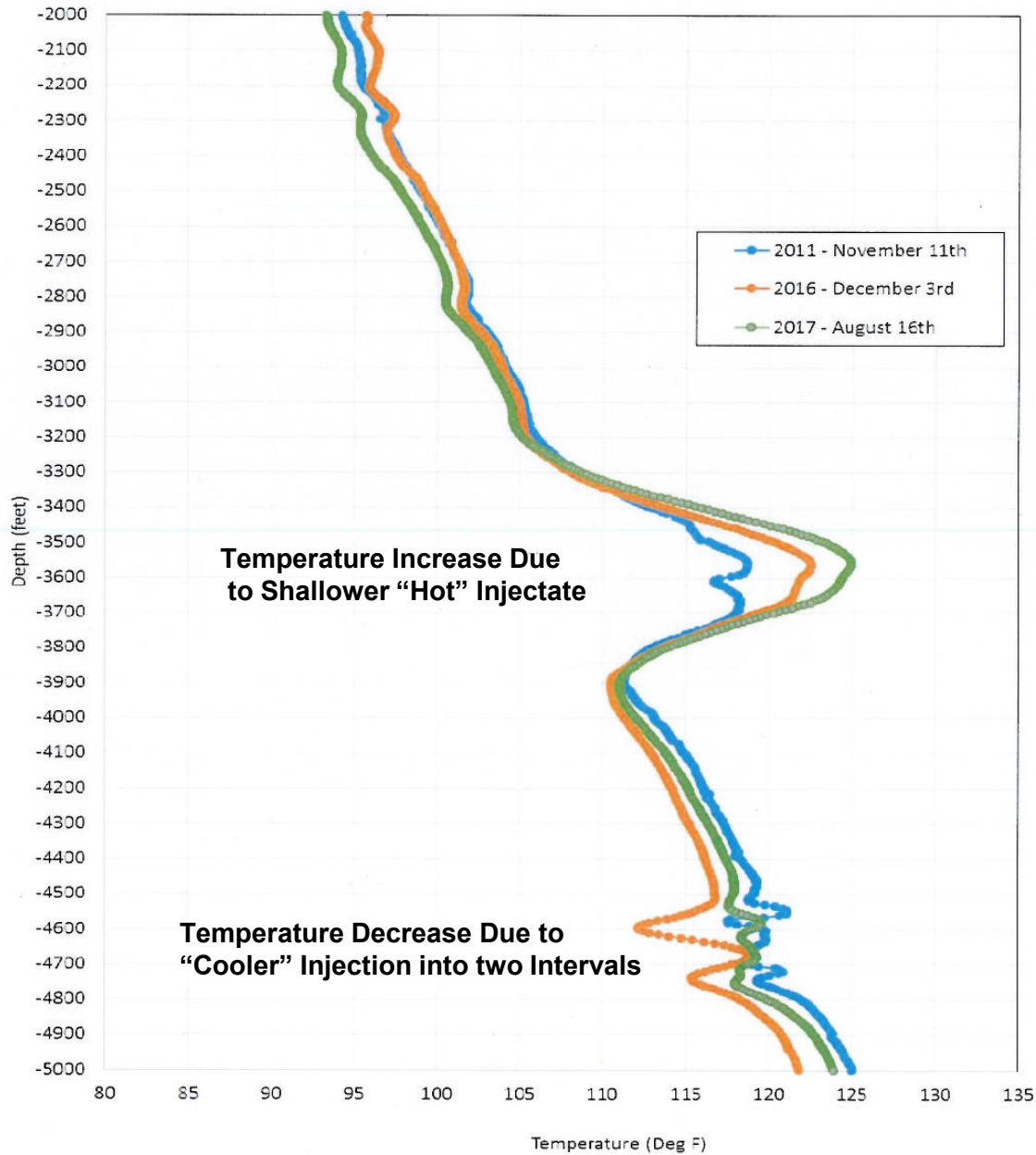


Figure 22. Temperature logs used in locating a casing leak (Peacock, 1965).

Comparison Plot of 1998, 2003, 2008, 2013, and 2018  
Temperature Surveys



### Well #1 Temperature Logs 2011, 2016 & 2017



# **NOISE LOG**

## **(External MI)**

# NOISE LOG PURPOSE

- TO **“HEAR” FLUID FLOW**  
OCCURRING INSIDE OR OUTSIDE  
WELL TUBULARS
  - ✓ BEHIND CASING CHANNELS (water flow pressure drop OR gas thru liquid)
  - ✓ TUBING AND/OR CASING LEAKS

# NOISE LOG OPERATION PRINCIPLES

- FLUID TURBULENCE (FLOW) - - - NOISE
- NOISE OCCURS OVER A RANGE OF FREQUENCIES - - TYPICAL TO THE **KIND OF FLOW** CREATED
  - **GAS** flow upward thru liquid
    - » Flows in “bubbles” which “ring”

# NOISE LOG OPERATION PRINCIPLES

- **FLUID TURBULENCE (FLOW) - - - NOISE**
- **NOISE OCCURS OVER A RANGE OF FREQUENCIES - - TYPICAL TO THE KIND OF FLOW CREATED**
  - **FLUID** turbulence when forced across constriction – pressure drop



# NOISE LOG OPERATION PRINCIPLES

- FLUID TURBULENCE (FLOW) - - - NOISE
- NOISE OCCURS OVER A RANGE OF FREQUENCIES - - TYPICAL TO THE KIND OF FLOW CREATED

➤ 200 Hz (cycles per second)

➤ 600 Hz

➤ 1000 Hz

➤ 2000 Hz

# **NOISE LOG EQUIPMENT**

- **TRANSDUCER (converts sound to electrical signal - to be amplified)**
- **FREQUENCY SEPARATING FILTERS**
- **SPEAKER (esp. headphones for operator)**
- **TYPICAL SIZE = 1<sup>3</sup>/<sub>4</sub> inch X 3<sup>1</sup>/<sub>2</sub> feet (as small as 1 inch O.D.)**

# NOISE LOG

## CHARACTERISTICS

ESSENTIAL TO INTERPRETATION

- **LOUDNESS** - measured levels above ambient... amplitude... on all 4 frequencies
  - severity of the problem
- **CHARACTER** – variation in level on a particular cut from station to station is related to the path of flow
  - how flow is taking place
- **PITCH** – frequency content of sound at a peak in noise level
  - type of flow (single phase or gas thru liquid)

# NOISE LOG OPERATION GUIDELINES

- Logging Sonde takes readings at different depths while **STATIONARY**.
- Log can be utilized in virtually any **DOWNHOLE CONDITION** (liquid or gas filled).
- **APPLY CRITERIA**

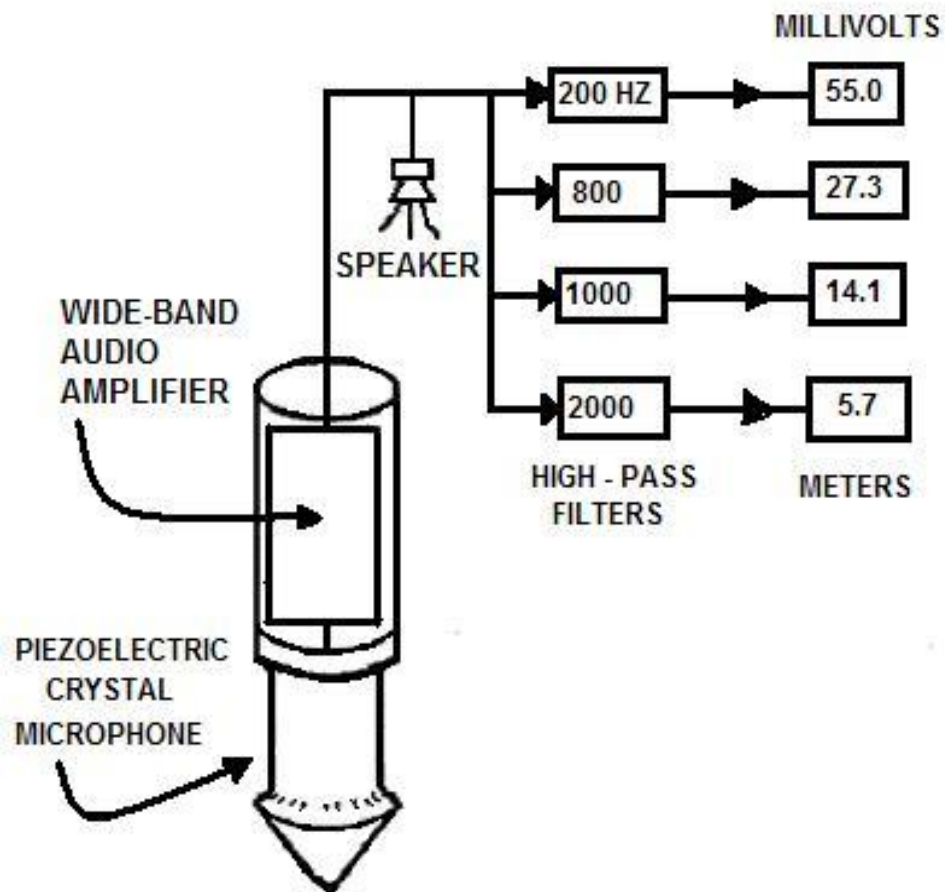
# NOISE LOG

## OPERATION CRITERIA

- Operator consults **CONSTRUCTION DETAILS**
- WELL **SHUT-IN** (for behind-pipe flow)
- Record Noise Levels at the **4 FREQUENCIES** (200Hz, 600Hz, 1000Hz, 2000Hz)
- **MINIMUM READINGS** taken opposite the Confining Layer, Base of USDWs and Well Construction changes
- **SPACING**: readings every 50 to 200 feet (low noise areas); 10 feet or less (zones of interest)
- **READING TIMES** of 3 or more minutes each

# EXAMPLE NOISE LOG PROCEDURE

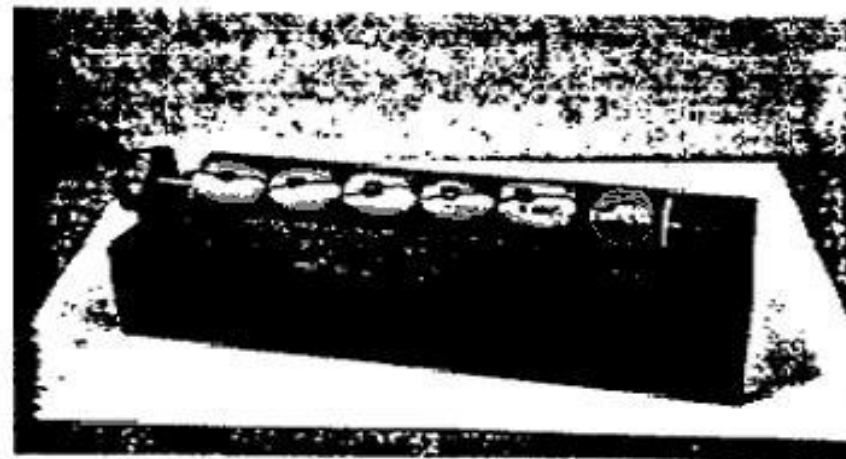
- **PULL TUBING ONLY** if necessary
- **RUN BASE LOG** – well shut-in
- **START INJECTION** (if necessary to initiate flow)
- **RUN NOISE LOG** – at same base log stops
- **ENSURE TOOL IS STATIONARY** at stops
- At **ZONES OF INTEREST**, perform readings at 10 ft. intervals plus/minus for locating source



TOOL SCHEMATIC



SIX PIEZOELECTRIC CRYSTALS



CRYSTALS ASSEMBLED FOR ENCAPSULATION

*Noise (sound) logging sonde with piezoelectric detection elements shown separately*

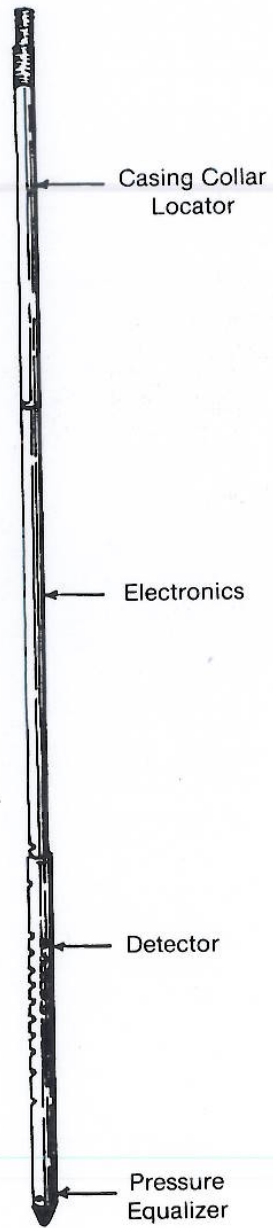
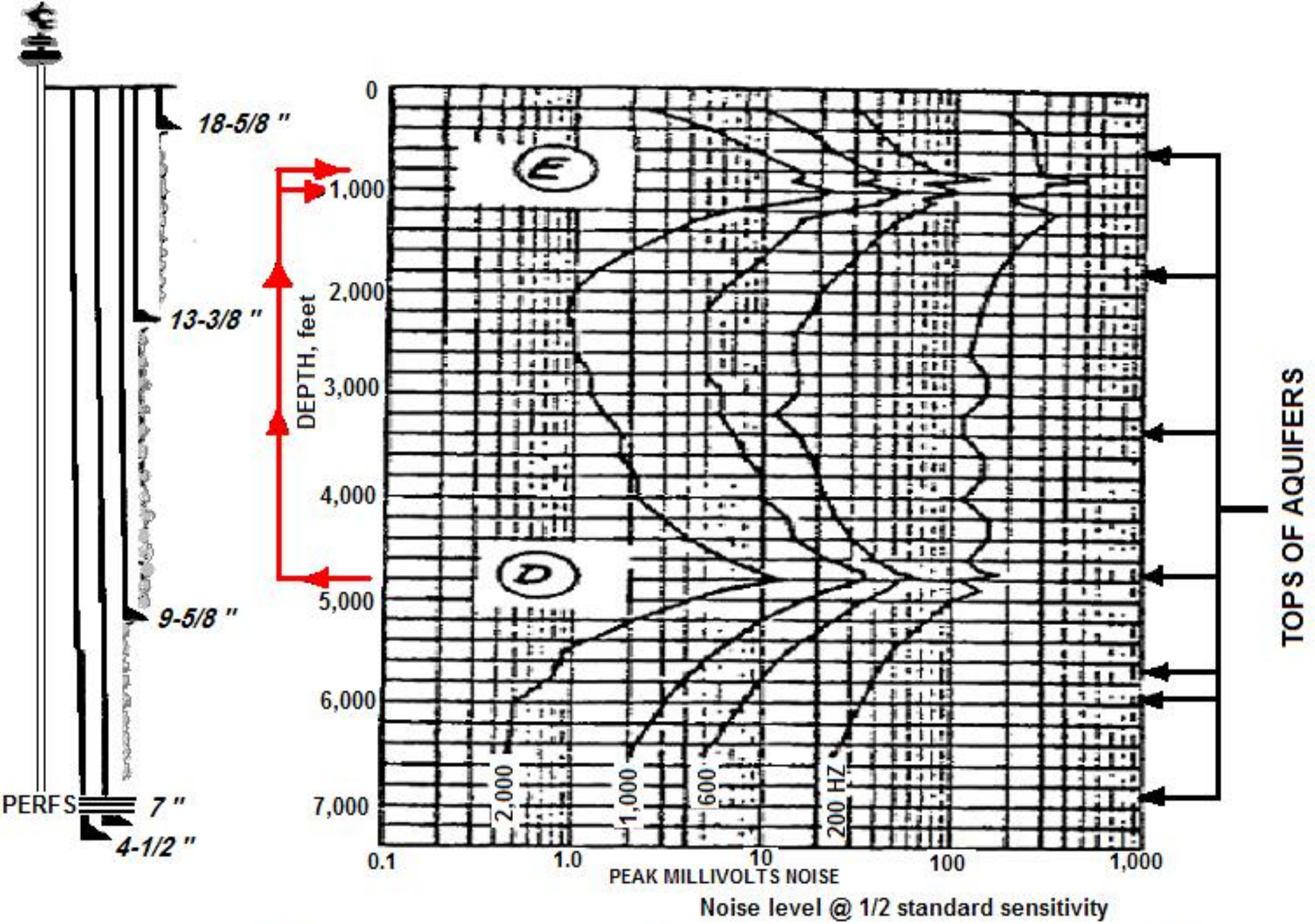


Figure 24. Typical noise logging tool (Robinson, 1976b).





*Noise log from shut-in well with water flow behind pipe @ 5,000 BPD estimated rate*

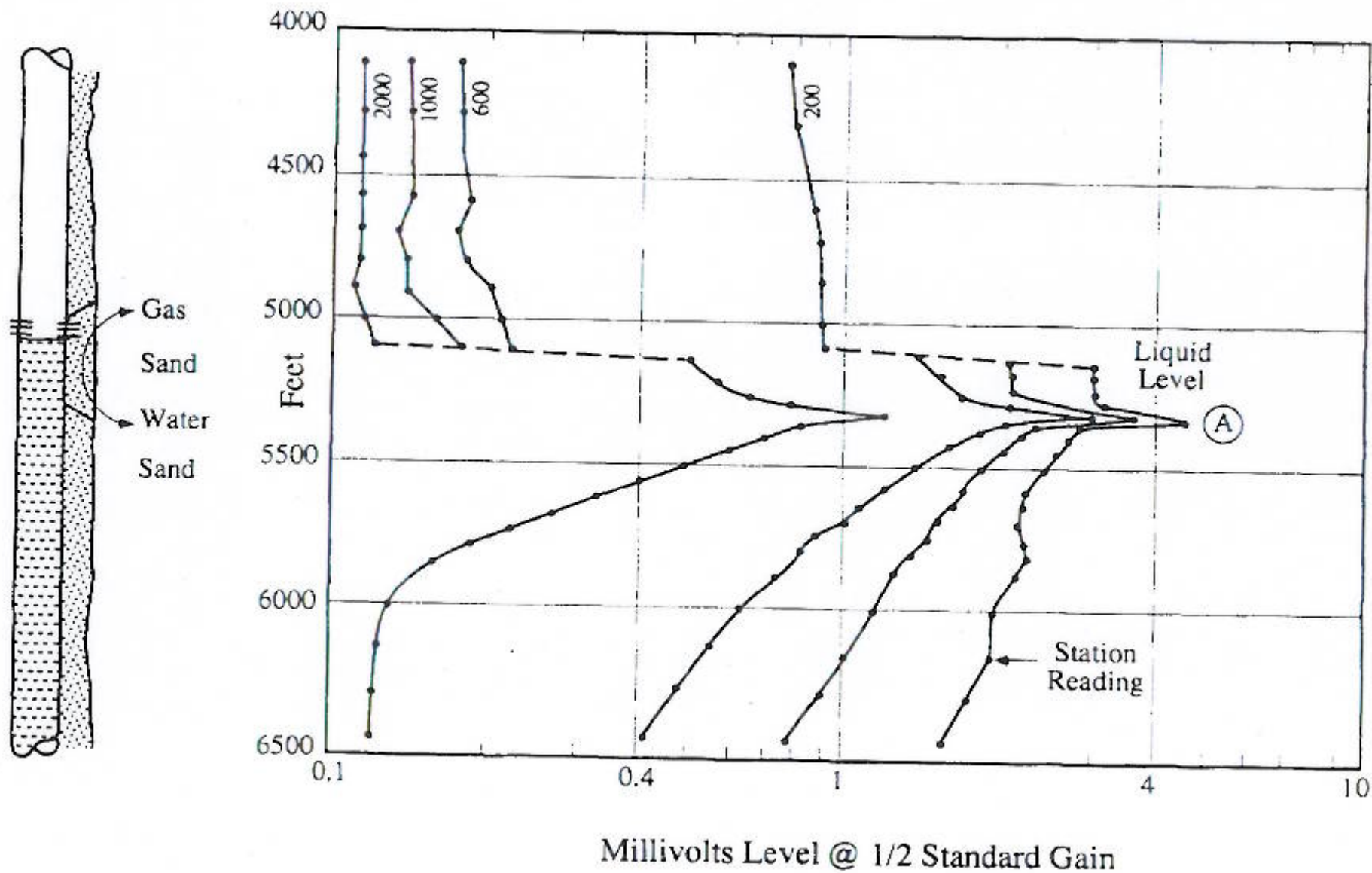


Figure 79. Noise log format with a 20-BPD water flow behind pipe into a gas zone depleted by 250 PSI.

# **OXYGEN ACTIVATION TRACER SURVEYS**

**(OA Logs)**

**(External MI )**

# OA LOG PURPOSE

- **Determine presence of**  
**FLUID FLOW BEHIND CASING**
- **Measure**
  - **Flow DIRECTION**
  - **Linear Flow VELOCITY**
  - **Volume Flow RATE ESTIMATE**
  - **RADIAL DISTANCE From Tool**

# OA LOG

## PRINCIPLE OF OPERATION

- Similar to **Radioactive Tracer Survey (RATS)**
- Tracer is **CREATED** within the flowing water behind the casing
  - Water behind pipe is bombarded with **ENERGETIC NEUTRONS**
  - **Radioactive Nitrogen Isotope** with half-life of 7 seconds formed when neutrons react with oxygen in water
- **EMMITTED GAMMA RAYS** detected by two detectors at different distances

# OA LOG LIMITATIONS

- **DEPTH OF INVESTIGATION**  
(approximately 12 inches)
- **FLUID COMPOSITION**  
(must contain Oxygen)
- **FLUID VELOCITY**

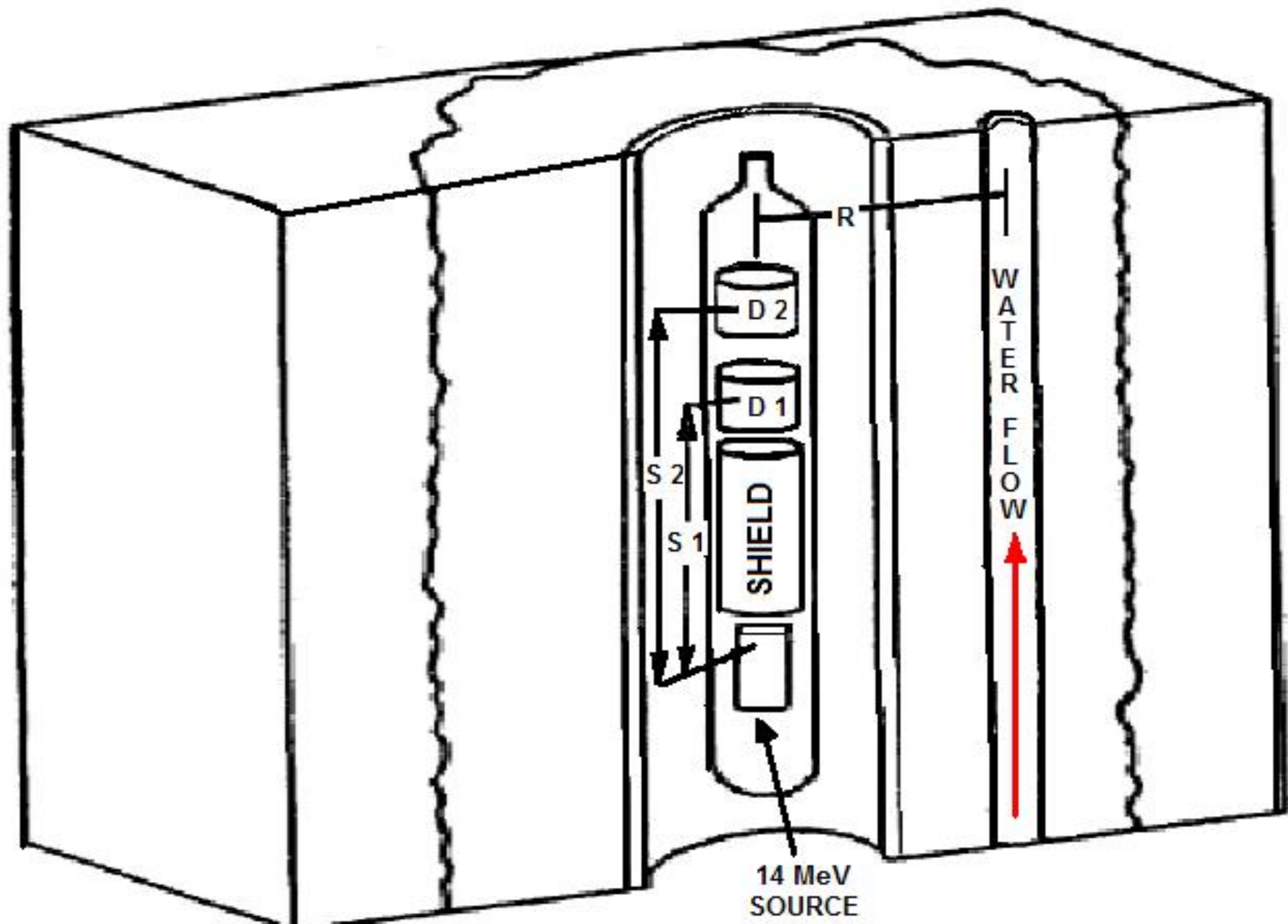
# OA LOG EQUIPMENT

- **NEUTRON SOURCE**
- **NEUTRON SHIELD**
- **2 GAMMA RAY DETECTORS**  
above source to detect upward flow
- **TOOL SIZES**  
1-3/4 to 3-5/8 inches X 34 to 26 feet
- **COMPUTER ANALYSIS @ surface**

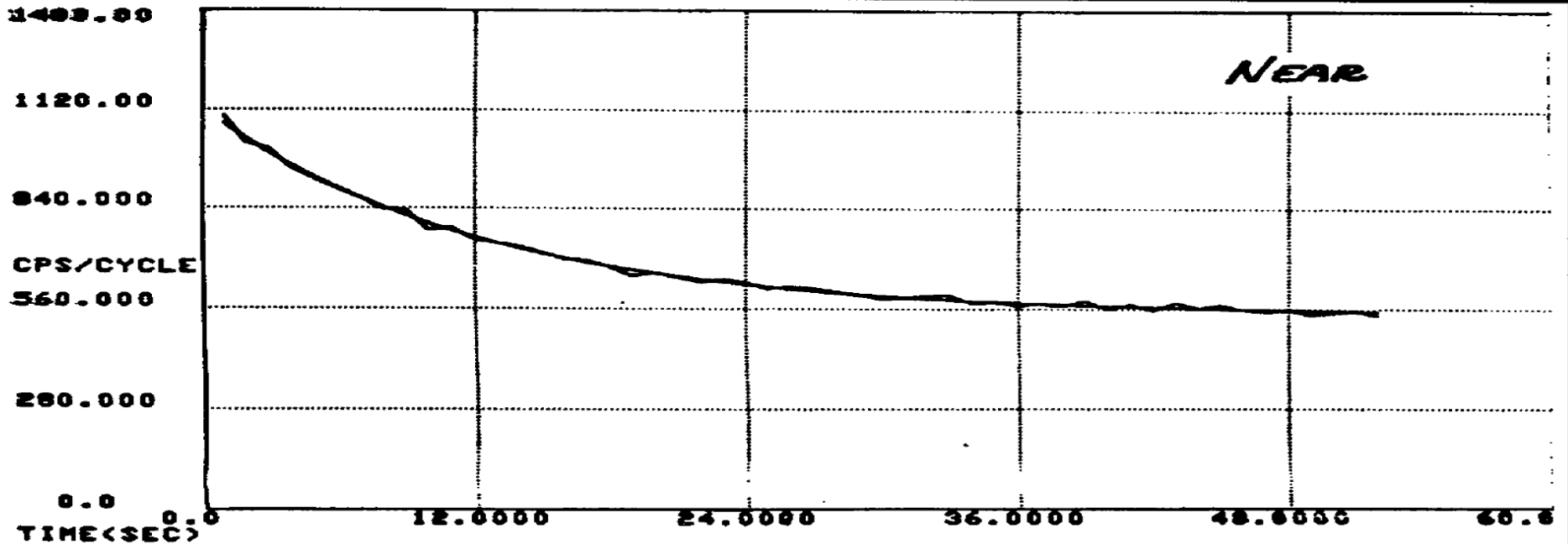
# OA LOG PROCEDURE

- **RUN LOG @ NORMAL INJECTION RATE**
- **CALIBRATE INSTRUMENT**
- **RUN BASE GAMMA-RAY LOG**
- **LOG @ 10 FT. STOPS (5 MIN. EA.)**  
**START BELOW PERFS (NO FLOW)**
  - **RELEASE SOURCE**
  - **READINGS FOR 5 MINUTES**
  - **REPEAT 10 FEET UP HOLE**





***OXYGEN ACTIVATION TOOL SCHEMATIC***



```

FILE NUMBER          DATA ACQUIRED
  25                 05-DEC-1990 11:38

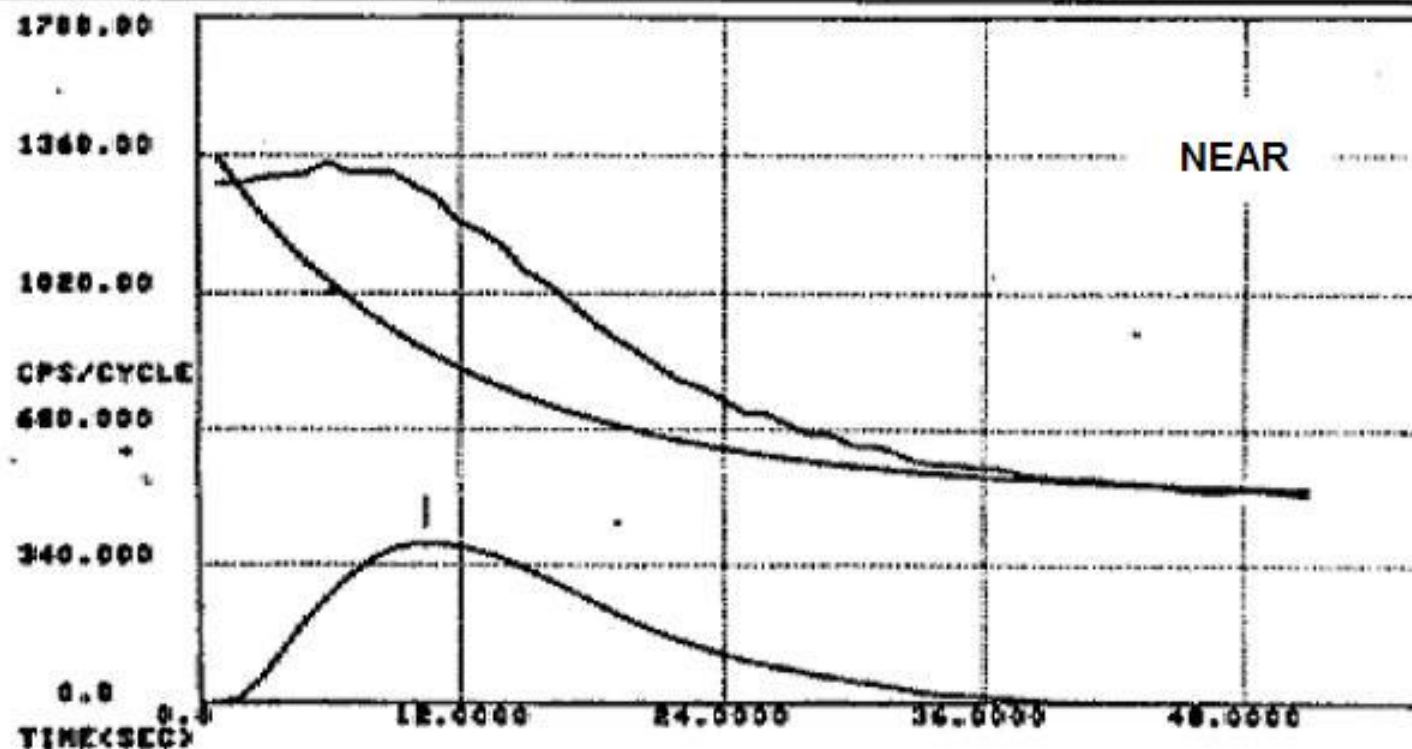
  DETECTOR = NEAR TDT-P          DEPTH = 2493.6 F

CASING SIZE          = 7.000 IN      SFT TYPE          = 178
NEAR TCHK            = 51377.0 CPS    FAR TCHK           = 23345.0 CPS
NEUTRON ON TIME     = 10.0 S         NUMBER OF CYCLES SUMMED = 12

FLOW NOT DETECTED
FLOW VELOCITY = 0.0 FT / MINUTE
FLOW RATE     = 0.0 BHPD

PEAK BACKGROUND SIGNAL = 556.8 +/- 1.3 CPS / CYCLE
PEAK STATIONARY SIGNAL = 548.7 +/- 4.8 CPS / CYCLE
TOTAL FLOWING SIGNAL   = 0.0 +/- 0.0 COUNTS / CYCLE
  
```

*Figure 31A. Mechanical integrity (near counter) at 2493.6 ft*



FILE NUMBER  
44

DATA ACQUIRED  
85-DEC-1990 18:23

DETECTOR = NEAR TDT-P

DEPTH = 3293.6 F

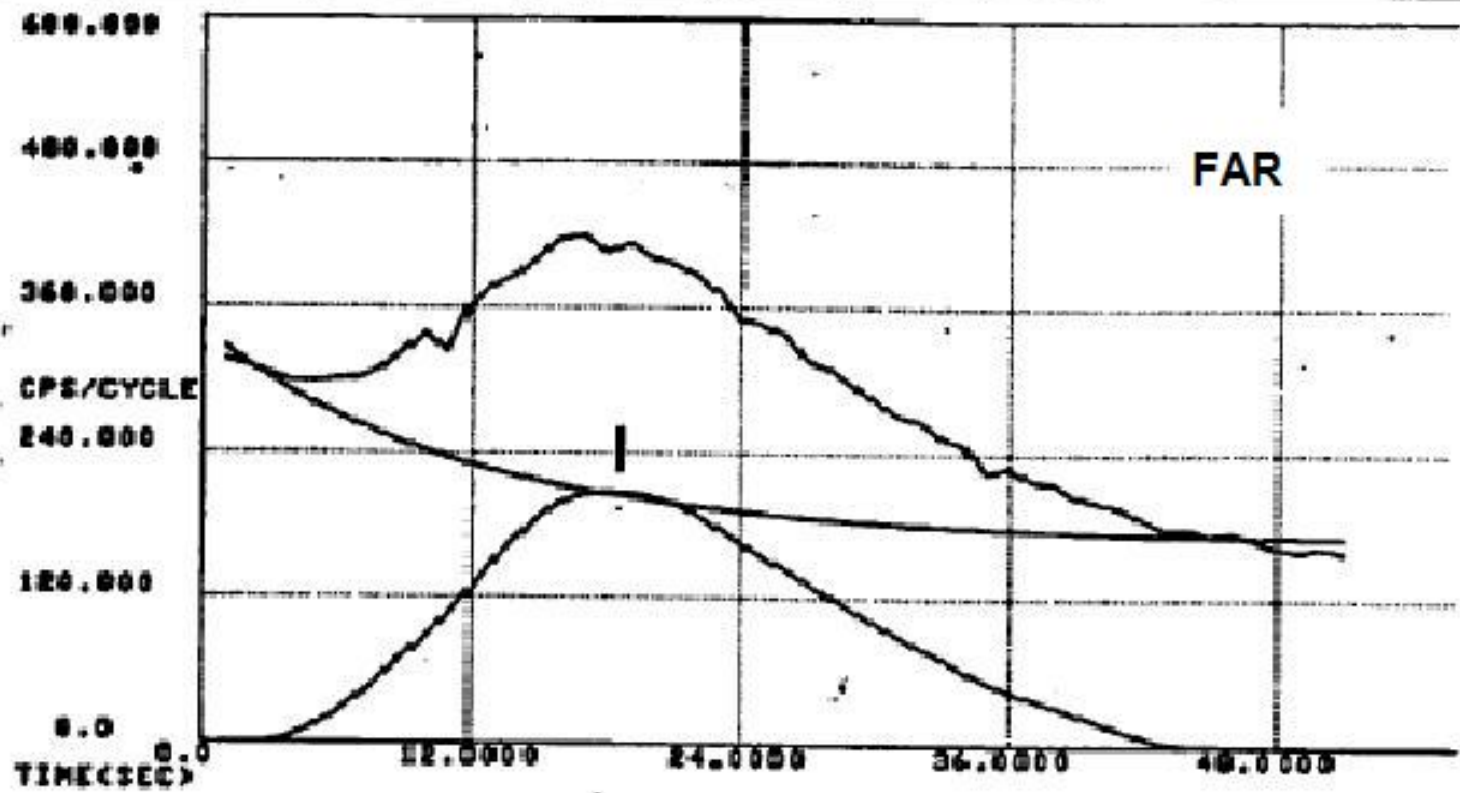
CASING SIZE = 7.000 IN  
NEAR TCHK = 43200.0 CPS  
NEUTRON ON TIME = 10.0 S

SFT TYPE = 278  
FAR TCHK = 21800.0 CPS  
NUMBER OF CYCLES SUMMED = 12

FLOW DETECTED  
FLOW VELOCITY = 1.0 FT / MINUTE  
FLOW RATE = 1.0 BHPD

PEAK BACKGROUND SIGNAL = 333.9 +/- 1.5 CPS / CYCLE  
PEAK STATIONARY SIGNAL = 854.6 +/- 4.3 CPS / CYCLE  
TOTAL FLOWING SIGNAL = 6483.3 +/- 48.1 COUNTS / CYCLE

**SAMPLE AVERAGE SPECTRUM NEAR COUNTER**



FILE NUMBER  
44

DATA ACQUIRED  
05-DEC-1990 18:23

DETECTOR = FAR TST-P

DEPTH = 3293.6 F

CASING SIZE = 7.000 IN  
NEAR TCHK = 43200.0 CPS  
NEUTRON ON TIME = 10.0 S

SFT TYPE = 178  
FAR TCHK = 21200.0 CPS  
NUMBER OF CYCLES SUMMED = 12

FLOW DETECTED  
FLOW VELOCITY = 3.0 FT / MINUTE  
FLOW RATE = 277.9 BWPD

PEAK BACKGROUND SIGNAL = 173.3 +/- 1.0 CPS / CYCLE  
PEAK STATIONARY SIGNAL = 160.8 +/- 2.0 CPS / CYCLE  
TOTAL FLOWING SIGNAL = 4079.7 +/- 39.0 COUNTS / CYCLE

## SAMPLE AVERAGE SPECTRUM FAR COUNTER

